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**APPENDIX A**  
**DETAILED TEST DATA AND TEST RESULTS**

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**TABLE A-1  
SUMMARY OF MERCURY SPECIATION TEST DATA AND TEST RESULTS  
UNIT 6-INLET**

TEST DATA:	1	2	3	
Test run number				
Location		Unit 6 Inlet		
Test date	7/14/99	7/15/99	7/15/99	
Test time period	1415-1640	0825-1050	1250-1510	
<b>PROCESS DATA:</b>				
Unit Load, MW	74	75	75	
Coal feed rate, lb/hr. <sup>(1)</sup>	63700	64200	64000	
Coal Btu content, Btu/lb. (as received)	12038	12132	12121	
Heat Input, 10 <sup>6</sup> Btu/hr (F-Factor)	761.3	818.0	749.1	
<b>SAMPLING DATA:</b>				
Sampling duration, min.	120.0	120.0	120.0	
Nozzle diameter, in.	0.253	0.267	0.267	
Cross sectional nozzle area, sq.ft.	0.000349	0.000389	0.000389	
Barometric pressure, in. Hg	29.47	29.50	29.56	
Avg. orifice press. diff., in H <sub>2</sub> O	1.02	1.17	1.21	
Avg. dry gas meter temp., deg F	112.5	109.0	116.5	
Avg. abs. dry gas meter temp., deg. R	573	569	577	
Total liquid collected by train, ml	149.9	151.2	156.8	
Std. vol. of H <sub>2</sub> O vapor coll., cu.ft.	7.1	7.1	7.4	
Dry gas meter calibration factor	1.0090	1.0090	1.0090	
Sample vol. at meter cond., dcf	68.275	71.469	74.243	
Sample vol. at std. cond., dscf <sup>(2)</sup>	62.713	66.142	67.957	
Percent of isokinetic sampling	103.9	100.6	101.5	
Sample vol. at std. cond., dscm <sup>(2)</sup>	1.776	1.873	1.924	
<b>GAS STREAM COMPOSITION DATA:</b>				
CO <sub>2</sub> , % by volume, dry basis	13.7	13.8	13.4	
O <sub>2</sub> , % by volume, dry basis	4.9	4.9	5.2	
N <sub>2</sub> , % by volume, dry basis	81.4	81.3	81.4	
Molecular wt. of dry gas, lb/lb mole	30.39	30.40	30.35	
H <sub>2</sub> O vapor in gas stream, prop. by vol.	0.101	0.097	0.098	
Mole fraction of dry gas	0.899	0.903	0.902	
Molecular wt. of wet gas, lb/lb mole	29.14	29.20	29.14	
<b>GAS STREAM VELOCITY AND VOLUMETRIC FLOW DATA:</b>				
Static pressure, in. H <sub>2</sub> O	-8.50	-8.00	-8.00	
Absolute pressure, in. Hg	28.85	28.91	28.97	
Avg. temperature, deg. F	309	307	308	
Avg. absolute temperature, deg.R	769	767	768	
Pitot tube coefficient	0.84	0.84	0.84	
Total number of traverse points	12	12	12	
Avg. gas stream velocity, ft./sec.	40.4	39.1	39.8	
Stack/duct cross sectional area, sq.ft.	151.960	151.960	151.960	AVERAGE
Avg. gas stream volumetric flow, wacf/min.(as measured)	368086	356867	363219	362724
Avg. gas stream volumetric flow, dscf/min.(as measured) <sup>(2)</sup>	218890	214153	218163	217068
Avg. gas stream outlet volumetric flow, dscf/min. (adjusted) <sup>(2) (3)</sup>	163300	173606	166999	167968
<b>MERCURY LABORATORY REPORT DATA:</b>				
Particulate bound, ug	4.3410	4.9830	5.0130	
Oxidized, ug	1.0000	1.2100	1.0350	
Elemental, ug	0.2700	0.4150	0.2950	
Total catch, ug	5.6110	6.6080	6.3430	
<b>PARTICULATE BOUND MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	2.44	2.66	2.61	2.57
Conc., ug/Nm <sup>3</sup> <sup>(4)</sup>	2.62	2.85	2.79	2.76
Emission rate, lbs/10 <sup>12</sup> Btu. <sup>(5)</sup>	1.96	2.11	2.18	2.08
Emission rate, lbs/hr. <sup>(5)</sup>	1.50E-03	1.73E-03	1.63E-03	1.62E-03
<b>OXIDIZED MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	0.56	0.65	0.54	0.58
Conc., ug/Nm <sup>3</sup> <sup>(4)</sup>	0.60	0.69	0.58	0.62
Emission rate, lbs/10 <sup>12</sup> Btu. <sup>(5)</sup>	0.45	0.51	0.45	0.47
Emission rate, lbs/hr. <sup>(5)</sup>	3.44E-04	4.20E-04	3.36E-04	3.67E-04
<b>ELEMENTAL MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	0.15	0.22	0.15	0.18
Conc., ug/Nm <sup>3</sup> <sup>(4)</sup>	0.16	0.24	0.16	0.19
Emission rate, lbs/10 <sup>12</sup> Btu. <sup>(5)</sup>	0.12	0.18	0.13	0.14
Emission rate, lbs/hr. <sup>(5)</sup>	9.30E-05	1.44E-04	9.59E-05	1.11E-04
<b>TOTAL MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	3.16	3.53	3.30	3.33
Conc., ug/Nm <sup>3</sup> <sup>(4)</sup>	3.39	3.79	3.54	3.57
Emission rate, lbs/10 <sup>12</sup> Btu. <sup>(5)</sup>	2.54	2.80	2.75	2.70
Emission rate, lbs/hr. <sup>(5)</sup>	1.93E-03	2.29E-03	2.06E-03	2.10E-03

(1) Based on plant gravimetric feeder readings.

(2) Standard conditions = 68 deg. F. (20 deg. C.) and 29.92 inches Hg (760mm Hg).

(3) Measured volumetric flow from the corresponding test run on the Unit 6 outlet corrected for O<sub>2</sub> measured at the inlet location.

(4) Nm<sup>3</sup> = Normal cubic meter ( 32 deg. F. (0 deg. C.) and 29.92 inches Hg (760mm Hg)).

(5) Emission rates are based on the adjusted volumetric flow.

**TABLE A-2**  
**SUMMARY OF MERCURY SPECIATION TEST DATA AND TEST RESULTS**  
**UNIT 6-OUTLET**

TEST DATA:	1	2	3	
Test run number		Unit 6 Outlet		
Location		7/15/99		
Test date	7/14/99	7/15/99	7/15/99	
Test time period	1415-1641	0825-1055	1250-1512	
<b>PROCESS DATA:</b>				
Unit Load, MW	74	75	75	
Coal feed rate, lb/hr <sup>(1)</sup>	63700	64200	64000	
Coal Btu content, Btu/lb. (as received)	12038	12132	12121	
Heat Input, 10 <sup>6</sup> Btu/hr (F-Factor)	761.3	818.0	749.1	
<b>SAMPLING DATA:</b>				
Sampling duration, min.	120.0	120.0	120.0	
Nozzle diameter, in.	0.199	0.210	0.210	
Cross sectional nozzle area, sq. ft.	0.000216	0.000241	0.000241	
Barometric pressure, in. Hg	29.47	29.50	29.56	
Avg. orifice press. diff., in H <sub>2</sub> O	1.37	1.83	1.66	
Avg. dry gas meter temp., deg F	90.3	97.0	89.1	
Avg. abs. dry gas meter temp., deg. R	550	557	549	
Total liquid collected by train, ml	161.4	182.9	174.5	
Std. vol. of H <sub>2</sub> O vapor coll., cu.ft.	7.6	8.6	8.2	
Dry gas meter calibration factor	1.0098	1.0098	1.0098	
Sample vol. at meter cond., def	75.662	86.342	81.939	
Sample vol. at std. cond., dscf <sup>(2)</sup>	72.428	81.834	78.898	
Percent of isokinetic sampling	100.7	98.1	99.5	
Sample vol. at std. cond., dscm <sup>(2)</sup>	2.051	2.317	2.234	
<b>GAS STREAM COMPOSITION DATA:</b>				
CO <sub>2</sub> , % by volume, dry basis	12.6	12.9	12.8	
O <sub>2</sub> , % by volume, dry basis	6.1	5.8	5.9	
N <sub>2</sub> , % by volume, dry basis	81.3	81.3	81.3	
Molecular wt. of dry gas, lb/lb mole	30.26	30.30	30.28	
H <sub>2</sub> O vapor in gas stream, prop. by vol.	0.095	0.095	0.094	
Mole fraction of dry gas	0.905	0.905	0.906	
Molecular wt. of wet gas, lb/lb mole	29.10	29.13	29.13	
<b>GAS STREAM VELOCITY AND VOLUMETRIC FLOW DATA:</b>				
Static pressure, in. H <sub>2</sub> O	-1.90	-1.90	-1.90	
Absolute pressure, in. Hg	29.33	29.36	29.42	
Avg. temperature, deg. F	305	304	306	
Avg. absolute temperature, deg. R	765	764	766	
Pitot tube coefficient	0.84	0.84	0.84	
Total number of traverse points	12	12	12	
Avg. gas stream velocity, ft./sec.	75.6	78.6	74.6	AVERAGE
Stack/duct cross sectional area, sq.ft.	63.617	63.617	63.617	
Avg. gas stream volumetric flow, wactf/min.	288413	299873	284780	291022
Avg. gas stream volumetric flow, dscf/min <sup>(2)</sup>	176540	183953	174792	178428
<b>MERCURY LABORATORY REPORT DATA:</b>				
Particulate bound, ug	0.1000	0.0510	< 0.0100	
Oxidized, ug	1.4300	1.9750	1.3800	
Elemental, ug	1.1800	1.8150	1.5300	
Total catch, ug	2.7100	3.8410	2.9100	
<b>PARTICULATE BOUND MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	0.049	0.022	< 0.004	0.035
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	0.052	0.024	< 0.005	0.038
Emission rate, lbs/10 <sup>12</sup> Btu.	0.042	0.019	< 0.004	0.030
Emission rate, lbs/hr	3.22E-05	1.52E-05	< 2.93E-06	2.37E-05
<b>OXIDIZED MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	0.70	0.85	0.62	0.72
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	0.75	0.91	0.66	0.78
Emission rate, lbs/10 <sup>12</sup> Btu.	0.61	0.72	0.54	0.62
Emission rate, lbs/hr	4.61E-04	5.87E-04	4.04E-04	4.84E-04
<b>ELEMENTAL MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	0.58	0.78	0.68	0.68
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	0.62	0.84	0.73	0.73
Emission rate, lbs/10 <sup>12</sup> Btu.	0.50	0.66	0.60	0.59
Emission rate, lbs/hr	3.80E-04	5.40E-04	4.48E-04	4.56E-04
<b>TOTAL MERCURY EMISSIONS: <sup>(4)</sup></b>				
Conc., ug/m <sup>3</sup>	1.32	1.66	1.30	1.43
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	1.42	1.78	1.40	1.53
Emission rate, lbs/10 <sup>12</sup> Btu.	1.15	1.40	1.14	1.23
Emission rate, lbs/hr	8.74E-04	1.14E-03	8.53E-04	9.56E-04
<b>TOTAL MERCURY REMOVAL EFFICIENCY:</b>	54.73%	50.13%	58.60%	54.49%

(1) Based on plant gravimetric feeder readings.

(2) Standard conditions = 68 deg. F. (20 deg. C.) and 29.92 inches Hg (760mm Hg).

(3) Nm<sup>3</sup> = Normal cubic meter ( 32 deg. F. (0 deg. C.) and 29.92 inches Hg (760mm Hg)).

(4) Non-detects not included in Total mercury catch value or in average emission rate.

**TABLE A-3**  
**SUMMARY OF MERCURY SPECIATION TEST DATA AND TEST RESULTS**  
**Unit 1-4 Outlet**

TEST DATA:	1	2	3	
Test run number				
Location		Units 1-4 Outlet		
Test date	7/16/99	7/16/99	7/16/99	
Test time period	0820-1037	1115-1338	1410-1641	
<b>PROCESS DATA:</b>				
Unit Load, MW	124	127	138	
Coal feed rate, lb/hr <sup>(1)</sup>	110000	111000	117000	
Coal Btu content, Btu/lb. (as received)	12180	12180	12180	
Heat Input, 10 <sup>6</sup> Btu/hr (F-Factor)	1784	1638	1755	
<b>SAMPLING DATA:</b>				
Sampling duration, min.	120.0	120.0	120.0	
Nozzle diameter, in.	0.150	0.152	0.150	
Cross sectional nozzle area, sq.ft.	0.000123	0.000126	0.000123	
Barometric pressure, in. Hg	29.50	29.50	29.50	
Avg. orifice press. diff., in H <sub>2</sub> O	1.13	0.94	0.98	
Avg. dry gas meter temp., deg F	96.6	98.7	99.8	
Avg. abs. dry gas meter temp., deg. R	557	559	560	
Total liquid collected by train, ml	138.9	106.1	125.7	
Std. vol. of H <sub>2</sub> O vapor coll., cu.ft.	6.5	5.0	5.9	
Dry gas meter calibration factor	1.0000	1.0000	1.0000	
Sample vol. at meter cond., dcf	68.759	54.982	60.161	
Sample vol. at std. cond., dscf <sup>(2)</sup>	68.759	54.982	60.161	
Percent of isokinetic sampling	109.6	90.4	96.8	
Sample vol. at std. cond., dscm <sup>(3)</sup>	1.947	1.557	1.704	
<b>GAS STREAM COMPOSITION DATA:</b>				
CO <sub>2</sub> , % by volume, dry basis	13.4	13.0	13.3	
O <sub>2</sub> , % by volume, dry basis	6.2	6.6	6.3	
N <sub>2</sub> , % by volume, dry basis	80.4	80.4	80.4	
Molecular wt. of dry gas, lb/lb mole	30.39	30.34	30.38	
H <sub>2</sub> O vapor in gas stream, prop. by vol.	0.087	0.083	0.090	
Mole fraction of dry gas	0.913	0.917	0.910	
Molecular wt. of wet gas, lb/lb mole	29.32	29.32	29.27	
<b>GAS STREAM VELOCITY AND VOLUMETRIC FLOW DATA:</b>				
Static pressure, in. H <sub>2</sub> O	-2.00	-2.00	-2.04	
Absolute pressure, in. Hg	29.35	29.35	29.35	
Avg. temperature, deg. F	285	299	310	
Avg. absolute temperature, deg.R	745	759	770	
Pitot tube coefficient	0.84	0.84	0.84	
Total number of traverse points	12	12	12	
Avg. gas stream velocity, ft./sec.	111.9	107.1	114.9	AVERAGE
Stack/duct cross sectional area, sq.ft.	97.930	97.930	97.930	
Avg. gas stream volumetric flow, wacfm/min.	657762	629574	675345	654227
Avg. gas stream volumetric flow, dscfm/min <sup>(2)</sup>	417226	393930	413261	408139
<b>MERCURY LABORATORY REPORT DATA:</b>				
Particulate bound, ug	< 0.0080	< 0.0080	< 0.0080	
Oxidized, ug	0.4850	0.2600	0.3250	
Elemental, ug	0.0850	0.1550	0.0200	
Total mercury catch, ug	0.5700	0.4150	0.3450	
<b>PARTICULATE BOUND MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	< 0.004	< 0.005	< 0.005	< 0.005
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	< 0.004	< 0.006	< 0.005	< 0.005
Emission rate, lbs/10 <sup>12</sup> Btu.	< 3.60E-03	< 4.63E-03	< 4.14E-03	< 4.12E-03
Emission rate, lbs/hr	< 6.42E-06	< 7.58E-06	< 7.27E-06	< 7.09E-06
<b>OXIDIZED MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	0.25	0.17	0.19	0.20
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	0.27	0.18	0.20	0.22
Emission rate, lbs/10 <sup>12</sup> Btu.	0.22	0.15	0.17	0.18
Emission rate, lbs/hr	3.89E-04	2.46E-04	2.95E-04	3.10E-04
<b>ELEMENTAL MERCURY EMISSIONS:</b>				
Conc., ug/m <sup>3</sup>	0.04	0.10	0.01	0.05
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	0.05	0.11	0.01	0.06
Emission rate, lbs/10 <sup>12</sup> Btu.	0.04	0.09	0.01	0.05
Emission rate, lbs/hr	6.82E-05	1.47E-04	1.82E-05	7.78E-05
<b>TOTAL MERCURY EMISSIONS: <sup>(4)</sup></b>				
Conc., ug/m <sup>3</sup>	0.29	0.27	0.20	0.25
Conc., ug/Nm <sup>3</sup> <sup>(3)</sup>	0.31	0.29	0.22	0.27
Emission rate, lbs/10 <sup>12</sup> Btu.	0.26	0.24	0.18	2.25E-01
Emission rate, lbs/hr	4.58E-04	3.93E-04	3.13E-04	3.88E-04

(1) Based on plant gravimetric feeder readings.

(2) Standard conditions = 68 deg. F. (20 deg. C.) and 29.92 inches Hg (760mm Hg).

(3) Nm<sup>3</sup> = Normal cubic meter (32 deg. F. (0 deg. C.) and 29.92 inches Hg (760mm Hg)).

(4) Non-detects not included in the total mercury catch value or in the average emission rates.

**Table A-4**  
**Presque Isle Hg Balance Data - July 1999**  
**Unit No. 6 Hg Material Balance Data**

	Test #1	Test #2	Test #3	Avgerage
Plant Load, MWe	73.9	73.4	73.2	73.5
<b>COAL DATA</b>				
% Carbon	72.90	72.84	74.46	73.40
% Ash	10.28	10.05	9.99	10.11
Btu	12694	12784	12772	12750
ppm Hg	0.039	0.039	0.039	0.039
F-Factor	9853	9749	10048	9883
Stack DSCFM	176540	183953	174792	178428
Stack DSCMM	4996	5206	4947	5050
Outlet % O <sub>2</sub>	6.1	5.8	5.9	5.9
EA Free, DSCFM	125014	132904	125449	127789
Heat Input, MM Btu/hr	761.3	818.0	749.1	776.1
Coal Firing Rate, lb/h <sup>(1)</sup>	59971	63983	58652	60868
Inlet % O <sub>2</sub>	4.9	4.9	5.2	5.0
Inlet DSCFM	163300	173606	166999	167968
Inlet DSCMM	4621	4913	4726	4753
ESP Ash Loading, lb/h	6219	7010	6018	6416
% Carbon in Ash	16.49	17.65	17.86	17.33
% Ash in Ash	82.30	81.30	80.89	81.50
ppm Hg in Ash	0.116	0.133	0.136	0.128
lb/h Carbon	1026	1237	1075	1113
lb/h Ash	5118	5699	4868	5228
Total Coal Fired, lb/h <sup>(2)</sup>	61378	65681	60095	62385
Total Coal Fired, lb/h <sup>(3)</sup>	63700	64200	64000	63967
% Diff in Coal Feed Rate	-4%	2%	-6%	-3%
Total Heat Input, MM Btu/h	779	840	768	795
Unit Heat Rate, Btu/kwh	10543	11440	10485	10823
Carbon Utilization	97.71	97.41	97.60	98
Maximum Ash Production, lb/h	6310	6601	6003	6305
% Ash in ESP Hoppers	81%	86%	81%	83%
Hg Input, ug/min	18093	19361	17715	18389
Max Hg in Inlet Gas, ug/m <sup>3</sup>	3.91	3.94	3.75	3.87
Hg in ESP Ash, ug/min	5453	7047	6186	6229
% of Total Hg in Coal	30.1%	36.4%	34.9%	33.8%
Total Hg at Inlet, ug/m <sup>3</sup>	3.16	3.53	3.30	3.33
Inlet Hg, ug/min	14604	17343	15596	15848
<b>% Hg Balance at Inlet</b>	<b>80.7%</b>	<b>89.6%</b>	<b>88.0%</b>	<b>86.1%</b>
Gas Phase Hg at Stack, ug/m <sup>3</sup>	1.32	1.66	1.30	1.43
Stack Hg, ug/min	6595	8642	6431	7222
Hg in Ash and Stack Gas, ug/min	12047	15689	12617	13451
<b>% of Total Hg Input in Coal</b>	<b>66.6%</b>	<b>81.0%</b>	<b>71.2%</b>	<b>72.9%</b>

1 - Coal firing rate from stack gas flow rate

2 - Coal firing rate from stack gas flow rate and carbon in fly ash

3 - Coal firing rate from plant totalizers

**Table A-5**  
**Presque Isle Hg Balance Data - July 1999**  
**Units 1-4 Hg Material Balance Data**

	Test 1	Test 2	Test 3	Average
Stack Gas Flow, dscfm	417226	393930	413261	408139
Stack Gas Flow, dscmm	11807	11148	11695	11550
%O2 in Flue Gas	6.2	6.6	6.3	6.4
Coal Btu/lb	12874	12874	12874	12874
Coal F-Factor	9870	9870	9870	9870
Heat Input, MM Btu/h	1784	1638	1755	1726
Coal Firing Rate, lb/h <sup>(1)</sup>	138568	127271	136317	134052
Estimated Plant Load, MWe	162	149	160	157
Inlet % O2	4.5	4.5	4.5	4.5
Estimated Inlet dscfm	373977	343488	367903	361789
Estimated Inlet dscmm	10584	9721	10412	10239
Coal Hg Conc., ppm	0.02	0.02	0.02	0.02
Coal Ash Conc., %	9.79	9.79	9.79	9.79
ESP Hg Conc., ppm	0.131	0.145	0.129	0.14
ESP Ash Conc., %	69.42%	74.40%	71.63%	71.8%
ESP Ash Ratio	80.0%	80.0%	80.0%	80.0%
Hg Input, ug/min	20947	19239	20607	20264
Baghouse Max Hg in Inlet Gas, ug	1.98	1.98	1.98	1.98
Total Ash Rate, lb/h	13566	12460	13345	13124
Ash Into Baghouse, lb/h	10853	9968	10676	10499
Baghouse Dust Loading, lb/h gr/dscf	15633 4.88	13398 4.55	14905 4.73	14645 4.72
Hg in Baghouse Ash, ug/min	15479	14683	14533	14898
% of Total Hg	73.9%	76.3%	70.5%	73.6%
Est. Gas Phase Hg at Inlet, ug/m3	0.52	0.47	0.58	0.52
Meas. Gas Phase Hg at Stack, ug	0.29	0.27	0.20	0.25
Hg in Stack Flue Gas, ug/min	3424	3010	2339	2924
% of Total Hg	16.3%	15.6%	11.4%	14.4%
Total Hg in Output Streams, ug/min	18903	17693	16872	17823
% of Total Hg	90.2%	92.0%	81.9%	88.0%

(1) Coal firing rate from stack gas flow rate.

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**APPENDIX B**  
**PROCESS OPERATIONS, FACILITY CEMS AND ESP DATA**

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## UNIT 6 PROCESS OPERATIONS DATA

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PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: SIX

TIME: 1400-1500

DATE: 7-14-99

- |                 |  |                 |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|-----------------|--|-----------------|-------------|--------------------------------|-----------------|---------------|-----------------------------|-----------------|---------------|-----------------------------|-----------------|---------------|------------|-----------------|---------------|------------|--|-----|-----------------------------|-------|
| ①               | Gross Generation - MWH   | <u>75.336</u>   | ③⑤          | Lbs. Coal/Net KWH              | <u>923</u>      |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ②               | Station Service - MWH  | <u>6.000</u>    | ③⑥          | Lbs. Steam/Net KWH             | <u>6.461</u>    |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ③               | Net Generation - MWH   | <u>69.336</u>   | 38.         | Barometric Press. In.Hg        | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ④               | Control Valve Position %   | <u>88%</u>      | 39.         | Vacuum In.Hg                   | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑤               | Main Steam Flow Lbs./Hr.   | <u>448000</u>   | 40.         | Back Press. In.Hg              | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑥               | F.W. Flow Lbs./Hr.   | <u>469000</u>   | 41.         | Circ. Water Pump Amps          | A _____ B _____ |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑦               | F.W. Press. Psig   | <u>1530</u>     |             |                                | N or W S or E   |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 8.              | Chart Throttle Press. Psig   | _____           | 42.         | Circ. Water Inlet Temp. °F     | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 9.              | Test Gauge Throttle Press. Psig  | _____           | 43.         | Circ. Water Outlet Temp °F     | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑩               | First Stage Press. Psig  | <u>980</u>      | 44.         | Circ. Water Inlet Press. Psig  | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑪               | Cold Reheat Press. Psig  | <u>345</u>      | 45.         | Circ. Water Outlet Press. Psig | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑫               | Hot Reheat Press. Psig   | <u>329</u>      | 46.         | Condensate Make-up             | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑬               | F.W. (Loading/Temp.)   | <u>45% 397</u>  | 47.         | Condensate Draw-off            | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑭               | Main Steam Temp. °F  | <u>990</u>      | 48.         | Hot Well Temp. °F              | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑮               | Cold Reheat Temp. °F   | <u>648</u>      | 49.         | Turbine Exhaust Temp. °F       | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑯               | Hot Reheat Temp. °F  | <u>670</u>      | 50.         | 1st Pt.Htr.Ext.Press. Psig     | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑰               | Superheat Spray Flow   | <u>0</u>        | 51.         | 1st Pt.Htr.Ext.Temp. °F        | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑱               | Reheat Spray Flow  | <u>0</u>        | 52.         | 1st Pt.Htr.F.W.Out Temp. °F    | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑲               | Air Flow   | <u>520000</u>   | 53.         | 2nd Pt.Htr.Ext.Press. Psig     | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ⑳               | Excess Oxygen %  | <u>3.2%</u>     | 54.         | 2nd Pt.Htr.Ext. Temp. °F       | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ㉑               | Inlet Air Temp. °F   | <u>130</u>      | 55.         | 2nd Pt.Htr.F.W.Out Temp. °F    | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ㉒               | Gas Outlet Temp. °F  | <u>280</u>      | 56.         | 3rd Pt.Htr.Ext. Press. Psig    | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 23.             | Opacity %  | <u>15.1%</u>    | 57.         | 3rd Pt.Htr.Ext. Temp. °F       | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ㉔               | I.D. Fan (Loading/Amps)  | <u>64% 156</u>  | 58.         | 3rd Pt.Htr.F.W.Out Temp. °F    | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ㉕               | F.D. Fan (Loading/rpm/Amps)  | <u>62% 85</u>   | 59.         | 4th Pt.Htr.Ext.Press. Psig     | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ㉖               | Air Heater Press. (H2O)  | _____           | 60.         | 4th Pt.Htr.Ext. Temp. °F       | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 | AIR <table border="0"><tr><td>IN</td><td>OUT</td><td>P</td></tr><tr><td><u>6.2</u></td><td><u>2.0</u></td><td><u>4.2</u></td></tr></table>   | IN              | OUT         | P                              | <u>6.2</u>      | <u>2.0</u>    | <u>4.2</u>                  |                 | 61.           | 4th Pt.Htr.F.W.Out Temp. °F | _____           |               |            |                 |               |            |  |     |                             |       |
| IN              | OUT  | P               |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| <u>6.2</u>      | <u>2.0</u>   | <u>4.2</u>      |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 | GAS <table border="0"><tr><td><u>-2.5</u></td><td><u>-7.4</u></td><td><u>4.9</u></td></tr></table>   | <u>-2.5</u>     | <u>-7.4</u> | <u>4.9</u>                     |                 | 62.           | 5th Pt.Htr.Ext. Press.In.Hg | _____           |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| <u>-2.5</u>     | <u>-7.4</u>  | <u>4.9</u>      |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 27.             | Burner Tilt Position/RH P  | _____           | 63.         | 5th Pt.Htr.Ext. Temp. °F       | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 28.             | Condensate Pump Amps   | A _____ B _____ | 64.         | 5th Pt.Htr.F.W.In Temp., °F    | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 29.             | Boiler Feed Pump Amps  | A _____ B _____ | 65.         | 5th Pt.Htr.F.W.Out Temp. °F    | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 | C _____  |                 | 66.         | 1st Pt.F.W.Out Temp.Minus(-)   | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 30.             | Coal Feeder Loading  | A _____ B _____ |             | 5th Pt.F.W. In Temp. °F -      | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 | C _____ D _____  |                 | 67.         | 1st Pt. Drain Temp. °F         | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 31.             | Pulverizer Amps  | A _____ B _____ | 68.         | 2nd Pt. Drain Temp. °F         | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 | C _____ D _____  |                 | 69.         | 3rd Pt. Drain Temp. °F         | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| 32.             | Mill Outage Temp.  | A _____ B _____ | 70.         | 4th Pt. Drain Temp. °F         | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 | C _____ D _____  |                 | 71.         | 5th Pt. Drain Temp. °F         | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ③③              | Coal Scale Readings:   |                 | 72.         | Vars - Mvar                    | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 | <table border="0"><tr><td>Beginning</td><td>Ending</td><td>Total</td></tr><tr><td><u>a 367627</u></td><td><u>367792</u></td><td><u>165</u></td></tr><tr><td><u>b 564242</u></td><td><u>564400</u></td><td><u>158</u></td></tr><tr><td><u>c 207131</u></td><td><u>207290</u></td><td><u>159</u></td></tr><tr><td><u>d 837732</u></td><td><u>837890</u></td><td><u>158</u></td></tr></table> | Beginning       | Ending      | Total                          | <u>a 367627</u> | <u>367792</u> | <u>165</u>                  | <u>b 564242</u> | <u>564400</u> | <u>158</u>                  | <u>c 207131</u> | <u>207290</u> | <u>159</u> | <u>d 837732</u> | <u>837890</u> | <u>158</u> |  | 73. | Generator Voltage - K volts | _____ |
| Beginning       | Ending   | Total           |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| <u>a 367627</u> | <u>367792</u>  | <u>165</u>      |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| <u>b 564242</u> | <u>564400</u>  | <u>158</u>      |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| <u>c 207131</u> | <u>207290</u>  | <u>159</u>      |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| <u>d 837732</u> | <u>837890</u>  | <u>158</u>      |             |                                |                 |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 |  |                 | 74.         | Auxiliary Steam Uses:          | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
|                 |  |                 | 75.         | Remarks:                       | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |
| ③④              | Coal Total Lbs. Hr.  | <u>64000</u>    |             |                                | _____           |               |                             |                 |               |                             |                 |               |            |                 |               |            |  |     |                             |       |

LANGFORD  
CRO  
\_\_\_\_\_ Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: SIX

TIME: 1500-1600

DATE: 7-14-99

- ① Gross Generation - MWH 73.264
  - ② Station Service - MWH 4.000
  - ③ Net Generation - MWH 69.264
  - ④ Control Valve Position % 88%
  - ⑤ Main Steam Flow Lbs./Hr. 445000
  - ⑥ F.W. Flow Lbs./Hr. 469000
  - ⑦ F.W. Press. Psig 1530
  - 8. Chart Throttle Press. Psig \_\_\_\_\_
  - 9. Test Gauge Throttle Press. Psig \_\_\_\_\_
  - ⑩ First Stage Press. Psig 980
  - ⑪ Cold Reheat Press. Psig 346
  - ⑫ Hot Reheat Press. Psig 329
  - ⑬ F.W. (Loading/Temp.) 47% 397
  - ⑭ Main Steam Temp. °F 990
  - ⑮ Cold Reheat Temp. °F 644
  - ⑯ Hot Reheat Temp. °F 960
  - ⑰ Superheat Spray Flow 0
  - ⑱ Reheat Spray Flow 0
  - ⑲ Air Flow 515000
  - ⑳ Excess Oxygen % 3.1%
  - ㉑ Inlet Air Temp. °F 132
  - ㉒ Gas Outlet Temp. °F 282
  - 23. Opacity % 12.5%
  - ⑳ I.D. Fan (Loading/Amps) 63% 157
  - ㉑ F.D. Fan (Loading/rpm/Amps) 63% 85
  - ⑳ Air Heater Press. (H2O)
- |     | IN          | OUT         | P          |
|-----|-------------|-------------|------------|
| AIR | <u>5.75</u> | <u>1.75</u> | <u>4.0</u> |
| GAS | <u>2.8</u>  | <u>-7.4</u> | <u>4.6</u> |
- 27. Burner Tilt Position/RH P \_\_\_\_\_
  - 28. Condensate Pump Amps A. \_\_\_\_\_ B. \_\_\_\_\_
  - 29. Boiler Feed Pump Amps A. \_\_\_\_\_ B. \_\_\_\_\_
  - C. \_\_\_\_\_
  - 30. Coal Feeder Loading A. \_\_\_\_\_ B. \_\_\_\_\_
  - C. \_\_\_\_\_ D. \_\_\_\_\_
  - 31. Pulverizer Amps A. \_\_\_\_\_ B. \_\_\_\_\_
  - C. \_\_\_\_\_ D. \_\_\_\_\_
  - 32. Mill Outage Temp. A. \_\_\_\_\_ B. \_\_\_\_\_
  - C. \_\_\_\_\_ D. \_\_\_\_\_
  - ⑳ Coal Scale Readings:
- |   | Beginning     | Ending        | Total      |
|---|---------------|---------------|------------|
| a | <u>367792</u> | <u>367957</u> | <u>165</u> |
| b | <u>564400</u> | <u>564558</u> | <u>158</u> |
| c | <u>207290</u> | <u>207448</u> | <u>158</u> |
| d | <u>837890</u> | <u>838049</u> | <u>159</u> |
- ⑳ Coal Total Lbs. Hr. 64,000

- ⑳ Lbs. Coal/Net KWH 924
- ㉑ Lbs. Steam/Net KWH 6425
- 38. Barometric Press. In.Hg \_\_\_\_\_
- 39. Vacuum In.Hg \_\_\_\_\_
- 40. Back Press. In.Hg \_\_\_\_\_
- 41. Circ. Water Pump Amps A. \_\_\_\_\_ B. \_\_\_\_\_
- N or W S or E
- 42. Circ. Water Inlet Temp. °F \_\_\_\_\_
- 43. Circ. Water Outlet Temp °F \_\_\_\_\_
- 44. Circ. Water Inlet Press. Psig \_\_\_\_\_
- 45. Circ. Water Outlet Press. Psig \_\_\_\_\_
- 46. Condensate Make-up \_\_\_\_\_
- 47. Condensate Draw-off \_\_\_\_\_
- 48. Hot Well Temp. °F \_\_\_\_\_
- 49. Turbine Exhaust Temp. °F \_\_\_\_\_
- 50. 1st Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 51. 1st Pt.Htr.Ext.Temp. °F \_\_\_\_\_
- 52. 1st Pt.Htr.F.W.Out Temp °F \_\_\_\_\_
- 53. 2nd Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 54. 2nd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 55. 2nd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 56. 3rd Pt.Htr.Ext. Press. Psig \_\_\_\_\_
- 57. 3rd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 58. 3rd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 59. 4th Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 60. 4th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 61. 4th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 62. 5th Pt.Htr.Ext. Press.In.Hg \_\_\_\_\_
- 63. 5th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 64. 5th Pt.Htr.F.W.In Temp. °F \_\_\_\_\_
- 65. 5th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 66. 1st Pt.F.W.Out Temp.Minus(-) \_\_\_\_\_
- 5th Pt.F.W. In Temp. °F - \_\_\_\_\_
- 67. 1st Pt. Drain Temp. °F \_\_\_\_\_
- 68. 2nd Pt. Drain Temp. °F \_\_\_\_\_
- 69. 3rd Pt. Drain Temp. °F \_\_\_\_\_
- 70. 4th Pt. Drain Temp. °F \_\_\_\_\_
- 71. 5th Pt. Drain Temp. °F \_\_\_\_\_
- 72. Vars - Mvar \_\_\_\_\_
- 73. Generator Voltage - K volts \_\_\_\_\_
- 74. Auxiliary Steam Uses: \_\_\_\_\_
- 75. Remarks: \_\_\_\_\_

LANGFORD  
CRO Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: SIX

TIME: 1600-1700

DATE: 7-14-99

- ① Gross Generation - MWH 73.264
- ② Station Service - MWH 4.000
- ③ Net Generation - MWH 69.264
- ④ Control Valve Position % 88%
- ⑤ Main Steam Flow Lbs./Hr. 447,000
- ⑥ F.W. Flow Lbs./Hr. 471,000
- ⑦ F.W. Press. Psig 1530
- 8. Chart Throttle Press. Psig \_\_\_\_\_
- 9. Test Gauge Throttle Press. Psig \_\_\_\_\_
- ⑩ First Stage Press. Psig 980
- ⑪ Cold Reheat Press. Psig 346
- ⑫ Hot Reheat Press. Psig 320
- ⑬ F.W. (Loading/Temp.) 46%
- ⑭ Main Steam Temp. °F 990
- ⑮ Cold Reheat Temp. °F 639
- ⑯ Hot Reheat Temp. °F 960
- ⑰ Superheat Spray Flow \_\_\_\_\_
- ⑱ Reheat Spray Flow \_\_\_\_\_
- ⑲ Air Flow 510,000
- ⑳ Excess Oxygen % 3.1%
- ㉑ Inlet Air Temp. °F 131
- ㉒ Gas Outlet Temp. °F 281
- 23. Opacity % 10.6%
- ㉔ I.D. Fan (Loading/Amps) 62% 156
- ㉕ F.D. Fan (Loading/rpm/Amps) 27% 85
- ㉖ Air Heater Press. (H2O)
- |     |             |             |             |
|-----|-------------|-------------|-------------|
|     | <u>IN</u>   | <u>OUT</u>  | <u>P</u>    |
| AIR | <u>5.75</u> | <u>1.8</u>  | <u>3.95</u> |
| GAS | <u>-2.8</u> | <u>-7.4</u> | <u>4.6</u>  |
- 27. Burner Tilt Position/RH P \_\_\_\_\_
- 28. Condensate Pump Amps A. \_\_\_\_\_ B. \_\_\_\_\_
- 29. Boiler Feed Pump Amps A. \_\_\_\_\_ B. \_\_\_\_\_  
C. \_\_\_\_\_
- 30. Coal Feeder Loading A. \_\_\_\_\_ B. \_\_\_\_\_  
C. \_\_\_\_\_ D. \_\_\_\_\_
- 31. Pulverizer Amps A. \_\_\_\_\_ B. \_\_\_\_\_  
C. \_\_\_\_\_ D. \_\_\_\_\_
- 32. Mill Outage Temp. A. \_\_\_\_\_ B. \_\_\_\_\_  
C. \_\_\_\_\_ D. \_\_\_\_\_
- ③③ Coal Scale Readings:

	Beginning	Ending	Total
a	<u>367957</u>	<u>368121</u>	<u>164</u>
b	<u>564558</u>	<u>564715</u>	<u>157</u>
c	<u>207448</u>	<u>207606</u>	<u>158</u>
d	<u>838049</u>	<u>838200</u>	<u>151</u>

- ③④ Coal Total Lbs. Hr. 63,000

- ③⑤ Lbs. Coal/Net KWH .910
- ③⑥ Lbs. Steam/Net KWH 6454
- 38. Barometric Press. In.Hg \_\_\_\_\_
- 39. Vacuum In.Hg \_\_\_\_\_
- 40. Back Press. In.Hg \_\_\_\_\_
- 41. Circ. Water Pump Amps A. \_\_\_\_\_ B. \_\_\_\_\_  
N or W S or E
- 42. Circ. Water Inlet Temp. °F \_\_\_\_\_
- 43. Circ. Water Outlet Temp °F \_\_\_\_\_
- 44. Circ. Water Inlet Press. Psig \_\_\_\_\_
- 45. Circ. Water Outlet Press. Psig \_\_\_\_\_
- 46. Condensate Make-up \_\_\_\_\_
- 47. Condensate Draw-off \_\_\_\_\_
- 48. Hot Well Temp. °F \_\_\_\_\_
- 49. Turbine Exhaust Temp. °F \_\_\_\_\_
- 50. 1st Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 51. 1st Pt.Htr.Ext.Temp. °F \_\_\_\_\_
- 52. 1st Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 53. 2nd Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 54. 2nd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 55. 2nd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 56. 3rd Pt.Htr.Ext. Press. Psig \_\_\_\_\_
- 57. 3rd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 58. 3rd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 59. 4th Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 60. 4th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 61. 4th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 62. 5th Pt.Htr.Ext. Press.In.Hg \_\_\_\_\_
- 63. 5th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 64. 5th Pt.Htr.F.W.In Temp. °F \_\_\_\_\_
- 65. 5th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 66. 1st Pt.F.W.Out Temp.Minus(-)  
5th Pt.F.W. In Temp. °F = \_\_\_\_\_
- 67. 1st Pt. Drain Temp. °F \_\_\_\_\_
- 68. 2nd Pt. Drain Temp. °F \_\_\_\_\_
- 69. 3rd Pt. Drain Temp. °F \_\_\_\_\_
- 70. 4th Pt. Drain Temp. °F \_\_\_\_\_
- 71. 5th Pt. Drain Temp. °F \_\_\_\_\_
- 72. Vars - Mvar \_\_\_\_\_
- 73. Generator Voltage - K volts \_\_\_\_\_
- 74. Auxiliary Steam Uses: \_\_\_\_\_
- 75. Remarks: \_\_\_\_\_

LANGFORD  
CRO Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: 6

TIME: 9:00-10:00

DATE: 7-15-99

- |     |  |                           |     |                                   |                      |
|-----|--|---------------------------|-----|-----------------------------------|----------------------|
| ①   | Gross Generation - MWH                       | <u>DEFECTED</u>           | ③⑤  | Lbs. Coal/Net KWH                 | <u>920.32</u>        |
| ②   | Station Service - MWH                        |                           | ③⑥  | Lbs. Steam/Net KWH                | <u>.6697</u>         |
| ③   | Net Generation - MWH                         | <u>69.432</u>             | 38. | Barometric Press. In.Hg           |                      |
| ④   | Control Valve Position %                     | <u>88%</u>                | 39. | Vacuum In.Hg                      |                      |
| ⑤   | Main Steam Flow Lbs./Hr.                     | <u>465,000</u>            | 40. | Back Press. In.Hg                 |                      |
| ⑥   | F.W. Flow Lbs./Hr.                           | <u>490,000</u>            | 41. | Circ. Water Pump Amps             | A _____ B _____      |
| ⑦   | F.W. Press. Psig                             | <u>1620</u>               |     |                                   | <u>N or W S or E</u> |
| 8.  | Chart Throttle Press. Psig                   | <u>1451</u>               | 42. | Circ. Water Inlet Temp. °F        |                      |
| 9.  | Test Gauge Throttle Press. Psig              | <u>1450</u>               | 43. | Circ. Water Outlet Temp °F        |                      |
| ⑩   | First Stage Press. Psig                      | <u>970</u>                | 44. | Circ. Water Inlet Press. Psig     |                      |
| ⑪   | Cold Reheat Press. Psig                      | <u>350</u>                | 45. | Circ. Water Outlet Press. Psig    |                      |
| ⑫   | Hot Reheat Press. Psig                       | <u>330</u>                | 46. | Condensate Make-up                |                      |
| ⑬   | F.W. (Loading/Temp.)                         | <u>45 398</u>             | 47. | Condensate Draw-off               |                      |
| ⑭   | Main Steam Temp. °F                          | <u>1000°</u>              | 48. | Hot Well Temp. °F                 |                      |
| ⑮   | Cold Reheat Temp. °F                         | <u>650</u>                | 49. | Turbine Exhaust Temp. °F          |                      |
| ⑯   | Hot Reheat Temp. °F                          | <u>980°</u>               | 50. | 1st Pt.Htr.Ext.Press. Psig        |                      |
| ⑰   | Superheat Spray Flow                         | <u>0</u>                  | 51. | 1st Pt.Htr.Ext.Temp. °F           |                      |
| ⑱   | Reheat Spray Flow                            | <u>0</u>                  | 52. | 1st Pt.Htr.F.W.Out Temp. °F       |                      |
| ⑲   | Air Flow                                     | <u>520,000</u>            | 53. | 2nd Pt.Htr.Ext.Press. Psig        |                      |
| ⑳   | Excess Oxygen %                              | <u>3.2%</u>               | 54. | 2nd Pt.Htr.Ext. Temp. °F          |                      |
| ㉑   | Inlet Air Temp. °F                           | <u>130°</u>               | 55. | 2nd Pt.Htr.F.W.Out Temp. °F       |                      |
| ㉒   | Gas Outlet Temp. °F                          | <u>280°</u>               | 56. | 3rd Pt.Htr.Ext. Press. Psig       |                      |
| 23. | Opacity %                                    | <u>11.8</u>               | 57. | 3rd Pt.Htr.Ext. Temp. °F          |                      |
| ⑳   | I.D. Fan (Loading/Amps)                      | <u>64 160</u>             | 58. | 3rd Pt.Htr.F.W.Out Temp. °F       |                      |
| ㉕   | F.D. Fan (Loading/rpm/Amps)                  | <u>63 87</u>              | 59. | 4th Pt.Htr.Ext.Press. Psig        |                      |
| ㉖   | Air Heater Press. (H2O)                      |                           | 60. | 4th Pt.Htr.Ext. Temp. °F          |                      |
|     | IN OUT P                                     |                           | 61. | 4th Pt.Htr.F.W.Out Temp. °F       |                      |
|     | AIR <u>6.0</u> <u>2.0</u> <u>4.0</u>         |                           | 62. | 5th Pt.Htr.Ext. Press.In.Hg       |                      |
|     | GAS <u>3</u> <u>2.5</u> <u>4.5</u>           |                           | 63. | 5th Pt.Htr.Ext. Temp. °F          |                      |
| 27. | Burner Tilt Position/RH P                    | <u>N/A</u>                | 64. | 5th Pt.Htr.F.W.In Temp. °F        |                      |
| 28. | Condensate Pump Amps                         | A <u>107</u> B <u>111</u> | 65. | 5th Pt.Htr.F.W.Out Temp. °F       |                      |
| 29. | Boiler Feed Pump Amps                        | A <u>190</u> B <u>202</u> | 66. | 1st Pt.F.W.Out Temp.Minus(-)      |                      |
|     | C _____                                      |                           |     | 5th Pt.F.W. In Temp. °F =         |                      |
| 30. | Coal Feeder Loading                          | A <u>65</u> B <u>65</u>   | 67. | 1st Pt. Drain Temp. °F            |                      |
|     | C <u>65</u> D <u>65</u>                      |                           | 68. | 2nd Pt. Drain Temp. °F            |                      |
| 31. | Pulverizer Amps                              | A <u>51</u> B <u>50</u>   | 69. | 3rd Pt. Drain Temp. °F            |                      |
|     | C <u>50</u> D <u>42</u>                      |                           | 70. | 4th Pt. Drain Temp. °F            |                      |
| 32. | Mill Outage Temp.                            | A <u>170</u> B <u>180</u> | 71. | 5th Pt. Drain Temp. °F            |                      |
|     | C <u>178</u> D <u>180</u>                    |                           | 72. | Vars - Mvar                       |                      |
| ③③  | Coal Scale Readings:                         |                           | 73. | Generator Voltage - K volts       |                      |
|     | Beginning Ending Total                       |                           | 74. | Auxiliary Steam Uses:             |                      |
|     | a <u>370551</u>   <u>370716</u>   <u>165</u> |                           | 75. | Remarks: <u>Unit #6 Gross</u>     |                      |
|     | b <u>567042</u>   <u>567199</u>   <u>157</u> |                           |     | <u>Generation with hour meter</u> |                      |
|     | c <u>209943</u>   <u>210102</u>   <u>159</u> |                           |     | <u>reading high (defected)</u>    |                      |
|     | d <u>840535</u>   <u>840693</u>   <u>158</u> |                           |     |                                   |                      |
| ③④  | Coal Total Lbs. Hr.                          | <u>63,900</u>             |     |                                   |                      |

Jim Davey CRO      Todd Papavi Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: 6

TIME: 1000-1100

DATE: 7-15-99

- ① Gross Generation - MWH Defected
- ② Station Service - MWH \_\_\_\_\_
- ③ Net Generation - MWH 69.264
- ④ Control Valve Position % 87%
- ⑤ Main Steam Flow Lbs./Hr. 470,000
- ⑥ F.W. Flow Lbs./Hr. 480,000
- ⑦ F.W. Press. Psig 1600
- 8. Chart Throttle Press. Psig 1450
- 9. Test Gauge Throttle Press. Psig 1450
- ⑩ First Stage Press. Psig 980
- ⑪ Cold Reheat Press. Psig 349
- ⑫ Hot Reheat Press. Psig 330
- ⑬ F.W. (Loading/Temp.) 46 398
- ⑭ Main Steam Temp. °F 1000
- ⑮ Cold Reheat Temp. °F 647
- ⑯ Hot Reheat Temp. °F 980
- ⑰ Superheat Spray Flow 0
- ⑱ Reheat Spray Flow 0
- ⑲ Air Flow 520,000
- ⑳ Excess Oxygen % 3.2%
- ㉑ Inlet Air Temp. °F 130
- ㉒ Gas Outlet Temp. °F 280
- 23. Opacity % 13%
- ㉔ I.D. Fan (Loading/Amps) 64 160
- ㉕ F.D. Fan (Loading/rpm/Amps) 87 92
- ㉖ Air Heater Press. (H2O)
- IN                      OUT                      P
- AIR 6.0                      2.0                      4.0
- GAS 3.0                      7.5                      4.5
- 27. Burner Tilt Position/RH P N/A
- 28. Condensate Pump Amps A106 B112
- 29. Boiler Feed Pump Amps A190 B203
- C \_\_\_\_\_
- 30. Coal Feeder Loading A66 B66
- C 65 D 65
- 31. Pulverizer Amps A52 B50
- C 50 D 42
- 32. Mill Outage Temp. A170 B180
- C 176 D 181
- ③③ Coal Scale Readings:
- Beginning                      Ending                      Total
- a 370716 | 370882 | 166
- b 567199 | 567358 | 159
- c 210102 | 210261 | 159
- d 840693 | 840853 | 160
- ③④ Coal Total Lbs. Hr. 64,400

- ③⑤ Lbs. Coal/Net KWH 929.77
- ③⑥ Lbs. Steam/Net KWH 16785
- 38. Barometric Press. In.Hg \_\_\_\_\_
- 39. Vacuum In.Hg \_\_\_\_\_
- 40. Back Press. In.Hg \_\_\_\_\_
- 41. Circ. Water Pump Amps A \_\_\_\_\_ B \_\_\_\_\_  
N or W S or E
- 42. Circ. Water Inlet Temp. °F \_\_\_\_\_
- 43. Circ. Water Outlet Temp °F \_\_\_\_\_
- 44. Circ. Water Inlet Press. Psig \_\_\_\_\_
- 45. Circ. Water Outlet Press. Psig \_\_\_\_\_
- 46. Condensate Make-up \_\_\_\_\_
- 47. Condensate Draw-off \_\_\_\_\_
- 48. Hot Well Temp. °F \_\_\_\_\_
- 49. Turbine Exhaust Temp. °F \_\_\_\_\_
- 50. 1st Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 51. 1st Pt.Htr.Ext.Temp. °F \_\_\_\_\_
- 52. 1st Pt.Htr.F.W.Out Temp °F \_\_\_\_\_
- 53. 2nd Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 54. 2nd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 55. 2nd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 56. 3rd Pt.Htr.Ext. Press. Psig \_\_\_\_\_
- 57. 3rd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 58. 3rd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 59. 4th Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 60. 4th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 61. 4th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 62. 5th Pt.Htr.Ext. Press.In.Hg \_\_\_\_\_
- 63. 5th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 64. 5th Pt.Htr.F.W.In Temp. °F \_\_\_\_\_
- 65. 5th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 66. 1st Pt.F.W.Out Temp.Minus(-)  
5th Pt.F.W. In Temp. °F = \_\_\_\_\_
- 67. 1st Pt. Drain Temp. °F \_\_\_\_\_
- 68. 2nd Pt. Drain Temp. °F \_\_\_\_\_
- 69. 3rd Pt. Drain Temp. °F \_\_\_\_\_
- 70. 4th Pt. Drain Temp. °F \_\_\_\_\_
- 71. 5th Pt. Drain Temp. °F \_\_\_\_\_
- 72. Vars - Mvar \_\_\_\_\_
- 73. Generator Voltage - K volts \_\_\_\_\_
- 74. Auxiliary Steam Uses: \_\_\_\_\_
- 75. Remarks: Unit #6 Gross Generation  
with hour meter reading  
high (defected).

Jim Davley                      Todd Rapawi  
CRO                                      Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: 6

TIME: 11:00-1200

DATE: 7-15-99

① Gross Generation - MWH Defected  
 ② Station Service - MWH \_\_\_\_\_  
 ③ Net Generation - MWH 69.240  
 ④ Control Valve Position % 88.1  
 ⑤ Main Steam Flow Lbs./Hr. 475,000  
 ⑥ F.W. Flow Lbs./Hr. 483,000  
 ⑦ F.W. Press. Psig 1590  
 8. Chart Throttle Press. Psig 1457  
 9. Test Gauge Throttle Press. Psig 1450  
 ⑩ First Stage Press. Psig 980  
 ⑪ Cold Reheat Press. Psig 349  
 ⑫ Hot Reheat Press. Psig 330  
 ⑬ F.W. (Loading/Temp.) 46399  
 ⑭ Main Steam Temp. °F 1000  
 ⑮ Cold Reheat Temp. °F 648  
 ⑯ Hot Reheat Temp. °F 985  
 ⑰ Superheat Spray Flow 0  
 ⑱ Reheat Spray Flow 0  
 ⑲ Air Flow 520,000  
 ⑳ Excess Oxygen % 3.2%  
 ㉑ Inlet Air Temp. °F 130  
 ㉒ Gas Outlet Temp. °F 280  
 23. Opacity % 11%  
 ㉔ I.D. Fan (Loading/Amps) 64160  
 ㉕ F.D. Fan (Loading/rpm/Amps) 8792  
 ㉖ Air Heater Press. (H2O)  
     IN                    OUT                    P  
 AIR 6.0                    2.0                    4.0  
 GAS (-13.0)                    (-7.5)                    4.5  
 27. Burner Tilt Position/RH P N/A  
 28. Condensate Pump Amps A 106 B 111  
 29. Boiler Feed Pump Amps A 190 B 203  
     C  
 30. Coal Feeder Loading A 66 B 66  
     C 65 D 65  
 31. Pulverizer Amps A 52 B 50  
     C 50 D 42  
 32. Mill Outage Temp. A 170 B 180  
     C 176 D 181  
 ③③ Coal Scale Readings:  
     Beginning            Ending            Total  
 a 370882 | 371048 | 166  
 b 567358 | 567518 | 160  
 c 210261 | 210422 | 161  
 d 840853 | 841013 | 160  
 ③④ Coal Total Lbs. Hr. 64,700

③⑤ Lbs. Coal/Net KWH 934.43  
 ③⑥ Lbs. Steam/Net KWH 6.860  
 38. Barometric Press. In.Hg \_\_\_\_\_  
 39. Vacuum In.Hg \_\_\_\_\_  
 40. Back Press. In.Hg \_\_\_\_\_  
 41. Circ. Water Pump Amps A B  
     N or W S or E  
 42. Circ. Water Inlet Temp. °F \_\_\_\_\_  
 43. Circ. Water Outlet Temp °F \_\_\_\_\_  
 44. Circ. Water Inlet Press. Psig \_\_\_\_\_  
 45. Circ. Water Outlet Press. Psig \_\_\_\_\_  
 46. Condensate Make-up \_\_\_\_\_  
 47. Condensate Draw-off \_\_\_\_\_  
 48. Hot Well Temp. °F \_\_\_\_\_  
 49. Turbine Exhaust Temp. °F \_\_\_\_\_  
 50. 1st Pt.Htr.Ext.Press. Psig \_\_\_\_\_  
 51. 1st Pt.Htr.Ext.Temp. °F \_\_\_\_\_  
 52. 1st Pt.Htr.F.W.Out Temp °F \_\_\_\_\_  
 53. 2nd Pt.Htr.Ext.Press. Psig \_\_\_\_\_  
 54. 2nd Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 55. 2nd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 56. 3rd Pt.Htr.Ext. Press. Psig \_\_\_\_\_  
 57. 3rd Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 58. 3rd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 59. 4th Pt.Htr.Ext.Press. Psig \_\_\_\_\_  
 60. 4th Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 61. 4th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 62. 5th Pt.Htr.Ext. Press.In.Hg \_\_\_\_\_  
 63. 5th Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 64. 5th Pt.Htr.F.W.In Temp. °F \_\_\_\_\_  
 65. 5th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 66. 1st Pt.F.W.Out Temp.Minus(-)  
     5th Pt.F.W. In Temp. °F = \_\_\_\_\_  
 67. 1st Pt. Drain Temp. °F \_\_\_\_\_  
 68. 2nd Pt. Drain Temp. °F \_\_\_\_\_  
 69. 3rd Pt. Drain Temp. °F \_\_\_\_\_  
 70. 4th Pt. Drain Temp. °F \_\_\_\_\_  
 71. 5th Pt. Drain Temp. °F \_\_\_\_\_  
 72. Vars - Mvar \_\_\_\_\_  
 73. Generator Voltage - K volts \_\_\_\_\_  
 74. Auxiliary Steam Uses: \_\_\_\_\_  
 75. Remarks: Unit # 6 Gross  
     Generation with hour meter  
     reading high (deflected)

Jim Davey CRO  
Todd Papari Engineer



PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: 6 TIME: 13:00-14:00 DATE: 7-15-99

- |     |   |                           |     |                                       |   |
|-----|---|---------------------------|-----|---------------------------------------|---|
| ①   | Gross Generation - MWH                        | <u>Defected</u>           | ③⑤  | Lbs. Coal/Net KWH                     | <u>924.47</u>                           |
| ②   | Station Service - MWH                         | <u>0</u>                  | ③⑥  | Lbs. Steam/Net KWH                    | <u>6872</u>                             |
| ③   | Net Generation - MWH                          | <u>69.120</u>             | 38. | Barometric Press. In.Hg               | <u>          </u>                       |
| ④   | Control Valve Position %                      | <u>88</u>                 | 39. | Vacuum In.Hg                          | <u>          </u>                       |
| ⑤   | Main Steam Flow Lbs./Hr.                      | <u>475,000</u>            | 40. | Back Press. In.Hg                     | <u>          </u>                       |
| ⑥   | F.W. Flow Lbs./Hr.                            | <u>480,000</u>            | 41. | Circ. Water Pump Amps                 | A <u>          </u> B <u>          </u> |
| ⑦   | F.W. Press. Psig                              | <u>1590</u>               |     |                                       | N or W S or E <u>          </u>         |
| 8.  | Chart Throttle Press. Psig                    | <u>1445</u>               | 42. | Circ. Water Inlet Temp. °F            | <u>          </u>                       |
| 9.  | Test Gauge Throttle Press. Psig               | <u>1450</u>               | 43. | Circ. Water Outlet Temp °F            | <u>          </u>                       |
| ⑩   | First Stage Press. Psig                       | <u>980</u>                | 44. | Circ. Water Inlet Press. Psig         | <u>          </u>                       |
| ⑪   | Cold Reheat Press. Psig                       | <u>349</u>                | 45. | Circ. Water Outlet Press. Psig        | <u>          </u>                       |
| ⑫   | Hot Reheat Press. Psig                        | <u>330</u>                | 46. | Condensate Make-up                    | <u>          </u>                       |
| ⑬   | F.W. (Loading/Temp.)                          | <u>47 398</u>             | 47. | Condensate Draw-off                   | <u>          </u>                       |
| ⑭   | Main Steam Temp. °F                           | <u>1000°</u>              | 48. | Hot Well Temp. °F                     | <u>          </u>                       |
| ⑮   | Cold Reheat Temp. °F                          | <u>637</u>                | 49. | Turbine Exhaust Temp. °F              | <u>          </u>                       |
| ⑯   | Hot Reheat Temp. °F                           | <u>985</u>                | 50. | 1st Pt.Htr.Ext.Press. Psig            | <u>          </u>                       |
| ⑰   | Superheat Spray Flow                          | <u>0</u>                  | 51. | 1st Pt.Htr.Ext.Temp. °F               | <u>          </u>                       |
| ⑱   | Reheat Spray Flow                             | <u>0</u>                  | 52. | 1st Pt.Htr.F.W.Out Temp °F            | <u>          </u>                       |
| ⑲   | Air Flow                                      | <u>518,000</u>            | 53. | 2nd Pt.Htr.Ext.Press. Psig            | <u>          </u>                       |
| ⑳   | Excess Oxygen %                               | <u>3.1%</u>               | 54. | 2nd Pt.Htr.Ext. Temp. °F              | <u>          </u>                       |
| ㉑   | Inlet Air Temp. °F                            | <u>130</u>                | 55. | 2nd Pt.Htr.F.W.Out Temp. °F           | <u>          </u>                       |
| ㉒   | Gas Outlet Temp. °F                           | <u>280</u>                | 56. | 3rd Pt.Htr.Ext. Press. Psig           | <u>          </u>                       |
| 23. | Opacity %                                     | <u>13%</u>                | 57. | 3rd Pt.Htr.Ext. Temp. °F              | <u>          </u>                       |
| ⑳   | I.D. Fan (Loading/Amps)                       | <u>64 760</u>             | 58. | 3rd Pt.Htr.F.W.Out Temp. °F           | <u>          </u>                       |
| ㉕   | F.D. Fan (Loading/rpm/Amps)                   | <u>87 90</u>              | 59. | 4th Pt.Htr.Ext.Press. Psig            | <u>          </u>                       |
| ㉖   | Air Heater Press. (H2O)                       | <u>          </u>         | 60. | 4th Pt.Htr.Ext. Temp. °F              | <u>          </u>                       |
|     | IN OUT P                                      |                           | 61. | 4th Pt.Htr.F.W.Out Temp. °F           | <u>          </u>                       |
|     | AIR <u>6.0</u> <u>2.0</u> <u>4.0</u>          |                           | 62. | 5th Pt.Htr.Ext. Press.In.Hg           | <u>          </u>                       |
|     | GAS (-) <u>13.0</u> (-) <u>7.5</u> <u>4.5</u> |                           | 63. | 5th Pt.Htr.Ext. Temp. °F              | <u>          </u>                       |
| 27. | Burner Tilt Position/RH P                     | <u>N/A</u>                | 64. | 5th Pt.Htr.F.W.In Temp. °F            | <u>          </u>                       |
| 28. | Condensate Pump Amps                          | A <u>106</u> B <u>112</u> | 65. | 5th Pt.Htr.F.W.Out Temp. °F           | <u>          </u>                       |
| 29. | Boiler Feed Pump Amps                         | A <u>192</u> B <u>202</u> | 66. | 1st Pt.F.W.Out Temp.Minus(-)          | <u>          </u>                       |
|     | C <u>          </u>                           |                           |     | 5th Pt.F.W. In Temp. °F -             | <u>          </u>                       |
| 30. | Coal Feeder Loading                           | A <u>66</u> B <u>66</u>   | 67. | 1st Pt. Drain Temp. °F                | <u>          </u>                       |
|     | C <u>65</u> D <u>65</u>                       |                           | 68. | 2nd Pt. Drain Temp. °F                | <u>          </u>                       |
| 31. | Pulverizer Amps                               | A <u>52</u> B <u>50</u>   | 69. | 3rd Pt. Drain Temp. °F                | <u>          </u>                       |
|     | C <u>50</u> D <u>42</u>                       |                           | 70. | 4th Pt. Drain Temp. °F                | <u>          </u>                       |
| 32. | Mill Outage Temp.                             | A <u>170</u> B <u>180</u> | 71. | 5th Pt. Drain Temp. °F                | <u>          </u>                       |
|     | C <u>176</u> D <u>181</u>                     |                           | 72. | Vars - Mvar                           | <u>          </u>                       |
| ③③  | Coal Scale Readings:                          |                           | 73. | Generator Voltage - K volts           | <u>          </u>                       |
|     | Beginning Ending Total                        |                           | 74. | Auxiliary Steam Uses:                 | <u>          </u>                       |
|     | a <u>371214</u>   <u>371378</u>   <u>164</u>  |                           | 75. | Remarks: <u>Gross generation with</u> |   |
|     | b <u>567676</u>   <u>567834</u>   <u>158</u>  |                           |     | <u>hour meter reading high</u>        |   |
|     | c <u>210580</u>   <u>210739</u>   <u>159</u>  |                           |     | <u>(defected)</u>                     |   |
|     | d <u>841171</u>   <u>841329</u>   <u>158</u>  |                           |     |                                       |   |
| ③④  | Coal Total Lbs. Hr.                           | <u>63,900</u>             |     |                                       |   |

Jim Davy CRO      Todd Papavi Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

UNIT NO.: 6

TIME: 14:00-1500

DATE: 7-15-99

- ① Gross Generation - MWH Defected
- ② Station Service - MWH \_\_\_\_\_
- ③ Net Generation - MWH 69,230
- ④ Control Valve Position % 88%
- ⑤ Main Steam Flow Lbs./Hr. 475,000
- ⑥ F.W. Flow Lbs./Hr. 480,000
- ⑦ F.W. Press. Psig 1590
- 8. Chart Throttle Press. Psig 1448
- 9. Test Gauge Throttle Press. Psig 1450
- ⑩ First Stage Press. Psig 980
- ⑪ Cold Reheat Press. Psig 349
- ⑫ Hot Reheat Press. Psig 330
- ⑬ F.W. (Loading/Temp.) 47 398
- ⑭ Main Steam Temp. °F 1000°
- ⑮ Cold Reheat Temp. °F 637
- ⑯ Hot Reheat Temp. °F 985
- ⑰ Superheat Spray Flow 0
- ⑱ Reheat Spray Flow 0
- ⑲ Air Flow 518,000
- ⑳ Excess Oxygen % 3.1%
- ㉑ Inlet Air Temp. °F 130
- ㉒ Gas Outlet Temp. °F 280
- 23. Opacity % 14%
- ㉔ I.D. Fan (Loading/Amps) 64 160
- ㉕ F.D. Fan (Loading/rpm/Amps) 87 90
- ㉖ Air Heater Press. (H2O)
- IN                      OUT                      P
- AIR 6.0                      2.0                      4.0
- GAS (-7) 13.0                      (-7) 7.5                      4.5
- 27. Burner Tilt Position/RH P N/A
- 28. Condensate Pump Amps A 106 B 112
- 29. Boiler Feed Pump Amps A 192 B 202
- C \_\_\_\_\_
- 30. Coal Feeder Loading A 66 B 66
- C 65 D 65
- 31. Pulverizer Amps A 52 B 50
- C 50 D 42
- 32. Mill Outage Temp. A 170 B 180
- C 176 D 181
- ③③ Coal Scale Readings:
- Beginning      Ending      Total
- a 371378      371564      166
- b 567834      568012      158
- c 210739      210917      160
- d 841329      841508      158
- ③④ Coal Total Lbs. Hr. 64,200

- ③⑤ Lbs. Coal/Net KWH 927.34
- ③⑥ Lbs. Steam/Net KWH .6861
- 38. Barometric Press. In.Hg \_\_\_\_\_
- 39. Vacuum In.Hg \_\_\_\_\_
- 40. Back Press. In.Hg \_\_\_\_\_
- 41. Circ. Water Pump Amps A \_\_\_\_\_ B \_\_\_\_\_
- N or W S or E
- 42. Circ. Water Inlet Temp. °F \_\_\_\_\_
- 43. Circ. Water Outlet Temp °F \_\_\_\_\_
- 44. Circ. Water Inlet Press. Psig \_\_\_\_\_
- 45. Circ. Water Outlet Press. Psig \_\_\_\_\_
- 46. Condensate Make-up \_\_\_\_\_
- 47. Condensate Draw-off \_\_\_\_\_
- 48. Hot Well Temp. °F \_\_\_\_\_
- 49. Turbine Exhaust Temp. °F \_\_\_\_\_
- 50. 1st Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 51. 1st Pt.Htr.Ext.Temp. °F \_\_\_\_\_
- 52. 1st Pt.Htr.F.W.Out Temp °F \_\_\_\_\_
- 53. 2nd Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 54. 2nd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 55. 2nd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 56. 3rd Pt.Htr.Ext. Press. Psig \_\_\_\_\_
- 57. 3rd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 58. 3rd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 59. 4th Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 60. 4th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 61. 4th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 62. 5th Pt.Htr.Ext. Press.In.Hg \_\_\_\_\_
- 63. 5th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 64. 5th Pt.Htr.F.W.In Temp. °F \_\_\_\_\_
- 65. 5th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 66. 1st Pt.F.W.Out Temp.Minus(-) \_\_\_\_\_
- 5th Pt.F.W. In Temp. °F = \_\_\_\_\_
- 67. 1st Pt. Drain Temp. °F \_\_\_\_\_
- 68. 2nd Pt. Drain Temp. °F \_\_\_\_\_
- 69. 3rd Pt. Drain Temp. °F \_\_\_\_\_
- 70. 4th Pt. Drain Temp. °F \_\_\_\_\_
- 71. 5th Pt. Drain Temp. °F \_\_\_\_\_
- 72. Vars - Mvar \_\_\_\_\_
- 73. Generator Voltage - K volts \_\_\_\_\_
- 74. Auxiliary Steam Uses: \_\_\_\_\_
- 75. Remarks: Unit #6 gross  
Generator with low  
voltage reading high  
(defected)

Jim Davey CRO      Todd Basari Engineer

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**UNIT 6 CEMS DATA**

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Plant Name: PIPP  
 General Average Report

Reporting Period: 07/14/1999 to 07/14/1999

Site Name: PIPPF6P6

Time of Report: 07/19/99 07:43

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/14/99	13:15	11.6	445.4	521.7	315.7	3.3	18.	297.2	74.
	13:16	11.6	444.8	521.0	314.2	3.3	10.	298.3	74.
	13:17	11.6	447.5	522.2	314.3	2.7	12.	298.5	74.
	13:18	11.7	446.6	526.1	315.6	0.5	18.	299.6	74.
	13:19	11.7	444.1	525.8	315.6	1.7	12.	299.6	74.
	13:20	11.7	446.5	524.8	314.5	2.2	13.	300.0	74.
	13:21	11.7	444.7	524.2	313.8	0.0	16.	300.1	75.
	13:22	11.8	442.7	525.1	313.8	0.9	15.	301.6	74.
	13:23	11.6	446.7	519.9	313.8	2.6	11.	301.8	74.
	13:24	11.6	447.2	520.7	314.2	1.5	14.	300.8	74.
	13:25	11.6	446.5	524.9	314.5	1.0	16.	300.0	74.
	13:26	11.7	447.5	527.8	314.4	0.7	14.	298.3	74.
	13:27	11.7	444.0	530.1	314.4	1.0	13.	297.1	74.
	13:28	11.7	444.4	533.0	314.1	0.0	24.	296.2	74.
	13:29	11.7	446.6	530.5	313.6	1.2	24.	294.5	74.
	13:30	11.7	446.8	529.2	313.6	3.6	14.	294.7	74.
	13:31	11.7	447.2	531.6	313.6	1.5	22.	294.9	74.
	13:32	11.6	449.7	526.8	313.6	1.1	11.	294.9	74.
	13:33	11.6	447.3	526.9	313.9	0.0	13.	294.8	74.
	13:34	11.7	444.5	529.2	314.0	2.4	12.	294.2	74.
	13:35	11.7	444.4	529.9	314.4	2.1	19.	292.7	74.
	13:36	11.7	443.7	530.9	314.4	2.4	10.	292.7	74.
	13:37	11.6	446.9	530.6	313.1	1.2	13.	291.6	74.
	13:38	11.6	451.1	528.5	312.9	1.2	16.	291.3	74.
	13:39	11.7	446.7	531.9	314.0	2.9	12.	293.2	74.
	13:40	11.7	446.8	531.9	314.2	0.0	13.	293.5	74.
	13:41	11.7	444.2	532.8	314.0	0.7	19.	294.1	75.
	13:42	11.8	441.8	530.3	313.9	0.0	16.	294.4	74.
	13:43	11.7	444.3	526.7	313.7	1.4	12.	293.4	74.
	13:44	11.6	446.6	525.3	313.6	1.8	14.	293.1	74.
	13:45	11.7	445.5	527.1	313.5	1.8	17.	292.5	74.
	13:46	11.7	447.2	528.6	313.0	1.2	13.	291.3	74.
	13:47	11.7	445.9	527.8	313.2	1.1	10.	291.5	74.
	13:48	11.8	443.2	529.6	313.6	3.1	18.	291.7	74.
	13:49	11.7	443.2	529.2	313.5	0.6	14.	292.3	74.
	13:50	11.6	446.5	524.5	313.2	0.6	11.	295.0	74.
	13:51	11.6	446.4	523.9	313.3	2.3	18.	295.1	74.
	13:52	11.7	445.8	526.0	314.1	1.4	13.	295.2	74.
	13:53	11.7	445.5	527.9	314.1	0.0	14.	295.2	74.
	13:54	11.8	442.5	527.8	315.1	1.2	10.	296.2	74.
	13:55	11.7	443.6	526.1	315.3	3.8	17.	296.3	74.
	13:56	11.6	446.2	524.3	315.0	2.0	12.	296.0	74.
	13:57	11.7	444.7	525.0	315.0	1.3	11.	296.0	74.
	13:58	11.7	446.1	524.8	314.6	2.0	17.	296.4	74.
	13:59	11.7	447.3	524.5	314.4	1.7	11.	296.6	74.
	14:00	11.7	445.2	527.3	314.5	2.5	13.	296.0	74.
	14:01	11.8	443.4	530.2	314.7	1.1	15.	295.6	74.
	14:02	11.7	446.3	527.2	314.7	0.6	15.	295.8	74.
	14:03	11.6	445.4	525.5	314.8	1.7	11.	296.0	74.
	14:04	11.6	444.7	526.5	315.2	2.4	12.	295.9	74.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/14/1999 to 07/14/1999

Site Name: PIPPF6P6  
 Data Averaging Type: 1m

Time of Report: 07/19/99 07:43  
 Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/14/99	14:05	11.6	446.5	528.6	315.7	2.7	17.	295.7	74.
	14:06	11.7	444.3	529.4	315.6	4.7	12.	295.7	74.
	14:07	11.8	441.3	531.0	313.6	3.1	12.	295.6	74.
	14:08	11.7	445.8	529.8	313.7	1.8	13.	295.1	74.
	14:09	11.6	446.5	526.2	315.7	3.4	15.	293.9	74.
	14:10	11.7	445.8	527.5	315.7	1.7	11.	293.9	74.
	14:11	11.7	444.0	529.1	315.0	1.0	14.	295.4	74.
	14:12	11.7	445.2	531.6	314.6	0.5	18.	295.6	74.
	14:13	11.7	443.0	532.1	313.9	3.6	12.	296.0	74.
	14:14	11.8	445.2	534.1	313.9	2.5	10.	296.0	74.
	14:15	11.7	447.7	532.8	315.5	1.3	17.	294.3	74.
	14:16	11.8	443.9	532.3	316.5	2.2	11.	293.9	74.
	14:17	11.7	445.3	531.4	316.3	2.1	15.	292.7	74.
	14:18	11.7	449.5	530.3	316.2	1.3	14.	292.4	74.
	14:19	11.8	443.3	531.1	315.9	3.0	13.	292.4	74.
	14:20	11.8	442.7	532.1	315.7	3.1	11.	292.3	74.
	14:21	11.8	444.3	531.2	315.5	1.8	16.	293.5	74.
	14:22	11.8	443.2	532.8	315.3	3.1	17.	294.2	74.
	14:23	11.7	442.7	529.0	315.3	2.6	13.	294.4	74.
	14:24	11.7	444.8	526.0	315.7	2.3	11.	295.9	74.
	14:25	11.7	444.8	524.3	315.5	1.5	20.	296.0	74.
	14:26	11.7	445.1	524.7	315.0	1.4	11.	296.3	74.
	14:27	11.7	447.8	529.5	315.0	0.7	12.	296.1	74.
	14:28	11.7	447.4	527.4	314.9	0.0	14.	294.9	74.
	14:29	11.7	444.9	528.1	314.8	3.0	15.	294.8	74.
	14:30	11.7	446.1	526.9	314.3	2.9	13.	293.8	74.
	14:31	11.7	450.2	526.1	314.2	2.5	16.	293.8	74.
	14:32	11.8	448.5	530.4	314.3	1.5	18.	293.2	74.
	14:33	11.8	448.7	530.7	314.4	2.9	13.	293.0	74.
	14:34	11.7	449.3	528.0	315.4	3.7	11.	293.4	74.
	14:35	11.7	448.5	529.6	315.7	1.8	15.	293.5	74.
	14:36	11.7	449.1	525.6	315.2	1.5	12.	293.1	74.
	14:37	11.7	449.5	526.1	314.7	1.7	12.	292.7	74.
	14:38	11.7	448.5	528.9	314.8	2.3	15.	292.7	74.
	14:39	11.8	446.6	532.3	315.0	1.8	13.	292.7	74.
	14:40	11.8	447.0	531.5	315.0	2.6	12.	292.7	74.
	14:41	11.8	446.5	531.3	315.1	2.7	13.	292.7	75.
	14:42	11.8	445.8	534.6	315.4	1.9	23.	292.6	74.
	14:43	11.8	447.8	534.2	315.9	3.3	10.	292.4	74.
	14:44	11.7	451.0	530.0	315.9	4.7	14.	292.4	74.
	14:45	11.7	449.8	530.2	315.5	1.4	18.	292.4	74.
	14:46	11.7	449.8	530.8	315.5	3.4	13.	292.2	74.
	14:47	11.8	450.1	532.4	315.6	2.6	11.	290.8	74.
	14:48	11.8	450.4	534.9	315.6	0.7	17.	290.8	74.
	14:49	11.9	448.4	537.8	314.9	1.1	13.	290.4	75.
	14:50	11.9	444.0	538.6	314.7	3.1	13.	290.2	74.
	14:51	11.8	449.4	536.7	315.3	2.6	12.	290.2	74.
	14:52	11.7	451.5	531.0	315.4	0.0	18.	290.2	74.
	14:53	11.7	450.3	530.1	315.4	2.7	15.	292.2	74.
	14:54	11.7	450.5	530.1	315.3	1.7	10.	293.7	74.

## General Average Report

Reporting Period: 07/14/1999 to 07/14/1999

Site Name: PIPPF6P6

Time of Report: 07/19/99 07:43

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OFC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/14/99	14:55	11.7	450.7	531.1	315.3	1.7	17.	294.8	74.
	14:56	11.8	448.7	535.3	315.3	3.9	11.	295.5	74.
	14:57	11.8	449.1	535.9	315.5	2.6	12.	294.9	74.
	14:58	11.8	448.7	534.5	315.7	4.2	13.	294.1	74.
	14:59	11.7	450.7	531.0	315.7	3.1	14.	293.5	74.
	15:00	11.8	448.3	535.0	315.7	1.0	12.	292.4	74.
	15:01	11.8	450.3	535.3	315.7	2.1	13.	292.5	74.
	15:02	11.8	450.0	536.0	315.4	2.0	18.	293.0	74.
	15:03	11.8	450.1	535.0	315.0	3.4	11.	292.8	74.
	15:04	11.8	447.7	532.6	313.8	3.0	12.	292.3	74.
	15:05	11.8	451.1	529.1	313.8	4.3	18.	292.3	74.
	15:06	11.8	450.7	532.5	315.2	2.6	11.	292.6	74.
	15:07	11.8	448.6	530.6	315.4	1.7	13.	292.6	74.
	15:08	11.7	450.5	528.6	315.3	4.1	13.	289.3	74.
	15:09	11.7	453.2	527.6	315.3	2.4	16.	289.3	74.
	15:10	11.7	452.8	527.3	315.9	2.1	9.	289.2	74.
	15:11	11.7	452.5	529.5	316.2	2.8	12.	289.1	74.
	15:12	11.8	450.5	530.6	315.5	4.4	22.	289.4	74.
	15:13	11.8	453.9	532.6	315.3	1.7	12.	289.5	74.
	15:14	11.8	450.4	533.8	315.7	1.9	14.	290.5	74.
	15:15	11.9	450.3	534.0	316.5	3.3	18.	292.2	74.
	15:16	11.8	450.6	533.8	316.5	4.1	13.	292.3	74.
	15:17	11.8	449.3	531.0	316.5	2.9	11.	292.7	74.
	15:18	11.7	451.2	527.6	316.5	3.2	15.	292.7	74.
	15:19	11.7	452.8	529.3	316.0	3.0	14.	293.2	74.
	15:20	11.8	451.5	532.3	316.1	2.7	14.	293.0	74.
	15:21	11.8	448.8	533.3	316.5	3.7	12.	292.3	74.
	15:22	11.8	449.8	533.5	316.5	2.4	20.	292.3	74.
	15:23	11.8	451.2	531.0	315.7	3.6	10.	291.9	74.
	15:24	11.8	449.8	534.0	315.6	3.1	13.	291.7	74.
	15:25	11.8	446.8	534.8	314.5	3.1	21.	290.0	74.
	15:26	11.8	450.0	535.6	314.4	3.0	11.	290.0	74.
	15:27	11.7	449.7	531.8	315.1	4.8	13.	290.4	74.
	15:28	11.8	446.7	532.3	315.4	1.6	13.	290.7	74.
	15:29	11.8	447.5	532.3	314.9	4.2	15.	291.7	74.
	15:30	11.8	448.5	532.5	314.8	4.4	10.	291.9	74.
	15:31	11.9	446.5	537.3	315.3	4.4	13.	292.0	74.
	15:32	11.9	445.1	537.1	315.9	3.7	19.	292.0	74.
	15:33	11.8	448.3	532.0	316.3	4.7	13.	291.6	74.
	15:34	11.7	449.7	531.8	316.5	3.7	12.	291.3	74.
	15:35	11.8	447.9	532.1	316.1	3.8	16.	291.3	74.
	15:36	11.7	448.5	531.5	315.4	5.1	13.	291.3	74.
	15:37	11.7	450.6	531.1	316.3	4.4	10.	291.2	74.
	15:38	11.8	447.8	533.3	317.3	3.0	15.	291.1	74.
	15:39	11.8	441.9	535.1	317.3	3.4	17.	291.1	74.
	15:40	11.8	445.2	533.6	314.9	4.7	14.	289.1	74.
	15:41	11.7	448.9	530.1	314.9	2.8	11.	289.0	74.
-----									
Average =		11.7	447.3	530.0	315.0	2.3	14.	293.7	74.
Maximum =		11.9	453.9	538.6	317.3	5.1	24.	301.8	75.
Minimum =		11.6	441.3	519.9	312.9	0.0	9.	289.0	74.
Possible Values =	147	147	147	147	147	147	147	147	147
Included Values =	147	147	147	147	147	147	147	147	147
Total =	1724.2	65748.1	77903.6	46301.5	340.1	2061.	43168.4	10896.	

\* - excluded values (missing, OOC, invalid, suspect)

&lt; - missing

T - out-of-control  
I - invalid  
S - suspect  
V - invalid for state  
H - exceedance  
F - stack not operating  
B - invalid (PADER)  
U - missing data substituted  
-999 - missing value  
-888 - value could not be calculated

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/15/1999 to 07/15/1999

Site Name: PIPPF6P6  
 Data Averaging Type: 1m

Time of Report: 07/19/99 07:43  
 Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/15/99	07:25	11.6	450.3	514.4	313.3	3.3	13.	293.2	74.
	07:26	11.7	449.4	516.8	313.4	2.9	9.	293.2	74.
	07:27	11.7	452.4	520.2	314.6	1.4	12.	293.0	74.
	07:28	11.7	453.9	522.1	314.7	3.0	10.	293.0	74.
	07:29	11.7	453.6	528.5	314.0	3.3	11.	292.8	74.
	07:30	11.8	450.8	531.1	313.4	2.3	26.	292.7	74.
	07:31	11.8	452.5	535.1	313.1	3.0	15.	291.1	74.
	07:32	11.8	452.1	532.9	313.1	1.5	11.	290.5	74.
	07:33	11.7	452.3	534.7	313.2	2.7	13.	289.7	74.
	07:34	11.8	451.7	540.4	313.5	3.0	11.	287.8	74.
	07:35	11.8	453.4	541.4	313.2	2.5	12.	287.9	75.
	07:36	11.9	450.3	543.0	312.6	0.7	10.	288.2	75.
	07:37	11.8	451.8	541.7	312.8	1.2	20.	288.2	74.
	07:38	11.7	453.3	537.3	314.4	2.0	11.	288.7	74.
	07:39	11.7	449.8	538.8	314.3	1.7	11.	288.6	74.
	07:40	11.8	448.3	541.0	313.1	1.9	11.	287.8	74.
	07:41	11.8	450.9	538.9	313.1	1.6	12.	287.8	74.
	07:42	11.8	450.9	543.3	314.1	2.4	11.	286.9	74.
	07:43	11.8	450.8	546.8	314.4	1.1	11.	286.8	74.
	07:44	11.8	452.6	545.0	313.6	1.9	16.	286.3	74.
	07:45	11.8	451.2	547.2	313.5	1.8	10.	286.2	75.
	07:46	11.9	449.9	548.5	313.5	0.8	11.	288.4	75.
	07:47	11.9	450.6	548.3	313.5	2.2	9.	290.1	75.
	07:48	11.8	450.5	547.0	313.9	0.7	13.	289.2	74.
	07:49	11.8	449.2	542.3	314.1	0.9	9.	288.7	74.
	07:50	11.8	451.1	540.1	313.7	0.0	18.	289.0	74.
	07:51	11.8	450.5	544.5	313.1	2.2	11.	289.5	74.
	07:52	11.9	451.5	550.6	313.2	1.7	13.	288.6	74.
	07:53	11.9	453.0	551.2	313.4	1.3	9.	287.9	74.
	07:54	11.8	452.3	546.8	313.4	1.4	12.	288.0	74.
	07:55	11.8	453.1	545.9	313.4	0.5	10.	289.0	74.
	07:56	11.8	451.9	546.9	313.5	2.7	12.	289.2	74.
	07:57	11.8	450.1	546.7	314.0	2.8	13.	289.5	74.
	07:58	11.9	447.6	551.1	314.0	1.6	12.	289.6	75.
	07:59	11.9	449.4	554.5	312.3	1.2	10.	289.8	75.
	08:00	11.8	452.3	551.4	312.3	1.5	11.	290.0	74.
	08:01	11.7	452.8	544.8	314.9	2.0	12.	290.9	74.
	08:02	11.7	453.9	543.5	314.9	0.0	13.	290.9	74.
	08:03	11.8	450.9	548.8	315.5	1.3	11.	291.5	74.
	08:04	11.8	450.3	549.0	315.8	3.1	16.	291.6	74.
	08:05	11.7	454.2	543.0	314.9	2.5	12.	291.1	74.
	08:06	11.8	451.7	546.1	314.7	3.2	13.	291.1	74.
	08:07	11.9	451.4	548.1	314.7	1.1	10.	291.7	74.
	08:08	11.9	452.4	549.5	314.7	3.7	16.	292.3	75.
	08:09	11.9	451.2	550.5	314.2	2.6	15.	292.7	75.
	08:10	11.8	452.6	546.6	313.7	2.0	11.	292.8	74.
	08:11	11.7	453.7	544.6	313.8	3.1	12.	292.8	75.
	08:12	11.8	450.3	547.1	314.1	2.0	10.	292.8	75.
	08:13	12.0	446.4	554.7	314.0	4.6	12.	293.3	75.
	08:14	11.9	450.9	550.7	314.0	3.6	11.	293.9	74.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/15/1999 to 07/15/1999

Site Name: PIPPF6P6  
 Data Averaging Type: 1m

Time of Report: 07/19/99 07:43  
 Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/15/99	08:15	11.6	457.3	536.2	314.0	2.9	10.	294.0	74.
	08:16	11.6	456.5	535.4	314.5	1.4	11.	294.5	74.
	08:17	11.7	453.9	539.7	314.5	0.0	11.	294.7	74.
	08:18	11.8	453.4	544.1	314.0	1.2	11.	295.7	75.
	08:19	11.9	452.2	547.1	314.0	2.8	11.	295.7	75.
	08:20	11.9	453.2	548.8	314.2	1.0	12.	296.2	75.
	08:21	11.9	450.8	552.4	314.3	2.6	11.	296.3	75.
	08:22	11.9	450.0	552.6	314.6	3.2	11.	296.6	74.
	08:23	11.6	457.2	542.9	314.7	3.1	12.	296.7	74.
	08:24	11.5	457.1	537.3	315.3	2.6	12.	296.9	74.
	08:25	11.8	452.8	546.9	316.1	2.1	10.	297.0	74.
	08:26	11.8	450.6	547.4	315.5	2.7	11.	295.4	74.
	08:27	11.8	454.6	549.5	315.2	2.0	11.	294.5	74.
	08:28	11.8	455.3	547.0	315.2	1.4	11.	293.8	74.
	08:29	11.8	456.0	548.8	314.9	2.8	11.	292.4	74.
	08:30	11.8	458.3	550.0	315.1	0.9	11.	292.4	75.
	08:31	11.9	457.7	550.3	315.5	1.3	11.	292.3	75.
	08:32	11.9	455.0	549.4	315.5	2.3	13.	292.3	75.
	08:33	11.9	457.5	551.1	315.0	2.4	12.	292.7	75.
	08:34	11.9	455.7	550.1	315.1	2.8	11.	292.9	75.
	08:35	11.8	458.9	549.8	315.3	3.2	10.	294.9	74.
	08:36	11.7	460.2	543.8	315.3	2.7	13.	294.9	74.
	08:37	11.7	458.7	546.9	314.4	5.1	10.	295.2	74.
	08:38	11.8	456.9	547.6	314.3	3.4	13.	295.3	74.
	08:39	11.8	459.0	545.2	315.2	3.8	11.	296.6	75.
	08:40	11.8	458.9	545.5	315.3	3.6	13.	296.6	75.
	08:41	11.8	455.2	546.5	315.2	3.8	11.	295.4	75.
	08:42	11.8	453.0	549.3	315.2	3.8	12.	294.8	75.
	08:43	11.7	457.3	546.6	316.3	4.4	11.	294.7	75.
	08:44	11.7	458.1	543.6	316.6	3.3	14.	294.6	74.
	08:45	11.7	457.1	542.3	315.6	3.4	11.	293.6	74.
	08:46	11.7	452.8	542.7	314.4	4.4	12.	292.4	74.
	08:47	11.8	453.9	548.3	314.9	2.7	11.	293.0	74.
	08:48	11.9	450.3	550.6	315.5	3.0	12.	293.8	75.
	08:49	11.9	450.9	550.0	315.6	4.7	23.	292.7	74.
	08:50	11.8	451.4	547.4	316.0	4.6	9.	291.1	74.
	08:51	11.8	448.6	549.1	315.6	3.0	18.	290.8	75.
	08:52	11.9	450.3	556.0	314.9	5.3	12.	290.4	75.
	08:53	11.9	450.5	556.2	314.9	3.1	12.	290.4	75.
	08:54	11.8	452.5	552.3	315.4	3.3	12.	289.5	75.
	08:55	11.8	452.8	551.7	315.5	4.0	11.	289.4	74.
	08:56	11.8	452.8	549.3	315.3	4.5	12.	289.4	74.
	08:57	11.8	454.2	550.1	315.3	4.3	12.	289.4	75.
	08:58	12.0	450.0	555.4	315.7	2.3	19.	291.5	75.
	08:59	11.9	450.8	552.4	315.8	2.3	13.	291.6	75.
	09:00	11.9	451.5	550.5	313.9	2.6	11.	291.8	75.
	09:01	11.8	454.8	546.3	313.7	4.2	10.	291.9	74.
	09:02	11.8	454.4	548.8	314.8	3.2	13.	292.7	75.
	09:03	11.8	456.9	546.3	315.8	3.3	11.	293.1	75.
	09:04	11.8	455.4	548.6	315.6	3.9	13.	292.1	74.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/15/1999 to 07/15/1999

Site Name: PIPPF6P6  
 Data Averaging Type: 1m

Time of Report: 07/19/99 07:43  
 Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	UGMEG (MEGAWATT)
07/15/99	09:05	11.8	454.5	548.8	315.5	4.6	17.	291.9	75.
	09:06	11.8	455.5	546.2	315.5	3.5	14.	291.3	75.
	09:07	11.8	454.1	546.7	315.8	4.4	11.	290.4	75.
	09:08	11.8	457.0	547.7	315.4	5.4	14.	290.7	75.
	09:09	11.9	456.2	545.3	314.7	2.3	12.	291.1	75.
	09:10	11.8	456.7	546.5	314.7	2.8	14.	291.1	75.
	09:11	11.8	455.9	542.8	314.9	4.2	16.	290.2	74.
	09:12	11.8	455.0	543.1	314.9	3.1	22.	290.3	74.
	09:13	11.8	455.5	545.2	314.7	2.9	12.	290.9	74.
	09:14	11.7	458.4	541.9	314.7	3.0	13.	290.9	74.
	09:15	11.7	458.6	537.2	314.6	2.9	11.	289.4	74.
	09:16	11.9	456.3	546.5	314.6	2.8	13.	289.1	75.
	09:17	12.1	450.7	558.2	312.7	2.5	11.	290.3	75.
	09:18	12.0	450.4	553.4	312.3	3.6	19.	290.5	75.
	09:19	11.8	455.9	546.9	313.3	3.0	13.	290.3	74.
	09:20	11.7	456.0	541.7	314.0	2.1	13.	290.1	74.
	09:21	11.8	453.8	546.2	314.0	2.8	10.	291.0	74.
	09:22	11.9	452.9	548.0	314.0	3.1	8.	291.2	75.
	09:23	11.9	453.5	547.1	313.8	4.7	8.	291.1	74.
	09:24	11.9	452.6	541.4	313.7	3.8	15.	290.9	74.
	09:25	11.9	452.0	545.9	314.0	1.6	20.	290.5	74.
	09:26	11.8	453.8	546.0	314.4	3.4	11.	290.2	74.
	09:27	11.8	456.5	544.1	314.6	3.3	13.	290.3	75.
	09:28	12.0	448.5	553.3	316.1	0.0	12.	291.3	75.
	09:29	12.1	444.6	553.9	316.0	2.1	11.	291.9	75.
	09:30	11.8	452.0	547.0	315.0	1.5	13.	293.7	74.
	09:31	11.7	455.7	541.9	315.0	2.7	15.	293.7	74.
	09:32	11.8	453.0	542.4	315.1	1.4	12.	293.3	74.
	09:33	11.9	451.2	547.8	315.2	2.3	12.	293.2	75.
	09:34	11.9	450.7	552.5	315.7	3.5	12.	292.9	75.
	09:35	11.9	453.6	550.1	315.8	2.4	11.	292.8	75.
	09:36	11.9	454.3	551.3	315.2	4.4	12.	292.1	75.
	09:37	11.9	453.1	551.8	314.7	3.9	12.	291.5	75.
	09:38	12.0	450.1	552.4	315.2	2.8	20.	292.8	75.
	09:39	11.9	453.1	550.3	315.5	3.3	13.	293.7	74.
	09:40	11.6	457.2	541.4	315.6	3.5	13.	293.7	74.
	09:41	11.7	456.1	541.6	317.5	4.0	12.	294.8	75.
	09:42	11.9	453.3	547.0	316.8	5.1	12.	294.8	75.
	09:43	11.9	454.4	545.8	314.7	3.2	12.	294.8	75.
	09:44	11.8	455.3	545.5	314.7	4.5	12.	294.8	74.
	09:45	11.8	456.2	543.3	314.9	4.3	29.	292.5	74.
	09:46	11.8	457.7	545.5	314.9	4.4	13.	292.0	74.
	09:47	11.9	452.5	549.0	315.8	4.2	12.	290.6	74.
	09:48	11.8	456.1	548.6	316.0	3.8	13.	290.7	74.
	09:49	11.8	457.6	544.3	315.9	4.9	12.	289.4	74.
	09:50	11.8	454.2	545.6	315.8	4.3	12.	289.0	74.
	09:51	11.8	453.7	545.8	315.3	5.2	16.	290.9	75.
	09:52	11.9	455.0	549.0	315.0	2.6	15.	291.6	75.
	09:53	12.0	450.0	552.9	315.3	4.3	11.	292.1	75.
	09:54	11.9	453.7	548.8	315.8	6.9	14.	292.8	75.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/15/1999 to 07/15/1999

Site Name: PIPPF6P6  
 Data Averaging Type: 1m

Time of Report: 07/19/99 07:43  
 Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/15/99	09:55	11.8	457.3	543.8	316.4	4.7	11.	294.2	75.
-----									
Average =		11.8	453.3	545.7	314.6	2.8	12.	291.8	74.
Maximum =		12.1	460.2	558.2	317.5	6.9	29.	297.0	75.
Minimum =		11.5	444.6	514.4	312.3	0.0	8.	286.2	74.
Possible Values =		151	151	151	151	151	151	151	151
Included Values =		151	151	151	151	151	151	151	151
Total =		1784.5	68453.3	82399.2	47510.4	428.2	1887.	44057.8	11246.

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect
- V - invalid for state
- H - exceedance
- F - stack not operating
- B - invalid (PADER)
- U - missing data substituted
- 999 - missing value
- 888 - value could not be calculated

## General Average Report

Reporting Period: 07/15/1999 to 07/15/1999

Site Name: PIPPF6P6

Time of Report: 07/19/99 07:43

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/15/99	11:50	11.7	454.7	528.8	316.0	4.1	14.	294.8	74.
	11:51	11.6	448.8	525.0	315.8	4.5	12.	295.4	74.
	11:52	11.8	450.2	531.8	315.8	2.6	13.	295.1	74.
	11:53	11.8	449.6	534.6	315.8	3.6	20.	294.3	74.
	11:54	11.8	448.9	536.8	315.6	3.9	14.	293.6	74.
	11:55	11.8	446.8	537.3	315.2	3.2	14.	292.4	74.
	11:56	11.8	449.6	537.5	315.2	4.4	14.	292.4	74.
	11:57	11.8	448.9	540.5	315.0	2.6	13.	292.8	74.
	11:58	11.8	449.5	541.5	315.0	3.5	18.	292.7	74.
	11:59	11.9	446.3	544.6	314.1	1.9	15.	290.9	74.
	12:00	12.0	446.5	548.3	314.1	2.6	12.	290.9	74.
	12:01	11.9	449.4	543.6	314.3	4.7	13.	290.5	74.
	12:02	11.8	452.4	541.8	314.4	1.9	12.	290.4	74.
	12:03	11.8	449.2	541.1	315.1	3.6	26.	290.8	74.
	12:04	11.8	448.6	543.8	315.3	3.3	13.	290.8	74.
	12:05	11.8	448.9	545.5	315.1	3.3	15.	291.6	74.
	12:06	11.8	450.0	543.0	314.9	3.5	12.	292.2	74.
	12:07	11.9	447.6	546.0	314.6	4.1	14.	291.2	74.
	12:08	12.0	442.8	549.0	314.6	3.1	17.	290.9	74.
	12:09	11.8	449.7	542.6	314.7	2.2	13.	290.2	74.
	12:10	11.7	450.9	540.8	314.9	4.0	11.	289.7	74.
	12:11	11.8	449.3	539.1	314.9	3.1	13.	289.7	74.
	12:12	11.8	446.5	539.6	314.9	2.6	11.	289.7	74.
	12:13	11.8	447.3	535.5	315.1	2.6	17.	289.9	74.
	12:14	11.8	446.7	536.6	315.5	4.8	12.	290.2	74.
	12:15	11.9	444.3	543.1	315.1	3.7	13.	289.6	74.
	12:16	12.0	440.9	542.5	314.6	4.7	13.	288.9	74.
	12:17	12.0	441.5	539.1	314.4	4.1	13.	288.7	74.
	12:18	11.8	447.8	534.1	314.1	4.8	21.	288.3	74.
	12:19	11.7	448.0	530.6	314.3	3.9	12.	288.1	74.
	12:20	11.8	446.4	535.6	314.6	3.2	15.	287.8	74.
	12:21	11.9	446.7	541.6	314.6	3.4	11.	287.9	74.
	12:22	11.9	449.0	545.1	314.2	4.9	13.	289.4	74.
	12:23	11.9	449.7	548.3	314.2	2.6	18.	289.3	74.
	12:24	11.8	450.4	542.8	315.5	4.1	15.	289.1	74.
	12:25	11.8	450.3	543.5	315.5	4.5	12.	289.1	74.
	12:26	11.8	451.0	544.1	314.7	5.3	14.	289.5	74.
	12:27	11.8	450.5	543.8	314.4	5.1	12.	289.5	74.
	12:28	11.8	448.8	546.0	314.4	5.4	17.	290.0	74.
	12:29	11.8	449.5	545.5	314.4	5.5	13.	290.1	74.
	12:30	11.8	450.4	545.3	315.1	5.0	13.	290.4	74.
	12:31	11.9	450.4	546.1	315.8	5.4	11.	290.5	74.
	12:32	11.9	448.1	542.3	314.7	5.1	14.	292.8	74.
	12:33	11.9	445.7	535.5	314.3	5.1	21.	293.5	74.
	12:34	11.7	451.3	532.3	314.5	5.5	15.	293.2	74.
	12:35	11.7	451.9	533.3	315.2	3.4	10.	292.3	74.
	12:36	11.8	449.5	536.8	315.5	5.9	15.	292.7	74.
	12:37	11.8	449.1	539.0	315.8	4.3	11.	293.1	74.
	12:38	11.8	455.3	541.8	315.6	3.4	23.	293.0	74.
	12:39	11.9	452.0	544.0	313.4	3.6	12.	291.7	75.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/15/1999 to 07/15/1999

Site Name: PIPPF6P6  
 Data Averaging Type: 1m

Time of Report: 07/19/99 07:43  
 Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PPM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/15/99	12:40	11.9	449.4	543.1	313.9	4.0	14.	292.6	74.
	12:41	11.8	449.9	538.5	315.0	3.2	10.	293.8	74.
	12:42	11.6	453.3	532.1	315.0	3.9	14.	293.7	74.
	12:43	11.7	452.0	535.3	315.7	2.0	13.	293.0	74.
	12:44	11.8	448.8	540.5	315.9	5.0	15.	293.0	74.
	12:45	11.8	449.9	538.7	316.6	2.7	11.	293.4	74.
	12:46	11.8	445.8	544.1	316.6	5.0	15.	293.4	74.
	12:47	11.9	441.5	542.5	316.0	6.0	11.	293.8	74.
	12:48	11.7	449.5	538.2	315.8	3.4	25.	293.9	74.
	12:49	11.7	450.8	536.9	314.8	3.1	11.	293.8	74.
	12:50	11.9	447.0	543.1	314.7	4.0	16.	293.8	74.
	12:51	11.9	444.7	547.6	315.1	3.8	11.	293.3	74.
	12:52	11.8	450.4	544.4	315.5	4.3	12.	292.8	74.
	12:53	11.8	451.1	540.1	315.3	4.8	18.	291.0	74.
	12:54	11.8	451.0	540.3	315.2	5.0	13.	290.2	74.
	12:55	11.8	449.7	541.0	315.4	3.0	11.	290.3	74.
	12:56	11.9	448.7	541.6	316.2	2.4	13.	290.4	74.
	12:57	11.8	451.9	540.9	316.4	4.7	11.	290.7	74.
	12:58	11.8	452.3	539.5	316.6	2.7	16.	291.3	74.
	12:59	11.8	451.0	542.5	316.5	5.0	12.	291.2	74.
	13:00	11.8	447.7	538.6	316.4	4.7	13.	290.2	74.
	13:01	11.7	451.0	541.7	316.3	3.3	11.	290.3	74.
	13:02	11.8	448.3	550.3	315.5	2.4	13.	290.5	75.
	13:03	12.1	438.8	552.6	315.5	1.4	22.	290.5	74.
	13:04	11.8	446.4	542.9	315.6	3.9	15.	288.5	74.
	13:05	11.6	451.5	532.1	315.6	5.4	13.	288.3	73.
	13:06	11.6	450.0	536.9	315.8	3.7	12.	290.3	74.
	13:07	11.8	446.4	540.0	315.8	1.7	10.	290.4	74.
	13:08	11.9	443.0	539.8	315.5	4.1	20.	291.1	74.
	13:09	12.0	440.7	543.9	315.3	5.7	12.	291.6	74.
	13:10	11.8	445.9	539.7	316.0	3.1	13.	292.8	74.
	13:11	11.7	444.9	535.4	316.2	4.7	12.	293.4	74.
	13:12	11.7	447.6	530.0	315.3	2.2	13.	293.1	74.
	13:13	11.7	447.5	531.7	314.4	2.8	15.	292.8	74.
	13:14	11.8	445.7	534.2	314.2	2.8	14.	291.5	74.
	13:15	11.8	445.6	537.2	314.1	3.5	12.	290.9	74.
	13:16	11.9	447.3	537.5	314.0	3.9	13.	290.1	74.
	13:17	11.9	448.1	536.7	313.8	3.3	13.	288.6	74.
	13:18	11.8	450.4	536.1	314.8	3.1	22.	288.9	74.
	13:19	11.8	451.1	536.1	316.2	3.7	13.	289.1	74.
	13:20	11.8	451.8	533.6	316.0	3.6	14.	289.5	74.
	13:21	11.8	449.8	531.9	315.2	4.9	12.	290.2	74.
	13:22	11.8	450.3	528.5	315.2	1.9	12.	291.1	74.
	13:23	11.8	448.8	535.0	315.2	3.8	18.	292.4	74.
	13:24	11.8	448.0	534.8	315.2	3.4	13.	292.4	74.
	13:25	11.8	448.3	533.9	315.5	2.7	12.	292.0	74.
	13:26	11.8	448.3	534.5	316.0	2.2	13.	292.2	74.
	13:27	11.7	449.7	530.5	317.6	3.0	11.	292.7	74.
	13:28	11.7	450.7	531.1	317.6	4.0	17.	292.7	74.
	13:29	11.8	445.7	533.3	316.0	4.0	12.	292.0	74.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/15/1999 to 07/15/1999

Site Name: PIPPF6P6

Time of Report: 07/19/99 07:43

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F6CPCO2 (PERCENT )	F6CPNOX (PPM )	F6CPSO2 (PFM )	F6STEMP (DEGFAHRE)	F6CO (PPM )	F6OPC (PERCENT )	F6AFLOW (KACFM )	U6MEG (MEGAWATT)
07/15/99	13:30	11.8	447.6	533.3	315.8	3.6	13.	291.8	74.
	13:31	11.8	447.7	533.7	315.9	3.2	11.	291.0	74.
	13:32	11.9	443.2	538.7	315.9	4.8	13.	291.0	74.
	13:33	11.7	445.4	533.2	316.0	2.6	22.	291.0	74.
	13:34	11.6	450.5	526.8	316.1	3.6	12.	290.9	74.
	13:35	11.8	449.8	529.8	316.1	4.2	14.	292.5	74.
	13:36	11.9	445.0	540.5	316.1	4.5	11.	293.1	74.
	13:37	11.8	447.7	540.0	315.9	4.3	13.	293.5	74.
	13:38	11.8	449.5	538.8	315.5	4.2	18.	293.8	74.
	13:39	11.8	449.5	533.1	315.2	4.4	14.	293.4	74.
	13:40	11.8	450.3	534.3	314.9	5.2	11.	292.8	74.
	13:41	11.8	452.5	536.9	315.1	5.0	15.	292.7	74.
	13:42	11.8	450.2	537.9	316.6	7.1	11.	292.2	74.
	13:43	11.8	451.3	539.9	316.5	4.7	19.	292.3	74.
	13:44	11.8	452.1	536.6	316.2	4.8	11.	292.6	74.
	13:45	11.8	451.4	537.5	316.3	6.2	14.	292.6	74.
	13:46	11.8	451.7	541.5	315.3	5.2	12.	291.5	74.
	13:47	11.9	452.3	542.1	315.2	5.4	14.	291.2	75.
	13:48	11.9	451.6	542.9	315.9	5.3	26.	290.5	75.
	13:49	11.9	450.9	545.6	316.0	5.9	15.	290.5	75.
	13:50	11.8	450.6	543.1	315.6	6.1	12.	289.4	75.
	13:51	11.8	451.6	542.5	315.5	5.5	14.	289.0	74.
	13:52	11.7	451.2	536.7	314.6	5.7	12.	288.6	74.
	13:53	11.7	452.1	534.7	314.3	4.1	21.	288.6	74.
	13:54	11.7	450.1	534.1	315.5	6.0	11.	289.0	74.
	13:55	11.7	450.4	534.0	316.6	3.9	14.	289.4	74.
	13:56	11.8	448.1	537.4	315.5	5.5	11.	291.9	74.
	13:57	11.8	448.4	537.8	314.9	5.0	14.	293.2	74.
	13:58	11.8	449.8	535.8	314.8	4.7	14.	293.8	74.
	13:59	11.7	450.8	536.0	314.0	4.7	16.	294.9	74.
	14:00	11.7	452.5	536.5	314.6	5.5	12.	294.4	74.
	14:01	11.7	448.6	537.1	315.8	5.5	14.	293.5	74.
	14:02	11.7	448.7	536.2	315.8	4.0	11.	293.5	74.
	14:03	11.7	448.3	536.2	314.2	4.4	23.	290.1	74.
	14:04	11.7	446.8	536.6	314.2	3.6	13.	289.8	74.
	14:05	11.6	448.0	532.5	314.6	4.2	14.	288.7	74.
	14:06	11.7	449.8	535.1	314.6	5.5	11.	288.7	74.
	14:07	11.8	446.4	541.1	314.8	5.2	14.	290.8	74.
	14:08	11.9	445.1	544.3	314.9	3.4	17.	292.0	74.
	14:09	11.9	442.4	540.9	314.8	5.3	15.	292.8	74.
	14:10	11.8	442.9	538.9	314.7	3.7	11.	293.0	74.
	14:11	11.7	444.9	536.0	314.8	5.3	12.	293.6	74.
	14:12	11.7	446.8	534.8	314.9	2.6	12.	294.4	74.
-----									
	Average =	11.8	448.7	538.7	315.3	4.1	14.	291.4	74.
	Maximum =	12.1	455.3	552.6	317.6	7.1	26.	295.4	75.
	Minimum =	11.6	438.8	525.0	313.4	1.4	10.	287.8	73.
Possible Values =	143	143	143	143	143	143	143	143	143
Included Values =	143	143	143	143	143	143	143	143	143
Total =	1686.8	64159.7	77029.4	45083.3	579.6	2014.	41675.5	10585.	

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect
- V - invalid for state

H - exceedance  
F - stack not operating  
B - invalid (PADER)  
U - missing data substituted  
-999 - missing value  
-888 - value could not be calculated

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**UNIT 6 ESP DATA**

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Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	298	46	35	233
T/R 6B	155	42	19	0
T/R 6C	308	18	39	58
T/R 6D	280	41	33	227
OPACITY	13.80%			
Boiler Load	75 Mw			
Excess Air	2.74%			
DATE:	07/14/1999	TIME:	14:12	

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	301	49	35	248
T/R 6B	158	42	19	0
T/R 6C	308	18	39	59
T/R 6D	283	43	34	238
OPACITY	12.33%			
Boiler Load	75 Mw			
Excess Air	2.70%			
DATE:	07/14/1999	TIME:	15:00	

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	301	48	35	246
T/R 6B	154	42	18	0
T/R 6C	311	19	40	63
T/R 6D	281	42	34	235
OPACITY	11.79%			
Boiler Load	75 Mw			
Excess Air	2.64%			
DATE:	07/14/1999	TIME:	16:00	

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	299	49	35	250
T/R 6B	150	42	18	0
T/R 6C	310	18	39	62
T/R 6D	280	42	34	233

OPACITY 14.63%  
Boiler Load 75 Mw  
Excess Air 2.60%

DATE: 07/14/1999                      TIME: 16:48

Wepeco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	303	46	36	235
T/R 6B	169	42	22	0
T/R 6C	325	21	41	72
T/R 6D	294	47	35	269

OPACITY 10.16%  
Boiler Load 75 Mw  
Excess Air 2.73%

DATE: 07/15/1999                      TIME: 8:00

Wepeco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	304	47	36	234
T/R 6B	164	42	21	0
T/R 6C	311	18	40	58
T/R 6D	285	42	34	237

OPACITY 14.65%  
Boiler Load 75 Mw  
Excess Air 2.74%

DATE: 07/15/1999                      TIME: 8:24

Wepeco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	306	50	36	259
T/R 6B	162	42	20	0
T/R 6C	320	19	41	64
T/R 6D	292	44	35	257

OPACITY 12.01%  
Boiler Load 75 Mw  
Excess Air 2.73%

DATE: 07/15/1999                      TIME: 9:00

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	300	49	35	251
T/R 6B	162	42	20	0
T/R 6C	316	19	40	63
T/R 6D	285	42	34	239
OPACITY	11.97%			
Boiler Load	75 Mw			
Excess Air	2.78%			
DATE:	07/15/1999		TIME:	10:00

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	318	57	37	306
T/R 6B	160	42	20	0
T/R 6C	329	22	40	80
T/R 6D	299	49	35	288
OPACITY	10.74%			
Boiler Load	75 Mw			
Excess Air	2.70%			
DATE:	07/15/1999		TIME:	10:54

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	304	50	36	255
T/R 6B	143	42	18	0
T/R 6C	312	18	40	59
T/R 6D	287	42	34	235
OPACITY	14.33%			
Boiler Load	75 Mw			
Excess Air	2.69%			
DATE:	07/15/1999		TIME:	12:48

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	305	51	36	264
T/R 6B	143	42	19	0
T/R 6C	316	19	40	61
T/R 6D	286	42	34	236

OPACITY 13.28%  
Boiler Load 75 Mw  
Excess Air 2.74%

DATE: 07/15/1999                      TIME: 13:00

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	308	51	36	262
T/R 6B	150	42	19	0
T/R 6C	317	19	40	66
T/R 6D	287	43	34	242

OPACITY 12.89%  
Boiler Load 75 Mw  
Excess Air 2.70%

DATE: 07/15/1999                      TIME: 14:00

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	308	51	36	269
T/R 6B	136	42	19	0
T/R 6C	319	19	41	66
T/R 6D	288	42	34	239

OPACITY 13.48%  
Boiler Load 75 Mw  
Excess Air 2.67%

DATE: 07/15/1999                      TIME: 15:00

Wepco Presque Isle  
Unit 6 Precipitator

Console	Primary		Secondary	
	VAC	IAC	Kv	mA
T/R 6A	304	50	36	255
T/R 6B	138	42	19	0
T/R 6C	316	19	40	65
T/R 6D	281	41	34	229

OPACITY 16.02%

Boiler Load 76 Mw

Excess Air 2.58%

DATE: 07/15/1999

TIME: 15:12

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## UNITS 1-4 PROCESS OPERATION DATA

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PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

21

UNIT NO.: "A" Bag House - 3

TIME: 0900-1000

DATE: 7-16-99

- ① Gross Generation - MWH 48.629
- ② Station Service - MWH 3.264
- ③ Net Generation - MWH 45.360
- ④ Control Valve Position % 0.05
- ⑤ Main Steam Flow Lbs./Hr. 292,000
- ⑥ F.W. Flow Lbs./Hr. 387,600
- ⑦ F.W. Press. Psig 1810
- 8. Chart Throttle Press. Psig \_\_\_\_\_
- 9. Test Gauge Throttle Press. Psig \_\_\_\_\_
- ⑩ First Stage Press. Psig 825
- ⑪ Cold Reheat Press. Psig 349
- ⑫ Hot Reheat Press. Psig 315
- ⑬ F.W. (Loading/Temp.) 14 lbs / 438
- ⑭ Main Steam Temp. °F 955
- ⑮ Cold Reheat Temp. °F 675
- ⑯ Hot Reheat Temp. °F 1010
- ⑰ Superheat Spray Flow 0
- ⑱ Reheat Spray Flow 0
- ⑲ Air Flow 360,000
- ⑳ Excess Oxygen % 3.3
- ⑰ Inlet Air Temp. °F NOTE
- ⑲ Gas Outlet Temp. °F NOTE
- 23. Opacity % \_\_\_\_\_
- ⑳ I.D. Fan (Loading/Amps) 239
- ㉑ F.D. Fan (Loading/rpm/Amps) 17 lbs / 69
- ⑳ Air Heater Press. (H2O) \_\_\_\_\_

	IN	OUT	P
AIR	<u>7.0</u>	<u>3.5</u>	<u>3.5</u>
GAS	<u>3.2</u>	<u>-7.9</u>	<u>-4.7</u>

- 27. Burner Tilt Position/RH P \_\_\_\_\_
  - 28. Condensate Pump Amps A \_\_\_\_\_ B \_\_\_\_\_
  - 29. Boiler Feed Pump Amps A \_\_\_\_\_ B \_\_\_\_\_  
C \_\_\_\_\_
  - 30. Coal Feeder Loading A \_\_\_\_\_ B \_\_\_\_\_  
C \_\_\_\_\_ D \_\_\_\_\_
  - 31. Pulverizer Amps A \_\_\_\_\_ B \_\_\_\_\_  
C \_\_\_\_\_ D \_\_\_\_\_
  - 32. Mill Outage Temp. A \_\_\_\_\_ B \_\_\_\_\_  
C \_\_\_\_\_ D \_\_\_\_\_
  - ⑳ Coal Scale Readings:
- |   | Beginning    | Ending       | Total        |
|---|--------------|--------------|--------------|
| a | <u>80255</u> | <u>81095</u> | _____        |
| b | <u>80815</u> | <u>81143</u> | _____        |
| c | <u>60</u>    | <u>48</u>    | <u>108</u>   |
| d | _____        | <u>4400</u>  | <u>43200</u> |

- ⑳ Lbs. Coal/Net KWH 952
- ㉑ Lbs. Steam/Net KWH 6.547
- 38. Barometric Press. In.Hg \_\_\_\_\_
- 39. Vacuum In.Hg \_\_\_\_\_
- 40. Back Press. In.Hg \_\_\_\_\_
- 41. Circ. Water Pump Amps A \_\_\_\_\_ B \_\_\_\_\_  
N or W S or E \_\_\_\_\_
- 42. Circ. Water Inlet Temp. °F \_\_\_\_\_
- 43. Circ. Water Outlet Temp °F \_\_\_\_\_
- 44. Circ. Water Inlet Press. Psig \_\_\_\_\_
- 45. Circ. Water Outlet Press. Psig \_\_\_\_\_
- 46. Condensate Make-up \_\_\_\_\_
- 47. Condensate Draw-off \_\_\_\_\_
- 48. Hot Well Temp. °F \_\_\_\_\_
- 49. Turbine Exhaust Temp. °F \_\_\_\_\_
- 50. 1st Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 51. 1st Pt.Htr.Ext.Temp. °F \_\_\_\_\_
- 52. 1st Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 53. 2nd Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 54. 2nd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 55. 2nd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 56. 3rd Pt.Htr.Ext. Press. Psig \_\_\_\_\_
- 57. 3rd Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 58. 3rd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 59. 4th Pt.Htr.Ext.Press. Psig \_\_\_\_\_
- 60. 4th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 61. 4th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 62. 5th Pt.Htr.Ext. Press.In.Hg \_\_\_\_\_
- 63. 5th Pt.Htr.Ext. Temp. °F \_\_\_\_\_
- 64. 5th Pt.Htr.F.W.In Temp. °F \_\_\_\_\_
- 65. 5th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_
- 66. 1st Pt.F.W.Out Temp.Minus(-)  
5th Pt.F.W. In Temp. °F = \_\_\_\_\_
- 67. 1st Pt. Drain Temp. °F \_\_\_\_\_
- 68. 2nd Pt. Drain Temp. °F \_\_\_\_\_
- 69. 3rd Pt. Drain Temp. °F \_\_\_\_\_
- 70. 4th Pt. Drain Temp. °F \_\_\_\_\_
- 71. 5th Pt. Drain Temp. °F \_\_\_\_\_
- 72. Vars - Mvar \_\_\_\_\_
- 73. Generator Voltage - K volts \_\_\_\_\_
- 74. Auxiliary Steam Uses: \_\_\_\_\_

NOTE

Remarks: Bag house  
INLET TEMP 248 OUTLET TEMP 263  
PRESS -12 OUTLET PRESS -17

⑳ Coal Total Lbs. Hr. 43200

John Brunner  
CRO

Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

R1

UNIT NO.: B BAG HSE 244

TIME: 1000-1100

DATE: 7-16-95

① Gross Generation - MWH 49.000  
 ② Station Service - MWH 3.00  
 ③ Net Generation - MWH 46.000  
 ④ Control Valve Position % 0.03  
 ⑤ Main Steam Flow Lbs./Hr. 378.000  
 ⑥ F.W. Flow Lbs./Hr. 423.000  
 ⑦ F.W. Press. Psig 1850  
 8. Chart Throttle Press. Psig \_\_\_\_\_  
 9. Test Gauge Throttle Press. Psig \_\_\_\_\_  
 ⑩ First Stage Press. Psig 900  
 ⑪ Cold Reheat Press. Psig 339  
 ⑫ Hot Reheat Press. Psig 305  
 ⑬ F.W. (Loading/Temp.) 510/442  
 ⑭ Main Steam Temp. °F 924  
 ⑮ Cold Reheat Temp. °F 685  
 ⑯ Hot Reheat Temp. °F 1009  
 ⑰ Superheat Spray Flow \_\_\_\_\_  
 ⑱ Reheat Spray Flow 0  
 ⑲ Air Flow 390,000  
 ⑳ Excess Oxygen % 3.5  
 ㉑ Inlet Air Temp. °F NOT R  
 ㉒ Gas Outlet Temp. °F NOT R  
 23. Opacity % \_\_\_\_\_  
 ⑳ I.D. Fan (Loading/Amps) 270 AMP  
 ㉑ F.D. Fan (Loading/rpm/Amps) 849/67  
 ⑳ Air Heater Press. (H2O) \_\_\_\_\_  

	IN	OUT	P
AIR	<u>5.0</u>	<u>3.5</u>	<u>1.5</u>
GAS	<u>-3.2</u>	<u>-4.0</u>	<u>-0.8</u>

 27. Burner Tilt Position/RH P \_\_\_\_\_  
 28. Condensate Pump Amps A \_\_\_\_\_ B \_\_\_\_\_  
 29. Boiler Feed Pump Amps A \_\_\_\_\_ B \_\_\_\_\_  
 C \_\_\_\_\_  
 30. Coal Feeder Loading A \_\_\_\_\_ B \_\_\_\_\_  
 C \_\_\_\_\_ D \_\_\_\_\_  
 31. Pulverizer Amps A \_\_\_\_\_ B \_\_\_\_\_  
 C \_\_\_\_\_ D \_\_\_\_\_  
 32. Mill Outage Temp. A \_\_\_\_\_ B \_\_\_\_\_  
 C \_\_\_\_\_ D \_\_\_\_\_  
 ⑳ Coal Scale Readings:  

	Beginning	Ending	Total
a	<u>27914</u>	<u>73066</u>	
b	<u>27980</u>	<u>73133</u>	
c	<u>66</u>	<u>61</u>	
d		<u>X400</u>	<u>50400</u>

⑳ Lbs. Coal/Net KWH 1.104  
 ㉑ Lbs. Steam/Net KWH 8.217  
 38. Barometric Press. In.Hg \_\_\_\_\_  
 39. Vacuum In.Hg \_\_\_\_\_  
 40. Back Press. In.Hg \_\_\_\_\_  
 41. Circ. Water Pump Amps A \_\_\_\_\_ B \_\_\_\_\_  
 N or W S or E \_\_\_\_\_  
 42. Circ. Water Inlet Temp. °F \_\_\_\_\_  
 43. Circ. Water Outlet Temp °F \_\_\_\_\_  
 44. Circ. Water Inlet Press. Psig \_\_\_\_\_  
 45. Circ. Water Outlet Press. Psig \_\_\_\_\_  
 46. Condensate Make-up \_\_\_\_\_  
 47. Condensate Draw-off \_\_\_\_\_  
 48. Hot Well Temp. °F \_\_\_\_\_  
 49. Turbine Exhaust Temp. °F \_\_\_\_\_  
 50. 1st Pt.Htr.Ext.Press. Psig \_\_\_\_\_  
 51. 1st Pt.Htr.Ext.Temp. °F \_\_\_\_\_  
 52. 1st Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 53. 2nd Pt.Htr.Ext.Press. Psig \_\_\_\_\_  
 54. 2nd Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 55. 2nd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 56. 3rd Pt.Htr.Ext. Press. Psig \_\_\_\_\_  
 57. 3rd Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 58. 3rd Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 59. 4th Pt.Htr.Ext.Press. Psig \_\_\_\_\_  
 60. 4th Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 61. 4th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 62. 5th Pt.Htr.Ext. Press.In.Hg \_\_\_\_\_  
 63. 5th Pt.Htr.Ext. Temp. °F \_\_\_\_\_  
 64. 5th Pt.Htr.F.W.In Temp. °F \_\_\_\_\_  
 65. 5th Pt.Htr.F.W.Out Temp. °F \_\_\_\_\_  
 66. 1st Pt.F.W.Out Temp.Minus(-) \_\_\_\_\_  
 5th Pt.F.W. In Temp. °F \_\_\_\_\_  
 67. 1st Pt. Drain Temp. °F \_\_\_\_\_  
 68. 2nd Pt. Drain Temp. °F \_\_\_\_\_  
 69. 3rd Pt. Drain Temp. °F \_\_\_\_\_  
 70. 4th Pt. Drain Temp. °F \_\_\_\_\_  
 71. 5th Pt. Drain Temp. °F \_\_\_\_\_  
 72. Vars - Mvar \_\_\_\_\_  
 73. Generator Voltage - K volts \_\_\_\_\_  
 74. Auxiliary Steam Uses: \_\_\_\_\_  
 75. Remarks: NOTE  
B. Baghouse  
INLET TEMP 311 OUTLET TEMP 302  
INLET PRESS -13 OUTLET PRESS -17

⑳ Coal Total Lbs. Hr. \_\_\_\_\_

J. Brunner  
 CRO Engineer





PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

R2

UNIT NO.: A-Baghouse #3 #11 TIME: 1300-1400 DATE: 07-16-90

1. Gross Generation - MWH	<u>51.480</u>	35. Lbs. Coal/Net KWH	<u>9653</u>
2. Station Service - MWH	<u>3.00</u>	36. Lbs. Steam/Net KWH	<u>6.590</u>
3. Net Generation - MWH	<u>48.480</u>	38. Barometric Press. In.Hg	_____
4. Control Valve Position %	<u>0.05</u>	39. Vacuum In.Hg	_____
5. Main Steam Flow Lbs./Hr.	<u>319.500</u>	40. Back Press. In.Hg	_____
6. F.W. Flow Lbs./Hr.	<u>414.000</u>	41. Circ. Water Pump Amps	A _____ B _____
7. F.W. Press. Psig	<u>1800</u>		N or W S or E _____
8. Chart Throttle Press. Psig	_____	42. Circ. Water Inlet Temp. °F	_____
9. Test Gauge Throttle Press. Psig	_____	43. Circ. Water Outlet Temp °F	_____
10. First Stage Press. Psig	<u>825</u>	44. Circ. Water Inlet Press. Psig	_____
11. Cold Reheat Press. Psig	<u>389</u>	45. Circ. Water Outlet Press. Psig	_____
12. Hot Reheat Press. Psig	<u>315</u>	46. Condensate Make-up	_____
13. F.W. (Loading/Temp.)	<u>14.889 439</u>	47. Condensate Draw-off	_____
14. Main Steam Temp. °F	<u>957</u>	48. Hot Well Temp. °F	_____
15. Cold Reheat Temp. °F	<u>675</u>	49. Turbine Exhaust Temp. °F	_____
16. Hot Reheat Temp. °F	<u>1009</u>	50. 1st Pt.Htr.Ext.Press. Psig	_____
17. Superheat Spray Flow	<u>0</u>	51. 1st Pt.Htr.Ext.Temp. °F	_____
18. Reheat Spray Flow	<u>0</u>	52. 1st Pt.Htr.F.W.Out Temp. °F	_____
19. Air Flow	<u>360,000</u>	53. 2nd Pt.Htr.Ext.Press. Psig	_____
20. Excess Oxygen %	<u>3.4</u>	54. 2nd Pt.Htr.Ext. Temp. °F	_____
21. Inlet Air Temp. °F	<u>NOTE</u>	55. 2nd Pt.Htr.F.W.Out Temp. °F	_____
22. Gas Outlet Temp. °F	<u>NOTE</u>	56. 3rd Pt.Htr.Ext. Press. Psig	_____
23. Opacity %	_____	57. 3rd Pt.Htr.Ext. Temp. °F	_____
24. I.D. Fan (Loading/Amps)	<u>235 AMPS</u>	58. 3rd Pt.Htr.F.W.Out Temp. °F	_____
25. F.D. Fan (Loading/rpm/Amps)	<u>64 AMPS</u>	59. 4th Pt.Htr.Ext.Press. Psig	_____
26. Air Heater Press. (H2O)	_____	60. 4th Pt.Htr.Ext. Temp. °F	_____
	IN OUT P	61. 4th Pt.Htr.F.W.Out Temp. °F	_____
AIR	<u>7.9</u>	<u>6.0</u>	<u>1.9</u>
GAS	<u>-3.4</u>	<u>-8.0</u>	<u>-4.6</u>
27. Burner Tilt Position/RH P	_____	62. 5th Pt.Htr.Ext. Press.In.Hg	_____
28. Condensate Pump Amps	A _____ B _____	63. 5th Pt.Htr.Ext. Temp. °F	_____
29. Boiler Feed Pump Amps	A _____ B _____	64. 5th Pt.Htr.F.W.In Temp. °F	_____
	C _____	65. 5th Pt.Htr.F.W.Out Temp. °F	_____
30. Coal Feeder Loading	A _____ B _____	66. 1st Pt.F.W.Out Temp.Minus(-)	_____
	C _____ D _____	5th Pt.F.W. In Temp. °F =	_____
31. Pulverizer Amps	A _____ B _____	67. 1st Pt. Drain Temp. °F	_____
	C _____ D _____	68. 2nd Pt. Drain Temp. °F	_____
32. Mill Outage Temp.	A _____ B _____	69. 3rd Pt. Drain Temp. °F	_____
	C _____ D _____	70. 4th Pt. Drain Temp. °F	_____
33. Coal Scale Readings:		71. 5th Pt. Drain Temp. °F	_____
Beginning Ending Total		72. Vars - Mvar	_____
a <u>81012</u> <u>81079</u> <u>66</u>		73. Generator Voltage - K volts	_____
b <u>81288</u> <u>81339</u> <u>51</u>		74. Auxiliary Steam Uses:	_____
c _____ _____ <u>117</u>			_____
d _____ _____ <u>8400</u>			_____

34. Coal Total Lbs. Hr. 41800

John B...  
CRO Engineer

75. Remarks: NOTE  
A-Baghouse  
INLET TEMP 285 OUTLET TEMP 284  
INLET PRESS -12 OUTLET PRESS -14

1236 # 1 ON THE LINE

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

R3

UNIT NO.: B- Baghouse <sup>204</sup> <sub>units</sub> TIME: 1400-1500 DATE: 7-16-95

- |                                    |                |                                    |   |
|------------------------------------|----------------|------------------------------------|---|
| ① Gross Generation - MWH           | <u>47.748</u>  | ③⑤ Lbs. Coal/Net KWH               | <u>1.010</u>                              |
| ② Station Service - MWH            | <u>3.00</u>    | ③⑥ Lbs. Steam/Net KWH              | <u>7.542.24</u>                           |
| ③ Net Generation - MWH             | <u>44.748</u>  | 38. Barometric Press. In.Hg        | _____                                     |
| ④ Control Valve Position %         | _____          | 39. Vacuum In.Hg                   | _____                                     |
| ⑤ Main Steam Flow Lbs./Hr.         | <u>337.500</u> | 40. Back Press. In.Hg              | _____                                     |
| ⑥ F.W. Flow Lbs./Hr.               | <u>373.500</u> | 41. Circ. Water Pump Amps          | A _____ B _____                           |
| ⑦ F.W. Press. Psig                 | <u>1850</u>    |                                    | N or W S or E                             |
| 8. Chart Throttle Press. Psig      | _____          | 42. Circ. Water Inlet Temp. °F     | _____                                     |
| 9. Test Gauge Throttle Press. Psig | _____          | 43. Circ. Water Outlet Temp °F     | _____                                     |
| ⑩ First Stage Press. Psig          | <u>900</u>     | 44. Circ. Water Inlet Press. Psig  | _____                                     |
| ⑪ Cold Reheat Press. Psig          | <u>335</u>     | 45. Circ. Water Outlet Press. Psig | _____                                     |
| ⑫ Hot Reheat Press. Psig           | <u>305</u>     | 46. Condensate Make-up             | _____                                     |
| ⑬ F.W. (Loading/Temp.)             | <u>510/442</u> | 47. Condensate Draw-off            | _____                                     |
| ⑭ Main Steam Temp. °F              | <u>925</u>     | 48. Hot Well Temp. °F              | _____                                     |
| ⑮ Cold Reheat Temp. °F             | <u>685</u>     | 49. Turbine Exhaust Temp. °F       | _____                                     |
| ⑯ Hot Reheat Temp. °F              | <u>1009</u>    | 50. 1st Pt.Htr.Ext.Press. Psig     | _____                                     |
| ⑰ Superheat Spray Flow             | <u>0</u>       | 51. 1st Pt.Htr.Ext.Temp. °F        | _____                                     |
| ⑱ Reheat Spray Flow                | <u>0</u>       | 52. 1st Pt.Htr.F.W.Out Temp. °F    | _____                                     |
| ⑲ Air Flow                         | <u>390000</u>  | 53. 2nd Pt.Htr.Ext.Press. Psig     | _____                                     |
| ⑳ Excess Oxygen %                  | <u>3.5</u>     | 54. 2nd Pt.Htr.Ext. Temp. °F       | _____                                     |
| ㉑ Inlet Air Temp. °F               | <u>1078</u>    | 55. 2nd Pt.Htr.F.W.Out Temp. °F    | _____                                     |
| ㉒ Gas Outlet Temp. °F              | <u>1076</u>    | 56. 3rd Pt.Htr.Ext. Press. Psig    | _____                                     |
| 23. Opacity %                      | _____          | 57. 3rd Pt.Htr.Ext. Temp. °F       | _____                                     |
| ㉔ I.D. Fan (Loading/Amps)          | <u>271</u>     | 58. 3rd Pt.Htr.F.W.Out Temp. °F    | _____                                     |
| ㉕ F.D. Fan (Loading/rpm/Amps)      | <u>8490/67</u> | 59. 4th Pt.Htr.Ext.Press. Psig     | _____                                     |
| ㉖ Air Heater Press. (H2O)          | _____          | 60. 4th Pt.Htr.Ext. Temp. °F       | _____                                     |
|                                    |                | 61. 4th Pt.Htr.F.W.Out Temp. °F    | _____                                     |
|                                    |                | 62. 5th Pt.Htr.Ext. Press.In.Hg    | _____                                     |
|                                    |                | 63. 5th Pt.Htr.Ext. Temp. °F       | _____                                     |
|                                    |                | 64. 5th Pt.Htr.F.W.In Temp. °F     | _____                                     |
|                                    |                | 65. 5th Pt.Htr.F.W.Out Temp. °F    | _____                                     |
|                                    |                | 66. 1st Pt.F.W.Out Temp.Minus(-)   | _____                                     |
|                                    |                | 5th Pt.F.W. In Temp. °F -          | _____                                     |
|                                    |                | 67. 1st Pt. Drain Temp. °F         | _____                                     |
|                                    |                | 68. 2nd Pt. Drain Temp. °F         | _____                                     |
|                                    |                | 69. 3rd Pt. Drain Temp. °F         | _____                                     |
|                                    |                | 70. 4th Pt. Drain Temp. °F         | _____                                     |
|                                    |                | 71. 5th Pt. Drain Temp. °F         | _____                                     |
|                                    |                | 72. Vars - Mvar                    | _____                                     |
|                                    |                | 73. Generator Voltage - K volts    | _____                                     |
|                                    |                | 74. Auxiliary Steam Uses:          | _____                                     |
|                                    |                | 75. Remarks: <u>NOTP</u>           | _____                                     |
|                                    |                |                                    | <u>B- Baghouse</u>                        |
|                                    |                |                                    | <u>INLET TEMP 311 OUTLET TEMP 301</u>     |
|                                    |                |                                    | <u>INLET PRESS - 13 OUTLET PRESS - 16</u> |

③④ Coal Total Lbs. Hr. 45200

J. Berman  
CRO Engineer

PRESQUE ISLE POWER PLANT LOAD TEST DATA (Units 1-9)

123

UNIT NO.: A-Baghouse <sup>14</sup> 3

TIME: 1500-1600

DATE: 07-16-95

- ① Gross Generation - MWH 48.420
- ② Station Service - MWH 3.00
- ③ Net Generation - MWH 45.420
- ④ Control Valve Position % -
- ⑤ Main Steam Flow Lbs./Hr. 256.500
- ⑥ F.W. Flow Lbs./Hr. 337.500
- ⑦ F.W. Press. Psig 180
- ⑧ Chart Throttle Press. Psig -
- ⑨ Test Gauge Throttle Press. Psig -
- ⑩ First Stage Press. Psig 825
- ⑪ Cold Reheat Press. Psig 345
- ⑫ Hot Reheat Press. Psig 315
- ⑬ F.W. (Loading/Temp.) 1448/439
- ⑭ Main Steam Temp. °F 957
- ⑮ Cold Reheat Temp. °F 625
- ⑯ Hot Reheat Temp. °F 1009
- ⑰ Superheat Spray Flow 0
- ⑱ Reheat Spray Flow 0
- ⑲ Air Flow 360,000
- ⑳ Excess Oxygen % 3.4
- ㉑ Inlet Air Temp. °F 107E
- ㉒ Gas Outlet Temp. °F 107B
- ㉓ Opacity % -
- ㉔ I.D. Fan (Loading/Amps) 299
- ㉕ F.D. Fan (Loading/rpm/Amps) 1748/64
- ㉖ Air Heater Press. (H2O)

	IN	OUT	P
AIR	<u>7.0</u>	<u>3.5</u>	<u>3.5</u>
GAS	<u>-3.2</u>	<u>-7.7</u>	<u>-4.7</u>

- 27. Burner Tilt Position/RH P -
- 28. Condensate Pump Amps A. - B. -
- 29. Boiler Feed Pump Amps A. - B. -
- 30. Coal Feeder Loading A. - B. -
- 31. Pulverizer Amps A. - B. -
- 32. Mill Outage Temp. A. - B. -
- 33. Coal Scale Readings:

	Beginning	Ending	Total
a	<u>81141</u>	<u>81197</u>	<u>56</u>
b	<u>81387</u>	<u>81430</u>	<u>43</u>
c	<u>-</u>	<u>-</u>	<u>99</u>
d	<u>-</u>	<u>-</u>	<u>2400</u>

- 34. Coal Total Lbs. Hr. 39600

- ⑳ Lbs. Coal/Net KWH 18718
- ㉑ Lbs. Steam/Net KWH 5.647
- 38. Barometric Press. In.Hg -
- 39. Vacuum In.Hg -
- 40. Back Press. In.Hg -
- 41. Circ. Water Pump Amps A. - B. -
- 42. Circ. Water Inlet Temp. °F -
- 43. Circ. Water Outlet Temp. °F -
- 44. Circ. Water Inlet Press. Psig -
- 45. Circ. Water Outlet Press. Psig -
- 46. Condensate Make-up -
- 47. Condensate Draw-off -
- 48. Hot Well Temp. °F -
- 49. Turbine Exhaust Temp. °F -
- 50. 1st Pt.Htr.Ext.Press. Psig -
- 51. 1st Pt.Htr.Ext.Temp. °F -
- 52. 1st Pt.Htr.F.W.Out Temp. °F -
- 53. 2nd Pt.Htr.Ext.Press. Psig -
- 54. 2nd Pt.Htr.Ext. Temp. °F -
- 55. 2nd Pt.Htr.F.W.Out Temp. °F -
- 56. 3rd Pt.Htr.Ext. Press. Psig -
- 57. 3rd Pt.Htr.Ext. Temp. °F -
- 58. 3rd Pt.Htr.F.W.Out Temp. °F -
- 59. 4th Pt.Htr.Ext.Press. Psig -
- 60. 4th Pt.Htr.Ext. Temp. °F -
- 61. 4th Pt.Htr.F.W.Out Temp. °F -
- 62. 5th Pt.Htr.Ext. Press.In.Hg -
- 63. 5th Pt.Htr.Ext. Temp. °F -
- 64. 5th Pt.Htr.F.W.In Temp. °F -
- 65. 5th Pt.Htr.F.W.Out Temp. °F -
- 66. 1st Pt.F.W.Out Temp.Minus(-) -
- 67. 5th Pt.F.W. In Temp. °F -
- 67. 1st Pt. Drain Temp. °F -
- 68. 2nd Pt. Drain Temp. °F -
- 69. 3rd Pt. Drain Temp. °F -
- 70. 4th Pt. Drain Temp. °F -
- 71. 5th Pt. Drain Temp. °F -
- 72. Vars - Mvar -
- 73. Generator Voltage - K volts -
- 74. Auxiliary Steam Uses: -

NOTE

75. Remarks: A-Baghouse  
INLET TEMP 314 OUTLET TEMP 301  
INLET PRESS 12 OUTLET PRESS -

CRO

Engineer



Plant Name: PIPP  
 General Average Report

Reporting Period: 07/15/1999 to 07/16/1999

Site Name: PIPPF4P4

Data Averaging Type: 1h

Time of Report: 01/11/00 14:07  
 Rolling Average Interval: 1

Date	Time	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/15/99	22:00	0.	1.	46.	48.
	23:00	0.	1.	46.	48.
07/16/99	00:00	0.	1.	46.	48.
	01:00	0.	1.	43.	47.
	02:00	0.	11.	35.	39.
	03:00	1.	26.	35.	38.
	04:00	1.	26.	35.	38.
	05:00	1.	26.	45.	45.
	06:00	1.	26.	49.	49.
	07:00	1.	26.	49.	49.
	08:00	1.	26.	49.	49.
	09:00	1.	26.	49.	49.
	10:00	1.	26.	49.	49.
	11:00	2.	26.	49.	49.
	12:00	10.	26.	48.	49.
	13:00	15.	26.	48.	50.
	14:00	16.	26.	48.	49.
	15:00	16.	26.	48.	49.
	16:00	16.	26.	48.	49.
	17:00	16.	26.	48.	49.
	18:00	16.	26.	48.	49.
	19:00	16.	26.	47.	49.
	20:00	16.	26.	47.	49.
	21:00	16.	26.	47.	49.
22:00	15.	26.	47.	49.	
-----					
Average =		7.	21.	46.	47.
Maximum =		15.	26.	49.	50.
Minimum =		0.	1.	35.	38.
Possible Values =	25	25	25	25	25
Included Values =	25	25	25	25	25
Total =		178.	529.	1149.	1187.

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect
- V - invalid for state
- H - exceedance
- F - stack not operating
- B - invalid (PADER)
- U - missing data substituted
- 999 - missing value
- 888 - value could not be calculated

## General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4

Time of Report: 11/01/99 11:54

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	07:20	125.	0.	26.	49.	50.
	07:21	125.	0.	26.	49.	50.
	07:22	125.	0.	26.	49.	50.
	07:23	124.	0.	26.	49.	49.
	07:24	124.	0.	26.	49.	49.
	07:25	124.	0.	26.	49.	49.
	07:26	124.	0.	26.	49.	49.
	07:27	124.	0.	26.	49.	49.
	07:28	125.	0.	26.	49.	49.
	07:29	125.	0.	26.	49.	50.
	07:30	125.	0.	26.	49.	50.
	07:31	125.	0.	26.	49.	49.
	07:32	125.	0.	26.	49.	49.
	07:33	125.	0.	26.	49.	49.
	07:34	125.	0.	26.	49.	49.
	07:35	125.	0.	26.	49.	49.
	07:36	125.	0.	26.	49.	49.
	07:37	124.	0.	26.	49.	49.
	07:38	124.	0.	26.	49.	49.
	07:39	124.	0.	26.	49.	49.
	07:40	124.	0.	26.	49.	49.
	07:41	124.	0.	26.	49.	50.
	07:42	124.	0.	26.	49.	49.
	07:43	125.	0.	26.	49.	49.
	07:44	125.	0.	26.	49.	49.
	07:45	125.	0.	26.	49.	49.
	07:46	125.	0.	26.	50.	49.
	07:47	124.	0.	26.	49.	49.
	07:48	124.	0.	26.	49.	49.
	07:49	124.	0.	26.	49.	49.
	07:50	124.	0.	26.	49.	49.
	07:51	124.	0.	26.	49.	49.
	07:52	125.	0.	26.	50.	49.
	07:53	124.	0.	26.	50.	49.
	07:54	124.	0.	26.	49.	49.
	07:55	124.	0.	26.	49.	49.
	07:56	124.	0.	26.	49.	49.
	07:57	124.	0.	26.	49.	49.
	07:58	123.	0.	26.	49.	49.
	07:59	123.	0.	26.	49.	49.
	08:00	124.	0.	26.	49.	49.
	08:01	124.	0.	26.	49.	49.
	08:02	125.	0.	26.	50.	49.
	08:03	125.	0.	26.	50.	49.
	08:04	125.	0.	26.	50.	49.
	08:05	125.	0.	26.	50.	49.
	08:06	125.	0.	26.	49.	50.
	08:07	125.	0.	26.	49.	50.
	08:08	125.	0.	26.	49.	50.
	08:09	125.	0.	26.	49.	50.

Plant Name: PIPP  
General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4

Time of Report: 11/01/99 11:54

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	08:10	124.	0.	26.	49.	50.
	08:11	124.	0.	26.	49.	50.
	08:12	124.	0.	26.	49.	50.
	08:13	125.	0.	26.	49.	50.
	08:14	125.	0.	26.	49.	50.
	08:15	125.	0.	26.	49.	50.
	08:16	125.	0.	26.	49.	50.
	08:17	125.	0.	26.	50.	50.
	08:18	125.	0.	26.	50.	49.
	08:19	125.	0.	26.	50.	49.
	08:20	125.	0.	26.	50.	49.
	08:21	125.	0.	26.	50.	49.
	08:22	124.	0.	26.	49.	49.
	08:23	124.	0.	26.	49.	49.
	08:24	124.	0.	26.	49.	49.
	08:25	124.	0.	26.	49.	49.
	08:26	124.	0.	26.	49.	49.
	08:27	124.	0.	26.	49.	49.
	08:28	124.	0.	26.	49.	49.
	08:29	124.	0.	26.	49.	49.
	08:30	124.	0.	26.	50.	49.
	08:31	125.	0.	26.	50.	49.
	08:32	125.	0.	26.	50.	49.
	08:33	125.	0.	26.	50.	49.
	08:34	125.	0.	26.	50.	50.
	08:35	125.	0.	26.	49.	50.
	08:36	125.	0.	26.	49.	50.
	08:37	125.	0.	26.	49.	50.
	08:38	125.	0.	26.	49.	50.
	08:39	125.	0.	26.	49.	50.
	08:40	124.	0.	26.	49.	50.
	08:41	125.	0.	26.	49.	50.
	08:42	125.	0.	26.	49.	50.
	08:43	125.	0.	26.	49.	50.
	08:44	125.	0.	26.	50.	50.
	08:45	125.	0.	26.	50.	50.
	08:46	126.	0.	26.	50.	50.
	08:47	126.	0.	26.	50.	49.
	08:48	125.	0.	26.	50.	49.
	08:49	125.	0.	26.	50.	49.
	08:50	124.	0.	26.	49.	49.
	08:51	123.	0.	26.	49.	49.
	08:52	123.	0.	26.	48.	49.
	08:53	122.	0.	26.	48.	48.
	08:54	122.	0.	26.	48.	48.
	08:55	122.	0.	26.	48.	48.
	08:56	122.	0.	26.	48.	48.
	08:57	123.	0.	26.	48.	48.
	08:58	122.	0.	26.	48.	48.
	08:59	122.	0.	26.	47.	48.

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPFF4P4  
 Data Averaging Type: 1m

Time of Report: 11/01/99 11:54  
 Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	09:00	122.	0.	26.	47.	48.
	09:01	121.	0.	26.	47.	49.
	09:02	121.	0.	26.	46.	49.
	09:03	121.	0.	26.	46.	49.
	09:04	122.	0.	26.	47.	49.
	09:05	122.	0.	26.	47.	49.
	09:06	123.	0.	26.	47.	49.
	09:07	123.	0.	26.	48.	50.
	09:08	124.	0.	26.	48.	50.
	09:09	125.	0.	26.	49.	50.
	09:10	125.	0.	26.	49.	50.
	09:11	125.	0.	26.	50.	50.
	09:12	125.	0.	26.	50.	50.
	09:13	125.	0.	26.	50.	49.
	09:14	125.	0.	26.	50.	49.
	09:15	124.	0.	26.	50.	49.
	09:16	124.	0.	26.	49.	49.
	09:17	124.	0.	26.	49.	49.
	09:18	124.	0.	26.	49.	49.
	09:19	124.	0.	26.	49.	49.
	09:20	124.	0.	26.	49.	49.
	09:21	124.	0.	26.	49.	49.
	09:22	124.	0.	26.	48.	49.
	09:23	124.	0.	26.	48.	50.
	09:24	124.	0.	26.	48.	50.
	09:25	124.	0.	26.	48.	50.
	09:26	124.	0.	26.	48.	50.
	09:27	124.	0.	26.	48.	49.
	09:28	124.	0.	26.	48.	49.
	09:29	124.	0.	26.	49.	49.
	09:30	124.	0.	26.	49.	49.
	09:31	124.	0.	26.	49.	49.
	09:32	125.	0.	26.	50.	49.
	09:33	-999F	-999F	-999F	-999F	-999F
	09:34	-999F	-999F	-999F	-999F	-999F
	09:35	-999F	-999F	-999F	-999F	-999F
	09:36	-999F	-999F	-999F	-999F	-999F
	09:37	-999F	-999F	-999F	-999F	-999F

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Average =	124.	0.	26.	49.	49.
Maximum =	126.	0.	26.	50.	50.
Minimum =	121.	0.	26.	46.	48.
Possible Values =	138	138	138	138	138
Included Values =	133	133	133	133	133
Total =	16524.	0.	3456.	6515.	6552.

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect
- V - invalid for state
- H - exceedance
- F - stack not operating
- B - invalid (PADER)
- U - missing data substituted
- 999 - missing value

Plant Name: PIPP  
General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
Data Averaging Type: 1m

Time of Report: 11/01/99 11:54  
Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	10:15	125.	0.	26.	49.	50.
	10:16	125.	0.	26.	49.	50.
	10:17	125.	0.	26.	49.	49.
	10:18	125.	0.	26.	49.	49.
	10:19	125.	0.	26.	49.	50.
	10:20	125.	0.	26.	49.	50.
	10:21	124.	0.	26.	49.	50.
	10:22	124.	0.	26.	49.	50.
	10:23	124.	0.	26.	49.	50.
	10:24	124.	0.	26.	49.	49.
	10:25	124.	0.	26.	49.	50.
	10:26	124.	0.	26.	49.	50.
	10:27	124.	0.	26.	49.	49.
	10:28	124.	0.	26.	49.	49.
	10:29	124.	0.	26.	49.	49.
	10:30	124.	0.	26.	49.	49.
	10:31	124.	0.	26.	49.	49.
	10:32	124.	0.	26.	49.	49.
	10:33	124.	0.	26.	49.	49.
	10:34	124.	0.	26.	49.	49.
	10:35	124.	0.	26.	49.	49.
	10:36	124.	0.	26.	49.	49.
	10:37	124.	0.	26.	49.	49.
	10:38	124.	0.	26.	49.	49.
	10:39	124.	0.	26.	49.	49.
	10:40	124.	0.	26.	49.	50.
	10:41	124.	0.	26.	49.	50.
	10:42	124.	0.	26.	49.	50.
	10:43	124.	0.	26.	49.	49.
	10:44	124.	0.	26.	49.	49.
	10:45	124.	0.	26.	49.	49.
	10:46	124.	0.	26.	49.	49.
	10:47	124.	0.	26.	49.	49.
	10:48	124.	0.	26.	49.	49.
	10:49	124.	0.	26.	49.	49.
	10:50	124.	0.	26.	49.	49.
	10:51	124.	0.	26.	49.	49.
	10:52	124.	0.	26.	49.	49.
	10:53	124.	0.	26.	49.	49.
	10:54	124.	0.	26.	49.	49.
	10:55	124.	0.	26.	49.	49.
	10:56	124.	0.	26.	49.	49.
	10:57	124.	0.	26.	49.	49.
	10:58	124.	0.	26.	49.	49.
	10:59	124.	0.	26.	49.	49.
	11:00	124.	0.	26.	49.	49.
	11:01	124.	0.	26.	49.	49.
	11:02	124.	0.	26.	49.	49.
	11:03	124.	0.	26.	49.	49.
	11:04	124.	0.	26.	49.	49.

Plant Name: PIPP  
General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
Data Averaging Type: 1m

Time of Report: 11/01/99 11:54  
Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	11:05	125.	0.	26.	49.	50.
	11:06	125.	0.	26.	49.	50.
	11:07	125.	0.	26.	49.	50.
	11:08	125.	0.	26.	49.	50.
	11:09	125.	0.	26.	49.	50.
	11:10	125.	0.	26.	49.	50.
	11:11	124.	0.	26.	49.	50.
	11:12	125.	0.	26.	49.	50.
	11:13	125.	0.	26.	49.	50.
	11:14	125.	0.	26.	49.	50.
	11:15	125.	0.	26.	49.	50.
	11:16	124.	0.	26.	49.	50.
	11:17	124.	0.	26.	49.	50.
	11:18	124.	0.	26.	49.	50.
	11:19	124.	0.	26.	49.	49.
	11:20	124.	0.	26.	49.	49.
	11:21	124.	0.	26.	49.	50.
	11:22	124.	0.	26.	49.	50.
	11:23	124.	0.	26.	49.	50.
	11:24	124.	0.	26.	49.	50.
	11:25	124.	0.	26.	49.	49.
	11:26	124.	0.	26.	49.	49.
	11:27	124.	0.	26.	49.	49.
	11:28	124.	0.	26.	49.	49.
	11:29	124.	0.	26.	49.	49.
	11:30	123.	0.	26.	49.	49.
	11:31	123.	0.	26.	49.	49.
	11:32	123.	0.	26.	49.	48.
	11:33	123.	0.	26.	49.	49.
	11:34	124.	0.	26.	49.	49.
	11:35	124.	0.	26.	49.	49.
	11:36	126.	1.	26.	49.	49.
	11:37	126.	2.	26.	49.	49.
	11:38	126.	2.	26.	49.	49.
	11:39	126.	2.	26.	49.	49.
	11:40	126.	2.	26.	49.	49.
	11:41	126.	2.	26.	49.	49.
	11:42	126.	2.	26.	49.	49.
	11:43	126.	2.	26.	49.	49.
	11:44	126.	2.	26.	49.	49.
	11:45	128.	4.	26.	49.	49.
	11:46	129.	5.	26.	49.	49.
	11:47	131.	6.	26.	50.	49.
	11:48	131.	6.	26.	50.	49.
	11:49	132.	7.	26.	50.	50.
	11:50	132.	7.	26.	49.	50.
	11:51	132.	7.	26.	49.	50.
	11:52	132.	7.	26.	49.	50.
	11:53	132.	7.	26.	49.	50.
	11:54	132.	7.	26.	49.	50.

## General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPFF4P4

Time of Report: 11/01/99 11:55

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	13:10	136.	13.	25.	48.	49.
	13:11	136.	14.	25.	48.	49.
	13:12	136.	14.	25.	48.	49.
	13:13	136.	14.	25.	48.	49.
	13:14	136.	14.	25.	48.	49.
	13:15	137.	14.	25.	48.	49.
	13:16	137.	15.	25.	48.	49.
	13:17	137.	15.	25.	48.	49.
	13:18	137.	15.	26.	48.	49.
	13:19	138.	15.	26.	48.	49.
	13:20	138.	15.	26.	48.	49.
	13:21	138.	15.	26.	48.	49.
	13:22	138.	15.	26.	48.	49.
	13:23	138.	15.	26.	48.	49.
	13:24	138.	15.	26.	48.	49.
	13:25	138.	15.	26.	48.	49.
	13:26	138.	15.	26.	48.	49.
	13:27	138.	15.	26.	48.	49.
	13:28	138.	15.	26.	48.	50.
	13:29	138.	15.	26.	48.	49.
	13:30	138.	15.	26.	48.	49.
	13:31	138.	15.	26.	48.	49.
	13:32	137.	15.	26.	48.	49.
	13:33	138.	15.	26.	48.	50.
	13:34	138.	15.	26.	48.	50.
	13:35	138.	15.	26.	48.	50.
	13:36	138.	15.	26.	48.	50.
	13:37	138.	15.	25.	48.	49.
	13:38	138.	15.	25.	48.	49.
	13:39	138.	15.	25.	48.	49.
	13:40	138.	15.	26.	48.	49.
	13:41	138.	16.	26.	48.	50.
	13:42	138.	16.	26.	48.	49.
	13:43	138.	16.	25.	48.	49.
	13:44	138.	16.	25.	48.	50.
	13:45	138.	16.	25.	48.	50.
	13:46	138.	16.	25.	48.	50.
	13:47	138.	16.	26.	48.	50.
	13:48	138.	15.	26.	48.	50.
	13:49	138.	16.	25.	48.	50.
	13:50	138.	15.	25.	48.	50.
	13:51	138.	15.	26.	48.	50.
	13:52	139.	15.	26.	48.	50.
	13:53	139.	15.	26.	48.	50.
	13:54	139.	15.	26.	48.	50.
	13:55	139.	15.	26.	48.	50.
	13:56	139.	16.	26.	48.	50.
	13:57	139.	15.	26.	48.	50.
	13:58	139.	15.	26.	48.	50.
	13:59	138.	15.	26.	48.	50.

## General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPFF4P4

Time of Report: 11/01/99 11:55

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	14:00	138.	15.	25.	48.	49.
	14:01	138.	15.	26.	48.	49.
	14:02	138.	15.	26.	48.	49.
	14:03	138.	15.	26.	48.	49.
	14:04	138.	15.	26.	48.	50.
	14:05	138.	15.	25.	48.	50.
	14:06	138.	15.	26.	48.	49.
	14:07	138.	15.	25.	48.	49.
	14:08	138.	15.	25.	48.	49.
	14:09	138.	15.	26.	48.	49.
	14:10	138.	15.	26.	48.	49.
	14:11	138.	15.	26.	48.	49.
	14:12	138.	15.	26.	48.	49.
	14:13	138.	15.	26.	48.	49.
	14:14	138.	15.	26.	48.	49.
	14:15	138.	15.	26.	48.	49.
	14:16	138.	15.	26.	48.	49.
	14:17	138.	15.	26.	48.	49.
	14:18	138.	15.	26.	48.	49.
	14:19	138.	15.	26.	48.	49.
	14:20	138.	15.	25.	48.	49.
	14:21	138.	15.	25.	48.	49.
	14:22	138.	15.	25.	48.	49.
	14:23	138.	15.	25.	48.	50.
	14:24	138.	15.	25.	48.	49.
	14:25	138.	16.	25.	48.	49.
	14:26	138.	16.	26.	48.	49.
	14:27	138.	16.	26.	48.	49.
	14:28	138.	16.	26.	48.	49.
	14:29	138.	16.	26.	48.	49.
	14:30	138.	16.	26.	48.	49.
	14:31	138.	16.	26.	48.	49.
	14:32	138.	16.	26.	48.	49.
	14:33	138.	16.	26.	48.	49.
	14:34	138.	16.	26.	48.	49.
	14:35	138.	16.	26.	48.	49.
	14:36	138.	16.	25.	48.	49.
	14:37	138.	16.	25.	48.	49.
	14:38	138.	16.	25.	48.	49.
	14:39	138.	16.	25.	48.	49.
	14:40	138.	16.	25.	48.	50.
	14:41	139.	16.	25.	48.	50.
	14:42	139.	16.	25.	48.	50.
	14:43	139.	16.	25.	48.	50.
	14:44	139.	16.	26.	48.	50.
	14:45	139.	16.	26.	48.	50.
	14:46	139.	16.	26.	48.	49.
	14:47	139.	16.	26.	48.	49.
	14:48	139.	16.	26.	48.	49.
	14:49	139.	16.	26.	48.	49.

Plant Name: PIPP  
General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
Data Averaging Type: 1m

Time of Report: 11/01/99 11:55  
Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	14:50	139.	16.	26.	48.	49.
	14:51	139.	16.	26.	48.	49.
	14:52	139.	16.	26.	48.	49.
	14:53	139.	16.	26.	48.	49.
	14:54	139.	16.	26.	48.	49.
	14:55	139.	16.	26.	48.	49.
	14:56	139.	16.	26.	48.	49.
	14:57	139.	16.	26.	48.	50.
	14:58	139.	16.	26.	48.	50.
	14:59	139.	16.	26.	48.	50.
	15:00	139.	16.	26.	48.	50.
	15:01	139.	16.	26.	48.	49.
	15:02	139.	16.	26.	48.	49.
	15:03	139.	16.	26.	48.	49.
	15:04	139.	16.	26.	48.	49.
	15:05	139.	16.	26.	48.	49.
	15:06	139.	16.	26.	48.	49.
	15:07	139.	16.	26.	48.	49.
	15:08	139.	16.	26.	48.	49.
	15:09	139.	16.	26.	48.	49.
	15:10	139.	16.	26.	48.	50.
	15:11	139.	16.	26.	48.	50.
	15:12	139.	16.	25.	48.	50.
	15:13	139.	16.	25.	48.	50.
	15:14	139.	16.	25.	48.	49.
	15:15	138.	16.	25.	48.	49.
	15:16	138.	16.	25.	48.	49.
	15:17	138.	16.	25.	48.	49.
	15:18	138.	16.	25.	48.	49.
	15:19	138.	16.	25.	48.	49.
	15:20	139.	16.	26.	48.	49.
	15:21	139.	16.	26.	48.	49.
	15:22	139.	16.	26.	48.	49.
	15:23	139.	16.	26.	48.	49.
	15:24	139.	16.	26.	48.	49.
	15:25	139.	16.	26.	48.	49.
	15:26	138.	16.	25.	48.	49.
	15:27	139.	16.	25.	48.	49.
	15:28	139.	16.	25.	48.	49.
	15:29	139.	16.	25.	48.	49.
	15:30	139.	16.	26.	48.	49.
	15:31	139.	16.	26.	48.	49.
	15:32	139.	16.	26.	48.	49.
	15:33	139.	16.	26.	48.	49.
	15:34	139.	16.	25.	48.	49.
	15:35	139.	16.	26.	48.	49.
	15:36	139.	16.	26.	48.	49.
	15:37	139.	16.	26.	48.	49.
	15:38	139.	16.	26.	48.	49.
	15:39	139.	16.	26.	48.	49.

Plant Name: PIPP  
General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
Data Averaging Type: 1m

Time of Report: 11/01/99 11:55  
Rolling Average Interval: 1

Date	Time	F4MEG (MEGAWATT)	U1MEG (MEGAWATT)	U2MEG (MEGAWATT)	U3MEG (MEGAWATT)	U4MEG (MEGAWATT)
07/16/99	15:40	139.	16.	26.	48.	49.
	15:41	139.	16.	26.	48.	49.
-----						
	Average =	138.	16.	26.	48.	49.
	Maximum =	139.	16.	26.	48.	50.
	Minimum =	136.	13.	25.	48.	49.
Possible Values =		152	152	152	152	152
Included Values =		152	152	152	152	152
	Total =	21012.	2365.	3885.	7258.	7504.

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect
- V - invalid for state
- H - exceedance
- F - stack not operating
- B - invalid (PADER)
- U - missing data substituted
- 999 - missing value
- 888 - value could not be calculated

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## UNITS 1-4 CEMS DATA

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Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
 Data Averaging Type: 1m

Time of Report: 10/18/99 09:22  
 Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	07:20	11.4	297.4	504.2	125.	315.0	19.4	513.0	2.
	07:21	11.4	299.2	504.2	125.	315.6	18.8	513.0	2.
	07:22	11.3	302.0	502.2	125.	316.3	19.5	512.9	2.
	07:23	11.3	302.7	502.3	124.	316.4	21.9	511.9	2.
	07:24	11.3	302.9	504.5	124.	316.8	20.5	511.7	2.
	07:25	11.3	305.1	506.2	124.	316.8	19.9	511.8	1.
	07:26	11.3	304.0	506.9	124.	316.6	19.5	511.9	1.
	07:27	11.3	303.1	504.6	124.	316.6	20.3	511.9	1.
	07:28	11.3	302.7	505.8	125.	316.4	20.6	512.0	1.
	07:29	11.4	302.4	510.1	125.	316.3	19.3	512.1	1.
	07:30	11.4	299.5	508.9	125.	316.2	19.1	512.2	1.
	07:31	11.4	300.4	506.2	125.	316.2	17.6	512.2	1.
	07:32	11.3	302.4	505.7	125.	316.2	17.8	512.2	1.
	07:33	11.3	303.6	504.4	125.	316.3	17.4	512.3	1.
	07:34	11.3	303.3	504.6	125.	316.4	16.4	512.4	1.
	07:35	11.4	300.6	505.7	125.	316.6	16.5	512.4	1.
	07:36	11.4	300.6	505.4	125.	316.6	16.2	512.6	1.
	07:37	11.4	302.1	503.2	124.	316.3	15.5	512.7	1.
	07:38	11.3	302.7	502.7	124.	316.2	15.9	513.0	1.
	07:39	11.3	303.5	504.5	124.	317.5	16.6	513.3	1.
	07:40	11.3	303.6	505.2	124.	318.0	16.8	514.1	1.
	07:41	11.3	303.7	504.5	124.	318.0	16.8	515.6	1.
	07:42	11.4	301.6	503.1	124.	317.6	14.8	514.5	1.
	07:43	11.4	300.9	504.9	125.	317.6	14.8	514.4	1.
	07:44	11.4	301.1	507.2	125.	317.4	14.9	514.5	1.
	07:45	11.4	302.0	507.9	125.	317.2	15.3	514.7	1.
	07:46	11.4	302.4	507.7	125.	317.2	16.7	516.2	1.
	07:47	11.4	302.7	507.8	124.	317.2	14.3	515.3	1.
	07:48	11.4	301.9	507.8	124.	317.3	16.3	514.4	1.
	07:49	11.3	305.3	504.0	124.	317.7	15.9	514.1	1.
	07:50	11.3	305.7	507.0	124.	317.7	14.7	514.4	1.
	07:51	11.4	305.0	506.3	124.	318.2	16.1	514.4	1.
	07:52	11.4	303.4	505.7	125.	318.2	15.6	514.3	1.
	07:53	11.4	298.9	507.4	124.	318.3	17.5	514.1	1.
	07:54	11.4	301.2	507.4	124.	318.3	19.1	514.1	1.
	07:55	11.4	302.7	506.9	124.	317.9	19.2	513.8	1.
	07:56	11.3	304.9	505.7	124.	317.7	16.4	513.9	1.
	07:57	11.3	304.0	505.6	124.	317.7	15.9	514.1	1.
	07:58	11.3	304.2	508.6	123.	317.7	15.3	514.0	1.
	07:59	11.4	305.1	510.1	123.	317.7	16.4	513.6	1.
	08:00	11.3	305.1	508.7	124.	317.7	16.6	512.2	1.
	08:01	11.4	303.4	510.0	124.	317.7	15.7	512.1	1.
	08:02	11.4	301.3	509.3	125.	318.2	17.2	512.1	1.
	08:03	11.4	301.6	507.0	125.	318.9	16.3	512.0	1.
	08:04	11.4	303.8	508.2	125.	319.0	17.5	512.0	1.
	08:05	11.4	302.7	508.7	125.	319.4	15.8	511.9	1.
	08:06	11.4	302.1	509.2	125.	319.4	15.5	511.9	1.
	08:07	11.4	302.0	506.4	125.	318.8	16.0	511.8	1.
	08:08	11.3	302.9	506.6	125.	318.8	14.4	511.8	1.
	08:09	11.3	303.5	506.6	125.	318.8	15.3	511.9	1.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4

Time of Report: 10/18/99 09:22

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F4PCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	08:10	11.3	303.5	504.4	124.	319.1	13.3	512.0	1.
	08:11	11.3	302.6	503.2	124.	319.1	12.5	512.1	1.
	08:12	11.3	302.2	505.2	124.	319.8	13.9	512.2	1.
	08:13	11.3	302.7	504.3	125.	319.9	12.6	512.3	1.
	08:14	11.4	302.1	501.5	125.	319.4	13.6	512.3	1.
	08:15	11.4	299.2	502.4	125.	319.2	13.0	512.5	1.
	08:16	11.5	296.4	502.2	125.	319.3	13.4	512.6	1.
	08:17	11.5	296.2	503.8	125.	318.8	14.8	512.8	1.
	08:18	11.5	298.5	504.8	125.	318.8	17.7	513.3	1.
	08:19	11.5	298.7	506.4	125.	319.2	14.9	513.6	1.
	08:20	11.4	302.0	504.0	125.	319.4	15.0	513.5	1.
	08:21	11.4	302.5	501.6	125.	319.5	17.2	513.3	1.
	08:22	11.3	302.8	499.2	124.	319.6	14.8	513.7	1.
	08:23	11.4	301.2	497.4	124.	319.4	14.6	514.2	1.
	08:24	11.4	302.0	496.6	124.	318.8	14.0	514.7	1.
	08:25	11.4	304.2	498.3	124.	318.8	13.7	515.8	1.
	08:26	11.3	303.4	499.1	124.	319.4	12.9	516.5	1.
	08:27	11.3	304.6	498.4	124.	319.4	15.2	514.3	2.
	08:28	11.3	306.4	498.7	124.	319.1	15.3	513.7	2.
	08:29	11.3	307.6	500.2	124.	318.9	20.1	514.1	2.
	08:30	11.4	307.3	504.3	124.	320.2	25.4	514.9	2.
	08:31	11.5	305.2	505.0	125.	320.6	77.4	515.9	2.
	08:32	11.5	302.6	501.5	125.	319.9	77.8	521.0	2.
	08:33	11.5	302.1	500.5	125.	318.9	54.8	520.2	2.
	08:34	11.6	300.2	502.7	125.	319.2	45.6	522.1	2.
	08:35	11.5	302.6	500.4	125.	319.7	40.7	518.2	2.
	08:36	11.5	302.1	494.9	125.	319.7	37.8	517.7	2.
	08:37	11.5	300.2	495.4	125.	320.3	37.8	518.3	2.
	08:38	11.5	301.5	495.6	125.	320.6	37.1	518.6	2.
	08:39	11.5	303.8	493.5	125.	320.7	39.9	520.2	2.
	08:40	11.4	305.6	493.1	124.	320.9	39.6	523.5	2.
	08:41	11.5	305.1	492.3	125.	320.8	40.0	525.0	2.
	08:42	11.4	306.0	493.6	125.	319.9	40.3	517.8	2.
	08:43	11.5	304.4	494.6	125.	319.9	38.4	515.7	2.
	08:44	11.5	302.8	497.4	125.	320.3	36.2	515.8	1.
	08:45	11.6	302.3	496.8	125.	320.3	37.4	518.6	1.
	08:46	11.5	301.4	495.3	126.	320.4	37.1	517.7	1.
	08:47	11.6	301.9	493.6	126.	320.5	36.4	515.9	1.
	08:48	11.5	298.8	491.8	125.	320.7	38.4	518.6	1.
	08:49	11.5	301.8	493.1	125.	321.1	39.0	524.2	1.
	08:50	11.4	304.0	491.8	124.	320.9	38.1	520.8	1.
	08:51	11.4	306.0	491.6	123.	320.6	35.6	519.9	1.
	08:52	11.3	307.0	492.0	123.	320.8	36.9	519.1	1.
	08:53	11.3	309.6	493.5	122.	321.5	38.4	519.4	1.
	08:54	11.3	311.1	496.6	122.	321.5	38.8	518.3	1.
	08:55	11.3	311.2	497.1	122.	321.4	40.3	518.3	1.
	08:56	11.3	310.9	497.6	122.	321.4	40.5	518.4	1.
	08:57	11.4	309.2	499.6	123.	321.1	43.0	518.7	1.
	08:58	11.5	307.0	499.6	122.	320.6	43.9	518.3	1.
	08:59	11.5	309.8	499.1	122.	320.8	43.2	517.8	1.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
 Data Averaging Type: 1m

Time of Report: 10/18/99 09:22  
 Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	09:00	11.3	314.5	497.5	122.	322.0	42.6	517.2	1.
	09:01	11.3	316.1	497.7	121.	322.0	42.3	517.0	1.
	09:02	11.2	315.3	496.4	121.	322.0	39.0	516.5	1.
	09:03	11.2	314.3	496.2	121.	322.0	37.5	516.3	1.
	09:04	11.2	313.0	497.8	122.	322.3	38.4	515.1	1.
	09:05	11.3	309.1	501.0	122.	322.5	38.5	515.0	1.
	09:06	11.4	307.6	502.5	123.	322.2	36.6	515.0	1.
	09:07	11.4	306.8	500.1	123.	322.0	38.7	514.9	1.
	09:08	11.5	304.4	498.4	124.	322.1	36.5	514.4	1.
	09:09	11.5	305.2	497.4	125.	322.3	39.0	514.2	1.
	09:10	11.5	302.2	494.6	125.	322.4	37.4	514.2	1.
	09:11	11.5	302.3	497.0	125.	322.8	35.3	514.2	1.
	09:12	11.5	303.8	497.3	125.	322.8	37.2	514.2	1.
	09:13	11.4	306.0	495.4	125.	321.8	36.6	514.2	1.
	09:14	11.5	305.5	497.1	125.	321.5	35.7	514.2	1.
	09:15	11.4	306.6	496.9	124.	321.7	36.6	514.3	1.
	09:16	11.3	307.1	497.1	124.	321.7	35.8	514.2	1.
	09:17	11.4	305.1	496.3	124.	321.8	37.4	514.2	1.
	09:18	11.4	305.0	497.3	124.	321.9	38.0	514.3	1.
	09:19	11.4	306.5	496.9	124.	321.8	41.0	514.3	1.
	09:20	11.5	305.7	497.5	124.	321.5	42.6	514.4	1.
	09:21	11.5	302.2	498.4	124.	321.5	41.8	514.5	1.
	09:22	11.6	302.8	497.2	124.	320.8	43.5	514.6	1.
	09:23	11.5	302.7	494.2	124.	320.8	40.7	514.6	1.
	09:24	11.5	302.5	491.7	124.	321.7	37.6	514.7	1.
	09:25	11.5	302.8	493.2	124.	321.9	38.0	514.8	1.
	09:26	11.5	304.2	495.0	124.	322.3	36.3	514.9	1.
	09:27	11.4	305.1	496.0	124.	322.9	36.1	515.1	1.
	09:28	11.4	303.3	497.2	124.	322.7	36.1	515.3	1.
	09:29	11.5	304.0	498.5	124.	322.0	35.9	515.4	1.
	09:30	11.4	302.5	497.9	124.	322.0	37.3	515.4	1.
	09:31	11.5	304.5	497.9	124.	322.3	40.0	515.4	1.
	09:32	11.5	303.9	498.1	125.	322.3	40.8	515.4	1.
	09:33	-999F	-999F	-999F	-999F	-999F	-999F	-999F	-999F
	09:34	-999F	-999F	-999F	-999F	-999F	-999F	-999F	-999F
	09:35	-999F	-999F	-999F	-999F	-999F	-999F	-999F	-999F
	09:36	-999F	-999F	-999F	-999F	-999F	-999F	-999F	-999F
	09:37	-999F	-999F	-999F	-999F	-999F	-999F	-999F	-999F
-----									
	Average =	11.4	303.9	501.1	124.	319.5	27.6	514.9	1.
	Maximum =	11.6	316.1	510.1	126.	322.9	77.8	525.0	2.
	Minimum =	11.2	296.2	491.6	121.	315.0	12.5	511.7	1.
Possible Values =	138	138	138	138	138	138	138	138	138
Included Values =	133	133	133	133	133	133	133	133	133
Total =	1516.1	40414.2	66643.7	16524.	42495.5	3666.8	68486.7	176.	

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect
- V - invalid for state
- H - exceedance
- F - stack not operating
- B - invalid (PADER)
- U - missing data substituted
- 999 - missing value

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
 Data Averaging Type: 1m

Time of Report: 10/18/99 09:28  
 Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	10:15	11.6	295.1	508.5	125.	324.5	17.4	515.5	1.
	10:16	11.6	297.0	506.1	125.	324.3	17.6	515.3	1.
	10:17	11.6	299.7	505.5	125.	325.6	17.5	515.2	1.
	10:18	11.6	297.0	506.7	125.	325.8	17.6	515.2	1.
	10:19	11.6	298.5	505.3	125.	325.8	16.6	515.3	1.
	10:20	11.5	298.6	505.8	125.	325.4	16.6	515.0	1.
	10:21	11.6	297.9	506.1	124.	325.4	16.7	514.8	1.
	10:22	11.6	295.9	504.6	124.	325.0	17.8	514.8	1.
	10:23	11.6	298.6	506.9	124.	324.9	16.4	514.8	1.
	10:24	11.6	299.4	507.6	124.	325.6	16.4	514.8	1.
	10:25	11.6	299.5	507.9	124.	326.0	17.4	514.8	1.
	10:26	11.5	300.3	508.2	124.	325.8	18.4	514.7	1.
	10:27	11.6	298.7	509.7	124.	325.5	16.7	514.7	1.
	10:28	11.6	302.1	512.8	124.	325.5	20.3	514.2	1.
	10:29	11.5	301.3	510.3	124.	325.7	18.2	514.1	1.
	10:30	11.6	301.1	510.6	124.	325.7	18.7	514.2	1.
	10:31	11.6	302.3	512.7	124.	326.3	18.5	514.5	1.
	10:32	11.6	301.7	511.6	124.	326.3	17.2	514.4	1.
	10:33	11.6	303.2	510.6	124.	326.1	18.7	514.4	1.
	10:34	11.5	303.5	512.1	124.	326.1	18.3	514.5	1.
	10:35	11.6	306.4	513.9	124.	326.6	18.2	514.5	1.
	10:36	11.5	306.1	512.4	124.	326.9	18.0	514.4	1.
	10:37	11.6	303.2	513.1	124.	326.4	16.7	514.5	1.
	10:38	11.6	302.1	513.4	124.	326.0	18.1	514.7	2.
	10:39	11.6	302.6	514.4	124.	326.0	18.3	515.0	1.
	10:40	11.6	303.2	514.1	124.	326.3	18.1	515.3	1.
	10:41	11.6	302.4	514.1	124.	326.3	20.2	515.8	1.
	10:42	11.6	301.7	514.2	124.	326.3	18.7	516.4	1.
	10:43	11.6	302.6	513.2	124.	326.3	19.5	519.9	1.
	10:44	11.6	303.8	512.1	124.	326.7	19.4	520.2	1.
	10:45	11.5	305.0	512.6	124.	327.0	19.1	516.9	1.
	10:46	11.5	303.5	514.7	124.	327.0	18.6	516.5	1.
	10:47	11.6	305.3	517.4	124.	326.7	19.1	516.3	1.
	10:48	11.6	304.8	516.2	124.	326.7	20.0	516.4	1.
	10:49	11.6	304.4	514.9	124.	326.9	19.6	516.4	1.
	10:50	11.6	303.1	514.2	124.	326.9	19.7	516.6	1.
	10:51	11.5	304.0	510.2	124.	326.5	18.3	521.5	1.
	10:52	11.6	301.8	513.2	124.	326.1	19.6	521.4	1.
	10:53	11.6	301.3	515.2	124.	326.1	17.7	528.1	1.
	10:54	11.6	302.2	513.9	124.	326.0	18.7	518.3	1.
	10:55	11.6	302.2	514.6	124.	326.0	19.2	518.8	1.
	10:56	11.6	302.5	511.4	124.	326.7	19.5	516.5	1.
	10:57	11.5	302.7	512.2	124.	326.7	22.7	522.4	1.
	10:58	11.6	304.1	515.1	124.	325.8	21.4	517.7	1.
	10:59	11.5	304.2	512.9	124.	325.8	20.6	514.8	1.
	11:00	11.5	305.9	512.7	124.	326.0	19.8	514.6	1.
	11:01	11.5	305.3	514.7	124.	326.4	20.4	514.5	1.
	11:02	11.6	304.8	514.7	124.	326.7	20.8	514.5	1.
	11:03	11.6	303.2	513.7	124.	327.0	20.7	514.6	1.
	11:04	11.5	303.8	511.7	124.	327.2	19.4	516.0	1.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPP4P4

Time of Report: 10/18/99 09:28

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	11:05	11.6	301.5	513.1	125.	327.3	19.5	516.4	1.
	11:06	11.7	300.0	510.2	125.	326.9	19.1	515.7	1.
	11:07	11.6	300.6	504.9	125.	325.9	18.0	514.1	1.
	11:08	11.7	300.2	504.2	125.	325.9	18.6	513.7	1.
	11:09	11.7	299.3	506.2	125.	325.6	19.4	513.6	1.
	11:10	11.6	301.6	507.2	125.	325.6	17.4	513.6	1.
	11:11	11.6	303.4	508.9	124.	326.1	17.2	513.6	1.
	11:12	11.6	304.0	509.6	125.	326.1	17.5	513.5	1.
	11:13	11.6	302.1	506.7	125.	327.3	16.5	513.5	1.
	11:14	11.7	299.8	506.7	125.	327.5	17.3	513.6	1.
	11:15	11.7	301.9	502.7	125.	326.6	17.1	513.7	1.
	11:16	11.6	301.8	501.7	124.	326.6	16.7	514.2	1.
	11:17	11.7	303.4	503.2	124.	326.9	17.7	521.7	1.
	11:18	11.7	305.3	504.6	124.	327.0	16.6	517.8	1.
	11:19	11.7	304.4	502.9	124.	326.9	18.0	514.9	1.
	11:20	11.7	304.4	498.9	124.	326.9	17.3	514.3	1.
	11:21	11.6	303.2	496.2	124.	326.9	16.2	514.1	1.
	11:22	11.6	303.6	497.1	124.	327.9	16.7	514.0	1.
	11:23	11.7	301.5	495.1	124.	327.9	18.6	514.0	1.
	11:24	11.6	304.7	493.9	124.	327.9	19.5	514.1	1.
	11:25	11.6	304.3	496.6	124.	327.9	19.6	514.2	1.
	11:26	11.6	307.1	498.7	124.	328.5	20.3	514.4	1.
	11:27	11.6	307.1	499.7	124.	328.7	18.2	515.1	1.
	11:28	11.5	306.9	498.7	124.	328.7	16.4	520.6	1.
	11:29	11.6	304.5	498.2	124.	328.6	17.9	515.5	1.
	11:30	11.6	306.5	501.1	123.	328.6	18.2	512.7	1.
	11:31	11.6	308.4	501.7	123.	328.6	17.8	512.5	2.
	11:32	11.5	308.8	503.4	123.	328.6	17.5	512.3	2.
	11:33	11.5	308.8	504.2	123.	328.3	18.6	512.2	2.
	11:34	11.6	307.7	507.1	124.	328.0	20.3	512.2	2.
	11:35	11.6	306.4	505.4	124.	328.0	21.1	512.1	2.
	11:36	11.6	306.1	503.4	126.	328.4	21.7	512.1	2.
	11:37	11.6	303.5	503.7	126.	328.7	20.6	512.1	2.
	11:38	11.7	304.1	504.9	126.	329.1	23.4	512.1	2.
	11:39	11.6	306.1	505.3	126.	329.8	23.4	512.0	2.
	11:40	11.6	307.2	505.7	126.	329.4	24.2	512.0	2.
	11:41	11.6	312.6	506.9	126.	328.9	24.9	512.0	2.
	11:42	11.7	316.5	512.2	126.	328.9	23.1	512.0	2.
	11:43	11.8	319.3	514.9	126.	328.8	21.6	512.0	2.
	11:44	11.8	320.2	514.7	126.	328.8	22.5	512.0	2.
	11:45	11.8	320.6	515.4	128.	328.5	23.5	512.0	2.
	11:46	11.8	322.3	516.6	129.	327.9	22.6	512.0	2.
	11:47	11.8	321.3	518.2	131.	327.9	24.6	512.0	2.
	11:48	11.9	321.8	516.4	131.	327.8	23.3	512.0	1.
	11:49	12.0	316.9	517.1	132.	327.8	21.5	512.0	1.
	11:50	12.0	316.6	518.1	132.	327.9	20.9	512.0	2.
	11:51	11.9	317.6	517.2	132.	327.9	20.6	512.1	2.
	11:52	11.9	318.2	518.4	132.	328.4	18.3	512.1	1.
	11:53	12.0	318.6	521.4	132.	328.4	19.9	512.2	1.
	11:54	12.0	320.5	524.4	132.	328.1	20.6	512.3	1.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPFF4P4  
 Data Averaging Type: 1m

Time of Report: 10/18/99 09:28  
 Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	11:55	12.1	319.6	522.7	132.	327.9	19.5	512.3	2.
	11:56	11.9	323.6	521.4	131.	328.1	18.3	512.4	2.
	11:57	11.8	327.0	519.9	130.	328.2	19.7	512.5	1.
	11:58	11.8	329.3	516.9	130.	328.4	16.9	512.5	1.
	11:59	11.8	327.0	518.6	130.	329.3	17.4	512.6	1.
	12:00	11.8	327.4	519.9	129.	329.3	19.2	512.7	2.
	12:01	11.8	328.0	519.2	130.	328.5	15.5	512.9	1.
	12:02	11.9	326.8	521.1	130.	328.5	16.0	513.0	1.
	12:03	12.0	327.0	524.9	130.	328.5	16.7	512.9	1.
	12:04	12.0	327.3	525.7	130.	328.4	17.4	512.9	1.
	12:05	11.9	328.0	523.9	130.	328.5	17.5	512.9	1.
	12:06	11.9	327.0	523.2	130.	329.2	16.8	512.9	1.
	12:07	11.9	328.2	524.4	130.	329.1	16.4	512.9	2.
	12:08	11.9	328.1	525.7	130.	327.8	17.2	512.9	1.
	12:09	11.9	329.6	525.2	130.	327.8	18.3	512.9	1.
	12:10	11.9	330.1	523.6	130.	328.0	17.1	512.8	1.
	12:11	11.9	328.4	525.9	130.	328.1	17.6	512.9	1.
	12:12	11.9	329.3	521.6	130.	328.5	18.2	512.9	1.
	12:13	11.9	328.9	521.7	130.	328.7	18.4	512.9	1.
	12:14	11.9	328.0	520.1	130.	328.7	17.2	512.9	2.
	12:15	12.0	327.8	520.1	130.	328.6	18.5	513.0	2.
	12:16	12.0	329.2	518.4	130.	328.6	17.8	512.9	1.
	12:17	12.0	329.4	521.4	130.	328.9	19.0	513.0	1.
	12:18	12.0	330.0	520.4	130.	328.9	18.0	513.0	1.
	12:19	12.0	329.7	524.1	131.	328.2	18.0	513.1	1.
	12:20	12.0	330.1	526.6	131.	328.1	18.9	513.1	1.
	12:21	12.2	327.4	527.6	131.	327.9	18.5	513.2	2.
	12:22	12.1	323.2	522.7	131.	327.8	21.4	513.2	1.
	12:23	12.1	324.9	521.7	131.	327.9	20.5	513.2	1.
	12:24	11.9	327.0	518.9	131.	329.3	18.6	513.2	1.
	12:25	11.9	327.0	520.2	132.	329.3	20.7	513.1	2.
	12:26	11.9	328.0	522.1	132.	329.8	22.3	513.1	1.
	12:27	12.0	333.0	527.2	132.	330.1	21.5	513.1	1.
	12:28	12.0	335.0	529.1	132.	329.5	20.0	513.1	1.
	12:29	11.9	331.2	526.1	132.	329.3	20.9	513.1	1.
	12:30	11.8	330.1	524.1	132.	329.3	21.2	513.1	1.
	12:31	11.8	333.6	525.4	133.	329.5	19.9	513.1	2.
	12:32	11.9	339.5	528.2	133.	329.4	19.9	513.1	2.
	12:33	12.0	340.3	532.9	133.	329.2	20.1	513.1	2.
	12:34	11.9	341.1	535.4	133.	329.2	18.9	513.2	2.
	12:35	12.0	339.9	535.2	133.	329.5	16.7	513.2	2.
	12:36	12.0	340.3	537.6	133.	329.6	17.5	513.2	2.
	12:37	12.1	340.5	538.6	134.	329.5	17.4	513.2	2.
	12:38	12.1	334.8	542.1	135.	329.5	16.1	513.1	2.
-----									
	Average =	11.7	312.7	514.0	127.	327.5	19.0	514.3	1.
	Maximum =	12.2	341.1	542.1	135.	330.1	24.9	528.1	2.
	Minimum =	11.5	295.1	493.9	123.	324.3	15.5	512.0	1.
Possible Values =	144	144	144	144	144	144	144	144	
Included Values =	144	144	144	144	144	144	144	144	
Total =	1689.3	45034.8	74016.8	18271.	47161.5	2729.6	74055.8	203.	

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4

Time of Report: 10/18/99 09:29

Data Averaging Type: 1m

Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	13:10	12.1	351.8	541.0	136.	331.5	20.5	514.2	2.
	13:11	12.1	347.8	542.2	136.	332.2	20.9	514.7	2.
	13:12	12.1	346.3	540.7	136.	332.1	19.9	514.9	2.
	13:13	12.1	349.0	542.5	136.	331.4	21.0	515.2	2.
	13:14	12.1	350.7	545.7	136.	331.4	19.6	515.4	1.
	13:15	12.2	351.5	544.6	137.	330.9	20.1	515.7	1.
	13:16	12.1	353.6	544.6	137.	330.8	18.7	517.7	1.
	13:17	12.1	352.9	546.2	137.	331.1	19.3	522.9	1.
	13:18	12.2	353.4	546.4	137.	331.1	17.9	520.4	1.
	13:19	12.2	354.9	545.8	138.	331.7	17.1	519.9	1.
	13:20	12.2	355.2	546.9	138.	332.5	16.0	519.5	1.
	13:21	12.2	358.1	548.1	138.	332.3	17.2	516.3	1.
	13:22	12.2	357.5	548.9	138.	331.6	18.1	515.8	1.
	13:23	12.2	359.4	546.9	138.	331.6	18.6	516.0	1.
	13:24	12.3	359.0	546.0	138.	331.5	16.4	515.5	1.
	13:25	12.2	358.4	543.2	138.	331.5	15.6	515.6	1.
	13:26	12.2	360.7	542.1	138.	331.7	16.1	515.9	1.
	13:27	12.2	361.4	545.7	138.	331.8	15.1	517.6	1.
	13:28	12.2	362.6	543.3	138.	331.1	16.1	508.7	1.
	13:29	12.1	361.8	544.7	138.	330.5	16.3	511.5	1.
	13:30	12.1	363.7	545.5	138.	330.9	15.4	512.3	1.
	13:31	12.1	364.5	546.7	138.	331.8	14.4	513.5	1.
	13:32	12.1	362.6	544.1	137.	331.8	16.0	517.9	1.
	13:33	12.2	363.6	546.6	138.	331.6	16.3	518.0	1.
	13:34	12.2	362.2	546.9	138.	331.6	14.2	519.5	1.
	13:35	12.2	361.2	546.7	138.	331.9	14.3	516.2	1.
	13:36	12.2	361.5	544.6	138.	331.9	14.2	514.7	1.
	13:37	12.2	362.1	544.2	138.	331.2	14.8	513.8	1.
	13:38	12.2	361.8	545.3	138.	331.0	15.5	513.6	1.
	13:39	12.1	364.4	547.4	138.	331.0	14.4	513.9	1.
	13:40	12.2	364.2	548.1	138.	331.0	13.6	514.1	1.
	13:41	12.1	364.8	546.7	138.	331.0	14.6	514.1	1.
	13:42	12.1	365.0	548.0	138.	331.0	13.4	514.5	1.
	13:43	12.2	366.3	547.7	138.	331.4	13.4	514.6	1.
	13:44	12.1	363.9	546.6	138.	332.1	14.2	514.6	1.
	13:45	12.1	366.4	547.4	138.	332.0	13.9	514.6	1.
	13:46	12.1	366.6	545.6	138.	330.9	15.2	514.6	1.
	13:47	12.1	364.8	546.6	138.	330.9	15.1	514.6	1.
	13:48	12.1	366.7	548.1	138.	331.7	13.9	514.7	1.
	13:49	12.1	365.6	549.2	138.	331.8	13.8	514.7	1.
	13:50	12.1	364.5	546.9	138.	331.1	17.0	514.6	1.
	13:51	12.1	367.2	548.4	138.	330.6	15.8	514.7	1.
	13:52	12.2	366.7	548.0	139.	330.5	14.0	514.8	1.
	13:53	12.1	366.0	546.1	139.	330.4	13.5	514.9	1.
	13:54	12.2	358.2	546.9	139.	330.4	14.9	515.0	1.
	13:55	12.2	357.7	544.7	139.	330.3	13.9	515.1	1.
	13:56	12.1	358.6	542.5	139.	330.4	13.6	515.2	1.
	13:57	12.1	361.5	541.7	139.	331.0	13.2	515.3	1.
	13:58	12.1	359.8	539.4	139.	331.0	13.6	515.4	1.
	13:59	12.0	362.3	538.9	138.	331.4	13.0	515.5	1.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
 Data Averaging Type: 1m

Time of Report: 10/18/99 09:29  
 Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	14:00	12.0	362.7	540.6	138.	331.6	13.1	515.3	1.
	14:01	12.1	362.5	543.7	138.	330.2	14.1	515.4	1.
	14:02	12.0	362.4	543.0	138.	329.8	12.2	515.4	1.
	14:03	12.0	362.7	541.2	138.	330.8	14.2	515.6	1.
	14:04	12.0	362.1	541.7	138.	331.2	12.1	515.7	2.
	14:05	12.1	362.3	541.9	138.	331.3	14.7	515.7	2.
	14:06	12.1	361.8	542.4	138.	331.5	12.5	515.7	2.
	14:07	12.1	359.9	542.4	138.	331.1	11.8	515.7	2.
	14:08	12.1	363.4	542.7	138.	330.4	11.6	515.7	2.
	14:09	12.1	365.9	545.8	138.	330.4	12.9	515.8	2.
	14:10	12.1	364.9	545.7	138.	330.6	12.3	515.9	2.
	14:11	12.1	363.2	544.4	138.	330.6	10.9	515.9	2.
	14:12	12.1	362.6	545.5	138.	330.6	9.7	515.8	2.
	14:13	12.1	362.1	546.2	138.	330.6	11.1	516.0	2.
	14:14	12.1	358.9	545.7	138.	330.6	12.1	516.1	2.
	14:15	12.1	360.0	545.8	138.	330.6	10.4	516.2	2.
	14:16	12.1	360.7	548.2	138.	330.8	11.5	516.3	2.
	14:17	12.1	358.5	547.2	138.	331.0	10.1	516.3	2.
	14:18	12.1	356.7	546.3	138.	330.9	11.3	516.3	2.
	14:19	12.2	357.2	548.9	138.	330.9	9.2	516.2	2.
	14:20	12.2	355.8	548.6	138.	330.8	10.7	516.2	2.
	14:21	12.2	355.7	547.4	138.	330.7	10.1	516.2	2.
	14:22	12.1	357.7	546.1	138.	330.7	10.2	516.3	2.
	14:23	12.1	359.2	545.7	138.	331.3	11.5	516.3	2.
	14:24	12.1	360.3	545.7	138.	331.3	9.9	516.3	2.
	14:25	12.1	360.5	547.6	138.	331.2	9.6	516.5	2.
	14:26	12.2	359.3	549.2	138.	331.2	8.5	516.6	2.
	14:27	12.1	360.8	548.9	138.	330.3	11.0	516.6	1.
	14:28	12.1	362.9	549.3	138.	329.9	8.8	516.6	1.
	14:29	12.2	362.5	552.5	138.	330.3	10.2	516.6	1.
	14:30	12.1	360.0	548.9	138.	330.9	9.8	516.7	1.
	14:31	12.1	360.0	549.9	138.	330.5	8.9	516.8	1.
	14:32	12.2	360.2	551.6	138.	329.9	9.1	516.9	1.
	14:33	12.2	359.8	552.0	138.	330.0	9.5	517.1	1.
	14:34	12.2	361.3	554.3	138.	331.0	9.8	517.2	1.
	14:35	12.1	363.5	553.1	138.	331.2	9.1	516.9	1.
	14:36	12.1	362.9	552.9	138.	330.3	9.1	516.7	1.
	14:37	12.1	364.4	550.7	138.	330.3	7.6	516.8	1.
	14:38	12.1	364.7	551.1	138.	330.5	9.1	516.6	1.
	14:39	12.1	363.0	552.6	138.	330.7	7.4	517.5	1.
	14:40	12.1	362.3	551.0	138.	330.7	8.8	522.1	1.
	14:41	12.2	360.0	550.2	139.	330.7	9.4	520.6	1.
	14:42	12.2	356.9	552.3	139.	330.7	11.0	522.6	1.
	14:43	12.3	359.1	554.6	139.	330.7	9.3	514.2	1.
	14:44	12.3	361.8	554.9	139.	330.6	9.2	520.1	1.
	14:45	12.3	363.9	557.7	139.	329.6	8.7	522.2	1.
	14:46	12.3	364.4	558.4	139.	329.6	7.4	517.8	1.
	14:47	12.2	364.4	555.2	139.	328.9	9.8	517.4	1.
	14:48	12.2	365.7	551.7	139.	328.9	9.9	521.8	1.
	14:49	12.2	365.5	552.5	139.	330.2	8.9	522.0	1.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPP4P4  
 Data Averaging Type: 1m

Time of Report: 10/18/99 09:29  
 Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4APFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	14:50	12.2	365.2	551.3	139.	330.6	8.8	516.9	1.
	14:51	12.2	362.9	553.0	139.	330.2	9.8	517.0	1.
	14:52	12.2	364.4	554.0	139.	329.6	9.6	517.4	1.
	14:53	12.2	362.9	555.0	139.	329.8	8.3	517.7	1.
	14:54	12.2	361.5	552.3	139.	330.4	7.8	517.9	1.
	14:55	12.2	360.8	553.2	139.	330.3	7.6	518.0	1.
	14:56	12.2	360.2	551.9	139.	330.1	6.9	518.2	1.
	14:57	12.2	359.9	550.6	139.	330.1	8.3	518.3	1.
	14:58	12.2	360.0	552.3	139.	328.7	9.0	518.6	1.
	14:59	12.3	359.7	553.4	139.	328.7	9.1	519.0	1.
	15:00	12.2	358.7	551.7	139.	329.0	7.4	519.1	1.
	15:01	12.3	360.1	552.4	139.	329.0	7.0	519.4	1.
	15:02	12.2	362.9	550.3	139.	329.5	7.7	520.2	1.
	15:03	12.2	362.7	550.8	139.	329.5	8.2	522.4	1.
	15:04	12.2	361.2	550.7	139.	328.9	5.2	527.5	1.
	15:05	12.2	360.9	551.4	139.	329.2	7.5	525.0	1.
	15:06	12.1	364.2	551.1	139.	330.7	8.1	518.3	1.
	15:07	12.2	362.2	552.9	139.	330.7	6.4	518.4	1.
	15:08	12.2	360.0	550.9	139.	329.9	5.3	522.1	1.
	15:09	12.2	361.2	550.6	139.	329.8	8.6	525.3	1.
	15:10	12.3	358.9	552.5	139.	329.0	6.8	528.6	1.
	15:11	12.3	358.7	551.3	139.	329.0	5.7	528.4	1.
	15:12	12.2	359.5	551.1	139.	328.9	4.9	528.3	1.
	15:13	12.2	361.4	551.1	139.	329.2	7.0	531.2	1.
	15:14	12.2	363.0	549.8	139.	330.4	9.1	527.6	1.
	15:15	12.2	363.4	550.6	138.	330.3	7.9	521.1	1.
	15:16	12.2	365.2	549.7	138.	329.6	5.6	520.3	1.
	15:17	12.1	364.7	551.9	138.	329.7	6.6	520.2	1.
	15:18	12.1	364.7	552.8	138.	329.8	8.1	520.0	1.
	15:19	12.2	362.3	555.6	138.	329.9	7.5	527.5	1.
	15:20	12.2	360.3	555.9	139.	330.3	6.6	525.9	1.
	15:21	12.2	359.7	556.5	139.	330.1	6.8	521.4	1.
	15:22	12.3	358.9	555.4	139.	329.3	10.5	525.4	1.
	15:23	12.2	359.2	555.5	139.	329.3	7.0	524.0	1.
	15:24	12.2	359.7	552.8	139.	329.3	8.1	524.4	1.
	15:25	12.2	361.8	552.6	139.	329.5	8.3	522.5	1.
	15:26	12.2	361.4	552.5	138.	330.1	5.4	517.4	1.
	15:27	12.2	361.7	551.6	139.	330.1	6.2	518.2	1.
	15:28	12.2	361.9	550.7	139.	329.8	7.5	517.3	1.
	15:29	12.2	362.4	552.4	139.	329.8	7.7	517.3	1.
	15:30	12.2	363.0	552.9	139.	330.0	9.2	518.2	1.
	15:31	12.2	363.7	552.1	139.	330.1	6.3	519.5	1.
	15:32	12.2	364.2	551.0	139.	330.8	7.2	520.3	1.
	15:33	12.2	363.5	551.8	139.	331.0	6.1	520.7	1.
	15:34	12.2	365.0	550.4	139.	331.0	6.1	521.6	1.
	15:35	12.2	364.2	549.3	139.	331.0	6.5	522.0	1.
	15:36	12.2	362.9	550.1	139.	331.0	6.3	522.1	1.
	15:37	12.2	361.2	548.3	139.	331.0	7.2	521.4	1.
	15:38	12.2	361.6	548.9	139.	331.0	7.3	520.6	1.
	15:39	12.2	361.9	550.3	139.	330.9	6.7	520.2	1.

Plant Name: PIPP  
 General Average Report

Reporting Period: 07/16/1999 to 07/16/1999

Site Name: PIPPF4P4  
 Data Averaging Type: 1m

Time of Report: 10/18/99 09:29  
 Rolling Average Interval: 1

Date	Time	F4CPCO2 (PERCENT )	F4CPNOX (PPM )	F4CPSO2 (PPM )	F4MEG (MEGAWATT)	F4STEMP (DEGFAHRE)	F4CO (PPM )	F4AFLOW (KACFM )	F4OPC (PERCENT )
07/16/99	15:40	12.2	361.9	548.0	139.	330.9	6.6	520.6	1.
	15:41	12.2	361.9	547.8	139.	331.2	7.7	520.9	1.
-----									
	Average =	12.2	361.1	548.6	138.	330.6	11.2	518.0	1.
	Maximum =	12.3	367.2	558.4	139.	332.5	21.0	531.2	2.
	Minimum =	12.0	346.3	538.9	136.	328.7	4.9	508.7	1.
	Possible Values =	152	152	152	152	152	152	152	152
	Included Values =	152	152	152	152	152	152	152	152
	Total =	1848.3	54894.1	83389.9	21012.	50252.4	1696.9	78735.6	164.

- \* - excluded values (missing, OOC, invalid, suspect)
- < - missing
- T - out-of-control
- I - invalid
- S - suspect
- V - invalid for state
- H - exceedance
- F - stack not operating
- B - invalid (PADER)
- U - missing data substituted
- 999 - missing value
- 888 - value could not be calculated

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**APPENDIX C  
RAW TEST DATA**

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**TABLE A-1**  
**ONTARIO HYDRO METHOD DATA INPUTS**  
**Unit 6 Inlet**

<b>Test Data</b>			
	1	2	3
Run number			
Location		Unit 6 Inlet	
Date	7/14/99	7/15/99	7/15/99
Time period	1415-1640	0825-1050	1250-1510
Operator	TB	TB	TB
<b>Process Data</b>			
Unit Load, MW	74	75	75
Coal feed rate, lb/hr.	63700	64200	64000
Coal Btu content, Btu/lb. (as received)	12038	12132	12121
Heat Input, 10 <sup>6</sup> Btu/hr (F-Factor)	761.3	818.0	749.1
<b>Inputs For Calcs.</b>			
Sq. rt. delta P	0.587660	0.57170	0.58184
Delta H	1.01500	1.16667	1.20583
Stack temp. (deg.F)	309.10	307.30	307.50
Meter temp. (deg.F)	112.50	109.00	116.52
Sample volume (act.)	68.275	71.469	74.243
Barometric press. (in.Hg)	29.47	29.50	29.56
Volume H <sub>2</sub> O imp. (ml)	136.6	137.8	142.5
Weight chnge sil. gel (g)	13.3	13.4	14.3
% CO <sub>2</sub>	13.7	13.8	13.4
% O <sub>2</sub>	4.9	4.9	5.2
% N	81.4	81.3	81.4
Area of stack (sq.ft.)	151.96	151.96	151.96
Sample time (min.)	120.00	120.00	120.00
Static pressure (in.H <sub>2</sub> O)	-8.50	-8.00	-8.00
Nozzle dia. (in.)	0.253	0.267	0.267
Meter box cal.	1.0090	1.0090	1.0090
Cp of pitot tube	0.84	0.84	0.84
Traverse points	12	12	12
<b>Mercury Laboratory Report Data</b>			
Particulate bound, ug	4.3410	4.9830	5.0130
Oxidized, ug	1.0000	1.2100	1.0350
Elemental, ug	0.2700	0.4150	0.2950
<b>Total mercury catch, ug</b>	<b>5.6110</b>	<b>6.6080</b>	<b>6.3430</b>

**TABLE A-2**  
**ONTARIO HYDRO METHOD DATA INPUTS**  
**Unit 6 Outlet**

**Test Data**

	1	2	3
Run number			
Location		Unit 6 Outlet	
Date	7/14/99	7/15/99	7/15/99
Time period	1415-1641	0825-1055	1250-1512
Operator	JP	JP	JP

**Process Data**

Unit Load, MW	74	75	75
Coal feed rate, lb/hr.	63700	64200	64000
Coal Btu content, Btu/lb. (as received)	12038	12132	12121
Heat Input, 10 <sup>6</sup> Btu/hr (F-Factor)	761.3	818.0	749.1

**Inputs For Calcs.**

Sq. rt. delta P	1.111320	1.15748	1.09899
Delta H	1.36583	1.82583	1.66000
Stack temp. (deg.F)	305.00	303.91	305.80
Meter temp. (deg.F)	90.25	96.95	89.10
Sample volume (act.)	75.662	86.342	81.939
Barometric press. (in.Hg)	29.47	29.50	29.56
Volume H <sub>2</sub> O imp. (ml)	146.7	165.9	156.0
Weight chng sil. gel (g)	14.7	17.0	18.5
% CO <sub>2</sub>	12.6	12.9	12.8
% O <sub>2</sub>	6.1	5.8	5.9
% N	81.3	81.3	81.3
Area of stack (sq.ft.)	63.62	63.62	63.62
Sample time (min.)	120.00	120.00	120.00
Static pressure (in.H <sub>2</sub> O)	-1.90	-1.90	-1.90
Nozzle dia. (in.)	0.199	0.210	0.210
Meter box cal.	1.0098	1.0098	1.0098
Cp of pitot tube	0.84	0.84	0.84
Traverse points	12	12	12

**Mercury Laboratory Report Data**

Particulate bound, ug	0.1000	0.0510	<	0.0100
Oxidized, ug	1.4300	1.9750		1.3800
Elemental, ug	1.1800	1.8150		1.5300
<b>Total mercury catch, ug</b>	<b>2.7100</b>	<b>3.8410</b>		<b>2.9100</b>

Note: Non-detects not included in Total mercury catch value.

**TABLE A-3**  
**ONTARIO HYDRO METHOD DATA INPUTS**  
**Unit 1-4 Outlet**

**Test Data**

	1	2	3
Run number			
Location		Units 1-4 Outlet	
Date	7/16/99	7/16/99	7/16/99
Time period	0820-1037	1115-1338	1410-1641
Operator			

**Process Data**

Unit Load, MW	124.0	127.0	138.0
Coal feed rate, lb/hr.	110000	111000	117000
Coal Btu content, Btu/lb.(as received)	12180	12180	12180
Heat Input, 10 <sup>6</sup> Btu/hr (F-Factor)	1784	1638	1755

**Inputs For Calcs.**

Sq. rt. delta P	1.674900	1.58912	1.69028
Delta H	1.13000	0.94000	0.98000
Stack temp. (deg.F)	285.40	298.60	310.30
Meter temp. (deg.F)	96.60	98.70	99.80
Sample volume (std.)	68.759	54.982	60.161
Barometric press. (in.Hg)	29.50	29.50	29.50
Volume H <sub>2</sub> O imp. (ml)	117.9	93.8	110.3
Weight chnge sil. gel (g)	21.0	12.3	15.4
% CO <sub>2</sub>	13.4	13.0	13.3
% O <sub>2</sub>	6.2	6.6	6.3
% N	80.4	80.4	80.4
Area of stack (sq.ft.)	97.93	97.93	97.93
Sample time (min.)	120.00	120.00	120.00
Static pressure (in.H <sub>2</sub> O)	-2.00	-2.00	-2.04
Nozzle dia. (in.)	0.150	0.152	0.150
Meter box cal.	1.0000	1.0000	1.0000
Cp of pitot tube	0.84	0.84	0.84
Traverse points	12	12	12

**Mercury Laboratory Report Data**

Particulate bound, ug	<	0.0080	<	0.0080	<	0.0080
Oxidized, ug		0.4850		0.2600		0.3250
Elemental, ug		0.0850		0.1550		0.0200
Total mercury catch, ug		0.5700		0.4150		0.3450

# Sample and Velocity Traverse Point Data Sheet - Method 1

Client DOE  
 Location/Plant LAKE PRESQUE ISLE  
 Source UNIT 6 INLET

Operator TB-LF  
 Date 7-14-99  
 W.O. Number 20009-011-006-0500

**Duct Type**     Circular     Rectangular Duct    Indicate appropriate type  
**Traverse Type**     Particulate Traverse     Velocity Traverse

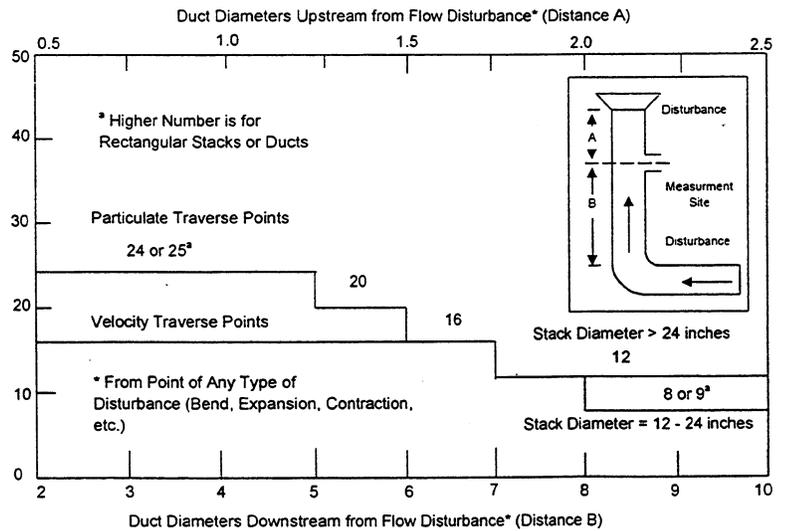
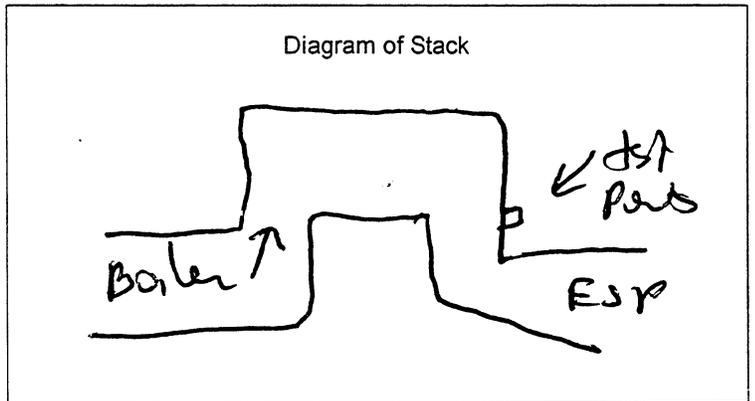
Distance from far wall to outside of port (in.) = C	99"
Port Depth (in.) = D	17.5"
Depth of Duct, diameter (in.) = C-D	181.5"
Area of Duct (ft <sup>2</sup> )	151.96 / 127.8
Total Traverse Points	12
Total Traverse Points per Port	6

**Rectangular Ducts Only**

Width of Duct, rectangular duct only (in.)	268.5"
Total Ports (rectangular duct only)	2014

Traverse Point Locations			
Traverse Point	% of Duct	Distance from Inside Duct Wall (in)	Distance from Outside of Port (in)
1	8.3	6 3/4	24 1/4
2	25	20 3/8	37 5/8
3	41.7	34	51 1/2
4	58.3	47 1/2	65
5	75	61 1/8	78 5/8
6	91.7	74 3/4	92 1/4
7			
8			
9			
10			
11			
12			

Flow Disturbances	
Upstream - A (ft)	
Downstream - B (ft)	
Upstream - A (duct diameters)	< 0.5
Downstream - B (duct diameters)	< 0.5



Equivalent Diameter =  $(2 * L * W) / (L + W)$

Traverse Point Location Percent of Stack - Circular													
		Number of Traverse Points											
		1	2	3	4	5	6	7	8	9	10	11	12
T r a v e r s e P o i n t	1		14.6		6.7		4.4		3.2		2.6		2.1
	2		85.4		25		14.6		10.5		8.2		6.7
	3			75		29.6		19.4		14.6		11.8	
	4				93.3		70.4		32.3		22.6		17.7
	5					85.4		67.7		34.2		25	
	6						95.6		80.6		65.8		35.6
	7							89.5		77.4		64.4	
	8								96.8		85.4		75
	9									91.8		82.3	
	10										97.4		88.2
	11											93.3	
	12												97.9

Traverse Point Location Percent of Stack - Rectangular													
		Number of Traverse Points											
		1	2	3	4	5	6	7	8	9	10	11	12
T r a v e r s e P o i n t	1		25.0	16.7	12.5	10.0	8.3	7.1	6.3	5.6	5.0	4.5	4.2
	2		75.0	50.0	37.5	30.0	25.0	21.4	18.8	16.7	15.0	13.6	12.5
	3			83.3	62.5	50.0	41.7	35.7	31.3	27.8	25.0	22.7	20.8
	4				87.5	70.0	58.3	50.0	43.8	38.9	35.0	31.8	29.2
	5					90.0	75.0	64.3	56.3	50.0	45.0	40.9	37.5
	6						91.7	78.6	68.8	61.1	55.0	50.0	45.8
	7							92.9	81.3	72.2	65.0	59.1	54.2
	8								93.8	83.3	75.0	68.2	62.5
	9									94.4	85.0	77.3	70.8
	10										95.0	86.4	79.2
	11											95.5	87.5
	12												95.8

- Rectangular Stack Points & Matrix
- 9 - 3 x 3
  - 12 - 4 x 3
  - 16 - 4 x 4
  - 20 - 5 x 4
  - 25 - 5 x 5
  - 30 - 6 x 5
  - 36 - 6 x 6
  - 42 - 7 x 6
  - 49 - 7 x 7



# Determination of Stack Gas Velocity - Method 2

Client Doe  
 Location/Plant Marguette MI  
 Source #6 Inlet

Operator JDR  
 Date 14 Jul 99  
 W.O. Number \_\_\_\_\_

Pitot Coeff (Cp) 0.84  
 Stack Area, ft<sup>2</sup> (As) 127.8  
 Pitot Tube/Thermo ID P142

Run Number	1	
Time	1307	
Barometric Press, in Hg (Pb)		
Static Press, in H <sub>2</sub> O (Pstatic)	-0.85	
Source Moisture, % (BWS)		
O <sub>2</sub> , %		
CO <sub>2</sub> , %		

Cyclonic Flow Determination		Traverse Location		Leak Check good ? Y/N		Leak Check good ? Y/N		Leak Check good ? Y/N	
Delta P at 0°	Angle yielding zero Delta P	Port	Point	Delta P	Source Temp, F° (Ts)	Delta P	Source Temp, F° (Ts)	Delta P	Source Temp, F° (Ts)
0.04	10	1	1	0.36	307				
0.10	10		2	0.45	311				
0.05	10		3	0.50	305				
0.05	5		4	0.50	300				
0.01	2		5	0.46	294				
0	0		6	0.35	300				
		2	1	0.18	307				
			2	0.40	317				
			3	0.41	318				
			4	0.44	318				
			5	0.42	316				
			6	0.35	315				
Avg Angle		Avg Delta P & Temp		0.402	310				
		avg $\sqrt{\Delta P}$		0.62958					
Average gas stream velocity, ft/sec.									
Vol. flow rate @ actual conditions, wacf/min									
Vol. flow rate at standard conditions, dscf/min									

$MWd = (0.32 * O_2) + (0.44 * CO_2) + (0.28 * (100 - (CO_2 + O_2)))$   
 $MWs = (MWd * (1 - (BWS/100))) + (18 * (BWS/100))$   
 $Tsa = Ts + 460$   
 $Ps = Pb + (Pstatic / 13.6)$   
 $Vs = 85.49 * Cp * \text{avg} \sqrt{\Delta P} * \sqrt{Tsa / (Ps * MWs)}$   
 $Qs(\text{act}) = 60 * Vs * As$   
 $Qs(\text{std}) = 17.64 * (1 - (BWS/100)) * (Ps/Tsa) * Qs(\text{act})$

Comments \_\_\_\_\_

where:  
 MWd = Dry molecular weight source gas, lb/lb-mole.  
 MWs = Wet molecular weight source gas, lb/lb-mole.  
 Tsa = Source Temperature, absolute(oR)  
 Ps = Absolute stack static pressure, inches Hg.  
 Vs = Average gas stream velocity, ft/sec.  
 Qs(act) = Volumetric flow rate of wet stack gas at actual,  
 Qs(std) = Volumetric flow rate of dry stack gas at standard conditions, dscf/min



# ISOKINETIC FIELD DATA SHEET

## Ontario Hydro Method - Mercury

Client	DOE	Stack Conditions	Meter Box ID	Leak Checks	Temp Check
W.O.#	20009-011-006-0500	Assumed	1009	Sample Train (ft <sup>2</sup> )	Meter Box Temp
Project ID	DOE	Actual	19055	Leak Check @ (in Hg)	Reference Temp
Mode/Source ID	BO 6	136.6	P300	Pilot good	Pass/Fail (+/- 2°)
Samp. Loc. ID	IN	13.3	Boro	Orsat good	Temp Change Response
Run No. ID	1	13.7	0.84		
Test Method ID	OHM	4.9	Nozzle ID		
Date ID	13JUL1999	300	Avg Nozzle Dia (in)		
Source/Location	Boiler 6 Inlet	115	Area of Stack (ft <sup>2</sup> )		
Sample Date	7-14-99	8.5	Sample Time		
Baro. Press (in Hg)	29.58		Total Traverse Pits		
Operator	TB				

K Factor	2.93
Initial	100
Mid-Point	100
Final	100
Pre-Test Set	yes / no
Post-Test Set	yes / no
Pass / Fail	Pass / Fail
Temp Change Response	Pass / Fail

TRAVERSE POINT NO.	SAMPLE TIME (min)	CLOCK TIME (plant time)	VELOCITY PRESSURE Delta P (in H2O)	ORIFICE PRESSURE Delta H (in H2O)	DRY GAS METER READING (ft <sup>3</sup> )	STACK TEMP (°F)	DGM INLET TEMP (°F)	DGM OUTLET TEMP (°F)	PROBE TEMP (°F)	FILTER BOX TEMP (°F)	IMPINGER EXIT TEMP (°F)	SAMPLE TRAIN VAC (in Hg)	COMMENTS
1	0	1915	0.30	0.88	140.267	301	110	108	256	255	60	2	
2	5		0.28	0.88	143.2	307	110	107	259	257	63	2	
3	10		0.37	1.08	158.6	308	111	107	250	256	61	2.5	
4	15		0.33	1.08	201.3	303	114	108	251	253	61	2.3	
5	20		0.33	0.97	204.3	298	114	108	251	252	60	2.3	
6	25		0.40	0.97	207.1	298	114	109	256	251	60	2.3	
7	30		0.40	1.17	210.1	298	115	109	249	253	60	3	
8	35		0.40	1.17	213.1	298	115	109	249	253	59	3	
9	40		0.36	1.05	216.0	297	116	109	250	253	59	3	
10	45		0.36	1.05	218.8	295	116	110	248	250	58	3	
11	50		0.31	0.95	221.6	295	116	110	249	251	58	3	
12	55		0.31	0.91	224.67	293	116	111	251	254	61	3	34-140
13	60	1815	0.31	0.91	224.67	293	116	111	250	258	61	3	
													103.9 % I
													10.1 % m
													194100 SCFM
													VM = 62.7
													haz
													Max Temp
													Max Vac
													Min/Max
													Temp
													Ontario Hydro Method



MID-TEST LEAK CK.  
'008 @ 11"

Ontario Hydro Method - Mercury

ISOKINETIC FIELD DATA SHEET

Client: 112 Operator: 7-14-09 K Factor: 2.93  
 Source: Boiler 6 Run No.: 1  
 Sample Loc.: Inlet Date: 7-14-09

TRAVERSE POINT NO.	SAMPLE TIME (min)	GLOCK TIME (plant time)	VELOCITY PRESSURE Delta P (in H2O)	ORIFICE PRESSURE Delta H (in H2O)	DRY GAS METER READING (ft <sup>3</sup> )	STACK TEMP (°F)	DGM INLET TEMP (°F)	DGM OUTLET TEMP (°F)	PROBE TEMP (°F)	FILTER BOX TEMP (°F)	IMPING EXIT TEMP (°F)	SAMPLE TRAIN VAC (in Hg)	COMMENTS
0	1540				204.772								
1	5		0.32	0.94	207.6	319	111	110	249	256	67	3	
2	10		0.25	0.73	209.1	321	113	110	249	251	64	3	
3	15		0.32	0.94	232.8	324	114	110	250	251	67	3	
4	20		0.32	0.94	236.6	325	116	111	254	253	67	3.5	
5	25		0.40	1.17	238.6	324	116	111	255	258	61	3.5	
6	30		0.40	1.17	241.6	324	117	111	251	252	61	4	
7	35		0.40	1.17	244.5	321	118	112	251	253	60	4	
8	40		0.40	1.17	247.6	321	118	112	250	254	60	4.5	
9	45		0.37	1.08	250.5	317	118	112	251	248	62	4.5	
10	50		0.37	1.11	253.3	318	118	113	250	248	62	4.5	
11	55		0.37	0.94	256.2	310	118	113	253	248	63	5	
12	60	1640	0.32	0.94	258.90	305	118	113	253	250	65	5	34-135

Avg Sqrt Delta P	0.57766	Avg Delta H	1.015	Total Volume	682.75	Avg Ts	309.1	Avg Tm	112.5	Min/Max	248/258	Max Vac	5	Max Temp	67
Avg Sqrt Del H	1.02558	Comments:													



*Handwritten signature*

MED-40556 LEAK CK.  
008 @ 11"

Ontario Hydro Method - Mercury

ISOKINETIC FIELD DATA SHEET

Client: TPB Operator: 7-14-09 K Factor: 2.93  
 Source: Boiler 6 Run No.: 1  
 Sample Loc.: Inlet Date: 7-14-09

TRAVERSE POINT NO	SAMPLE TIME (min)	CLOCK TIME (plant time)	VELOCITY PRESSURE Delta P (in H2O)	ORIFICE PRESSURE Delta H (in H2O)	DRY GAS METER READING (ft <sup>3</sup> )	STACK TEMP (°F)	DGM INLET TEMP (°F)	DGM OUTLET TEMP (°F)	PROBE TEMP (°F)	FILTER BOX TEMP (°F)	IMPING EXIT TEMP (°F)	SAMPLE TRAIN VAC (in Hg)	COMMENTS
1	0	1540	0.32	0.94	204.772	319	111	110	248	256	67	3	
	5		0.32	0.73	207.0	321	113	110	249	251	64	3	
	10		0.32	0.94	209.8	324	114	110	250	251	67	3	
	15		0.32	0.94	232.8	325	116	111	254	253	67	3	
	20		0.32	1.17	236.6	324	116	111	255	258	61	3.5	
	25		0.40	1.17	238.6	324	116	111	251	252	61	3.5	
	30		0.40	1.17	241.6	321	117	111	251	253	61	4	
	35		0.40	1.17	244.5	321	118	112	250	254	60	4	
	40		0.37	1.08	247.6	317	118	112	251	248	61	4.5	
	45		0.37	1.11	250.5	318	118	112	250	248	60	4.5	
	50		0.32	0.94	253.2	310	118	113	255	248	63	5	
	55		0.32	0.94	256.2	305	118	113	255	248	63	5	
	60	1640	0.32	0.94	256.90	305	118	113	258	250	65	5	34-135

Avg Sqrt Delta P	0.58766	Avg Delta H	1.015	Avg Ts	309.1	Avg Tm	112.5	Min/Max	248/258	Max Temp	67	Max Vac	5	Max Temp
Total Volume	68.275	Avg Sqrt-Del H	1.0253	Comments:										



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# ISOKINETIC FIELD DATA SHEET

## Ontario Hydro Method - Mercury

Client	DOE	Stack Conditions	Meter Box ID	Leak Checks	Pre-Test Set	Post-Test Set
W.O.#	20009-011-006-0500	Assumed	Meter Box Y	Sample Train (ft*)	Pass / Fail	Pass / Fail
Project ID	DOE	Actual	Meter Box Del H	Leak Check @ (in Hg)	Pass / Fail	Pass / Fail
Mode/Source ID	BO 6	137.8	Probe ID / Length	Pilot good	Pass / Fail	Pass / Fail
Samp. Loc. ID	IN	13.4	Probe Material	Orsat good	Pass / Fail	Pass / Fail
Run No. ID	2	13.8	Pilot / Thermocouple ID	Temp Check	Pass / Fail	Pass / Fail
Test Method ID	OHM	4.9	Pilot Coefficient	Meter Box Temp	Pass / Fail	Pass / Fail
Date ID	13JUL1999	3.0	Nozzle ID	Reference Temp	Pass / Fail	Pass / Fail
Source/Location	Boiler 6	1.0	Avg Nozzle Dia (in)	Temp Change Response	Pass / Fail	Pass / Fail
Sample Date	7-15-99	-8.0	Area of Stack (ft²)			
Baro. Press (in Hg)	29.58		Sample Time			
Operator	79		Total Traverse Pts			

TRAVERSE POINT NO.	SAMPLE TIME (min)	CLOCK TIME (plant time)	VELOCITY PRESSURE Delta P (in H2O)	ORIFICE PRESSURE Delta H (in H2O)	DRY GAS METER READING (ft³)	STACK TEMP (°F)	DGM INLET TEMP (°F)	DGM OUTLET TEMP (°F)	PROBE TEMP (°F)	FILTER BOX TEMP (°F)	IMPING EXIT TEMP (°F)	SAMPLE TRAIN VAC (in Hg)	COMMENTS
1	0	0825	0.03	0.82	259.170	319	107	101	247	244	67	2	
2	5		0.03	0.82	261.8	319	107	102	247	243	64	3	
3	10		0.03	1.17	267.4	321	106	102	246	249	61	3	
4	15		0.03	1.17	272.3	321	108	103	247	247	60	3	
5	20		0.03	1.35	273.5	322	109	103	252	250	60	3	
6	25		0.03	1.35	278.7	322	111	104	252	247	60	3	
7	30		0.03	1.28	280.1	322	111	104	250	249	58	4	
8	35		0.03	1.35	283.0	322	112	105	250	244	68	4	
9	40		0.03	1.28	286.1	306	112	106	245	246	60	4	
10	45		0.03	1.24	289.9	315	113	106	250	248	60	4	
11	50		0.03	1.12	290.9	316	113	107	249	246	61	4	
12	55		0.03	1.03	294.8	310	113	107	249	246	62	4	
13	60	0925	0.03	1.03	294.8	310	113	107	249	246	62	4	

Avg Sqrt Delta P	Avg Delta H	Total Volume	Avg Ts	Avg Tm	Min/Max	Max Temp	Max Vac	Max Temp



Ontario Hydro Method







# Source Gas Analysis Data Sheet - Method 3

Client Dot/Wr Analyst KIK  
 Location/Plant Mannville Date 2/14/99  
 Source #6 inlet Analytical Method (circle one) EPA 3 using 3A *analyzers*  
 W.O. Number \_\_\_\_\_

Run Number 1 *Cal*  
~~Leak~~ Check Good? (circle one) Yes No

Analysis Number	Analysis Time	Percent CO <sub>2</sub> (A)	Percent Total (B)	Percent O <sub>2</sub> (B - A)	Percent N <sub>2</sub> (100 - B)
1		13.7		4.9	
2		13.7		5.0	
3		13.7		4.9	
Average		13.7		4.9	

Run Number 2 *Cal*  
~~Leak~~ Check Good? (circle one) Yes No

Analysis Number	Analysis Time	Percent CO <sub>2</sub> (A)	Percent Total (B)	Percent O <sub>2</sub> (B - A)	Percent N <sub>2</sub> (100 - B)
1		13.8		4.9	
2		13.8		4.9	
3		13.8		4.9	
Average		13.8		4.9	

Run Number 3 *Cal*  
~~Leak~~ Check Good? (circle one) Yes No

Analysis Number	Analysis Time	Percent CO <sub>2</sub> (A)	Percent Total (B)	Percent O <sub>2</sub> (B - A)	Percent N <sub>2</sub> (100 - B)
1		13.4		5.2	
2		13.4		5.2	
3		13.5		5.1	
Average		13.4		5.2	

Acceptable differences for repeat analysis:  
 if CO<sub>2</sub> > 4% than +/- 0.3%  
 if CO<sub>2</sub> < or = 4% than +/- 0.2%  
 if O<sub>2</sub> > or = 15% than +/- 0.2%  
 if O<sub>2</sub> < 15% than +/- 0.3%

Ambient Check  (20.9)  
 Oxygen  
 Carbon Dioxide  (0.0)

Report all values to the nearest 0.1 percent

Comments *Cal w/ 9 N<sub>2</sub>, 12.6% O<sub>2</sub>, 9.9% CO<sub>2</sub>*



# Sample and Velocity Traverse Point Data Sheet - Method 1

Client DOE/WP  
 Location/Plant MARSHVILLE  
 Source #6 STACK

Operator KK JP  
 Date 7/14/98  
 W.O. Number \_\_\_\_\_

**Duct Type**     Circular     Rectangular Duct    Indicate appropriate type  
**Traverse Type**     Particulate Traverse     Velocity Traverse

Distance from far wall to outside of port (in.) = C	115"
Port Depth (in.) = D	7
Depth of Duct, diameter (in.) = C-D	108"
Area of Duct (ft <sup>2</sup> )	63.67
Total Traverse Points	12
Total Traverse Points per Port	3

**Rectangular Ducts Only**

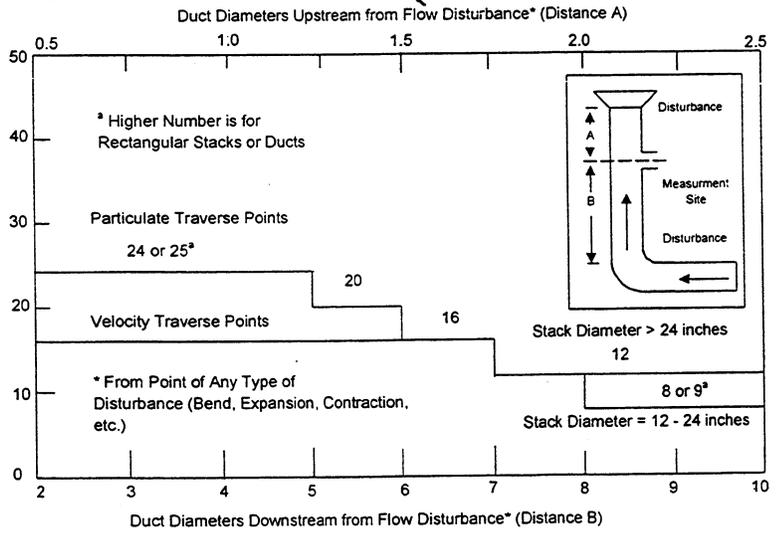
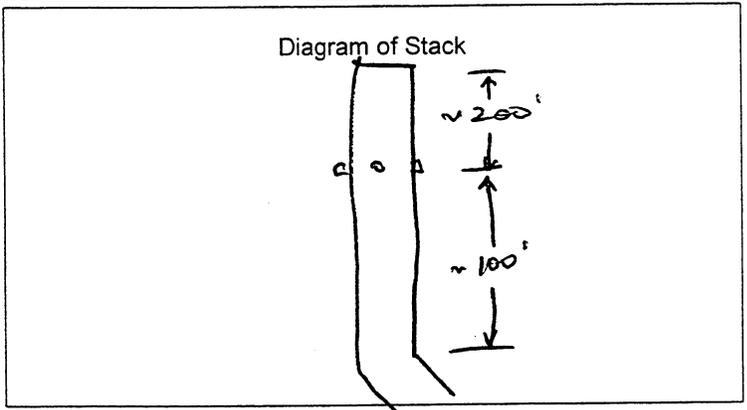
Width of Duct, rectangular duct only (in.)	
Total Ports (rectangular duct only)	

**Traverse Point Locations**

Traverse Point	% of Duct	Distance from Inside Duct Wall (in)	Distance from Outside of Port (in)
1	.044	4.752	1134
2	.146	15.768	2234
3	.296	31.968	39
4			
5			
6			
7			
8			
9			
10			
11			
12			

**Flow Disturbances**

Upstream - A (ft)	~ 200'
Downstream - B (ft)	~ 100
Upstream - A (duct diameters)	22
Downstream - B (duct diameters)	11



Equivalent Diameter =  $(2 * L * W) / (L + W)$

**Traverse Point Location Percent of Stack - Circular**

Traverse Point	Number of Traverse Points												
	1	2	3	4	5	6	7	8	9	10	11	12	
1		14.6		6.7		4.4		3.2		2.6		2.1	
2			85.4		25		14.6		10.5		8.2	6.7	
3				75		29.6		19.4		14.6		11.8	
4					93.3		70.4		32.3		22.6	17.7	
5						85.4		67.7		34.2		25	
6							95.6		80.6		65.8	35.6	
7								89.5		77.4		64.4	
8									96.8		85.4	75	
9										91.8		82.3	
10											97.4	88.2	
11												93.3	
12													97.9

**Traverse Point Location Percent of Stack - Rectangular**

Traverse Point	Number of Traverse Points												
	1	2	3	4	5	6	7	8	9	10	11	12	
1		25.0	16.7	12.5	10.0	8.3	7.1	6.3	5.6	5.0	4.5	4.2	
2			75.0	50.0	37.5	30.0	25.0	21.4	18.8	16.7	15.0	13.6	12.5
3				83.3	62.5	50.0	41.7	35.7	31.3	27.8	25.0	22.7	20.8
4					87.5	70.0	58.3	50.0	43.8	38.9	35.0	31.8	29.2
5						90.0	75.0	64.3	56.3	50.0	45.0	40.9	37.5
6							91.7	78.6	68.8	61.1	55.0	50.0	45.8
7								92.9	81.3	72.2	65.0	59.1	54.2
8									93.8	83.3	75.0	68.2	62.5
9										94.4	85.0	77.3	70.8
10											95.0	86.4	79.2
11												95.5	87.5
12													95.8

- Rectangular Stack Points & Matrix**
- 9 - 3 x 3
  - 12 - 4 x 3
  - 16 - 4 x 4
  - 20 - 5 x 4
  - 25 - 5 x 5
  - 30 - 6 x 5
  - 36 - 6 x 6
  - 42 - 7 x 6
  - 49 - 7 x 7



# Determination of Stack Gas Velocity - Method 2

Client ODE/WR Operator WJ Jr Pitot Coeff (Cp) 0.84  
 Location/Plant MANAGERS Date 7/14/99 Stack Area, ft<sup>2</sup> (As) 63.617  
 Source #6 STACK W.O. Number \_\_\_\_\_ Pitot Tube/Thermo ID P266

Run Number	<u>PNE</u>		
Time	<u>1210</u>		
Barometric Press, in Hg (Pb)	<u>29.47</u>		
Static Press, in H <sub>2</sub> O (Pstatic)	<u>-6.9</u>		
Source Moisture, % (BWS)			
O <sub>2</sub> , %			
CO <sub>2</sub> , %			

Cyclonic Flow Determination		Traverse Location		Leak Check good ? <u>Y</u> / N		Leak Check good ? Y / N		Leak Check good ? Y / N	
Delta P at O°	Angle yielding zero Delta P	Port	Point	Delta P	Source Temp, F° (Ts)	Delta P	Source Temp, F° (Ts)	Delta P	Source Temp, F° (Ts)
<u>-0.05</u>	<u>45</u>	<u>A</u>	<u>1</u>	<u>1.5</u>	<u>290</u>				
<u>-1.05</u>	<u>45</u>		<u>2</u>	<u>1.5</u>	<u>290</u>				
<u>0</u>	<u>—</u>		<u>3</u>	<u>1.1</u>	<u>290</u>				
<u>0</u>	<u>—</u>	<u>B</u>	<u>1</u>	<u>1.5</u>	<u>291</u>				
<u>0</u>	<u>—</u>		<u>2</u>	<u>1.4</u>	<u>292</u>				
<u>-1.05</u>	<u>5</u>		<u>3</u>	<u>1.2</u>	<u>291</u>				
<u>0</u>	<u>—</u>	<u>C</u>	<u>1</u>	<u>1.4</u>	<u>291</u>				
<u>-0.05</u>	<u>5</u>		<u>2</u>	<u>1.4</u>	<u>291</u>				
<u>-1.10</u>	<u>8</u>		<u>3</u>	<u>1.2</u>	<u>292</u>				
<u>-1.05</u>	<u>45</u>	<u>D</u>	<u>1</u>	<u>1.3</u>	<u>290</u>				
<u>-1.10</u>	<u>10</u>		<u>2</u>	<u>1.4</u>	<u>290</u>				
<u>0</u>	<u>—</u>		<u>3</u>	<u>1.96</u>	<u>290</u>				
Avg Angle		Avg Delta P & Temp avg $\sqrt{\Delta P}$		<u>1.3</u>	<u>~290</u>				
Average gas stream velocity, ft/sec.		Vol. flow rate @ actual conditions, wacf/min							
Vol. flow rate at standard conditions, dscf/min									

$$MWd = (0.32 * O_2) + (0.44 * CO_2) + (0.28 * (100 - (CO_2 + O_2)))$$

$$MWs = (MWd * (1 - (BWS/100))) + (18 * (BWS/100))$$

$$Tsa = Ts + 460$$

$$Ps = Pb + (Pstatic/13.6)$$

$$Vs = 85.49 * Cp * \text{avg} \sqrt{\Delta P} * \sqrt{Tsa / (Ps * MWs)}$$

$$Qs(\text{act}) = 60 * Vs * As$$

$$Qs(\text{std}) = 17.64 * (1 - (BWS/100)) * (Ps/Tsa) * Qs(\text{act})$$

Comments \_\_\_\_\_

where:

MWd = Dry molecular weight source gas, lb/lb-mole.

MWs = Wet molecular weight source gas, lb/lb-mole.

Tsa = Source Temperature, absolute (oR)

Ps = Absolute stack static pressure, inches Hg.

Vs = Average gas stream velocity, ft/sec.

Qs(act) = Volumetric flow rate of wet stack gas at actual

Qs(std) = Volumetric flow rate of dry stack gas at standard conditions, dscf/min



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# ISOKINETIC FIELD DATA SHEET

## Ontario Hydro Method - Mercury

Client JP Operator KW  
 Source 2 Boiler # 7/15/99 Run No. 1-36  
 Sample Loc. 7/15/99 Date 7/15/99 K Factor

TRAVERSE POINT NO.	SAMPLE TIME (min)	CLOCK TIME (H:MM:SS)	VELOCITY PRESSURE Delta P (in H2O)	ORIFICE PRESSURE Delta H (in H2O)	DRY GAS METER READING (ft <sup>3</sup> )	STACK TEMP (°F)	DGM INLET TEMP (°F)	DGM OUTLET TEMP (°F)	PROBE TEMP (°F)	FILTER BOX TEMP (°F)	IMPING EXIT TEMP (°F)	SAMPLE TRAIN VAC (in Hg)	COMMENTS
0	945				333.458								
1	5		1.6	2.17	337.4	304	97	94	227	243	65	4.0	
2	10		1.6	2.17	341.2	305	100	101	240	251	64	4.5	
3	15		1.5	2.04	345.1	305	103	95	245	248	64	4.5	
4	20		1.5	2.04	348.8	304	104	95	245	240	65	4.5	
5	25		1.2	1.63	352.2	304	104	96	247	239	66	4.5	
6	30	1015	1.2	1.63	355.7/8	304	104	99	240	238	67	5.0	22.260
7	35												
8	40												
9	45												
10	50	10	1.5	2.04	359.8	303	93	94	230	240	66	4.5	
11	55		1.5	2.04	363.6	304	101	95	228	240	62	4.5	
12	60		1.3	1.76	367.2	304	103	95	230	242	58	4.5	
13	65		1.3	1.76	370.8	305	103	95	234	241	58	4.5	
14	70		1.1	1.49	374.1	305	104	96	238	241	58	4.5	
15	75		1.1	1.49	377.364	305	102	96	240	242	59	4.5	21400
16	80												
17	85												
18	90												
19	95												
20	100												
21	105												
22	110												
23	115												
24	120												
25	125												
26	130												
27	135												
28	140												
29	145												
30	150												
31	155												
32	160												
33	165												
34	170												
35	175												
36	180												
37	185												
38	190												
39	195												
40	200												
41	205												
42	210												
43	215												
44	220												
45	225												
46	230												
47	235												
48	240												
49	245												
50	250												
51	255												
52	260												
53	265												
54	270												
55	275												
56	280												
57	285												
58	290												
59	295												
60	300												
61	305												
62	310												
63	315												
64	320												
65	325												
66	330												
67	335												
68	340												
69	345												
70	350												
71	355												
72	360												
73	365												
74	370												
75	375												
76	380												
77	385												
78	390												
79	395												
80	400												
81	405												
82	410												
83	415												
84	420												
85	425												
86	430												
87	435												
88	440												
89	445												
90	450												
91	455												
92	460												
93	465												
94	470												
95	475												
96	480												
97	485												
98	490												
99	495												
100	500												

90 F = 98.1  
 90 M 9.5  
 SCPM 184000  
 Vmax = 81.83  
 M³ Max Temp  
 2.29

**WESTON**  
 MANAGERS  
 RESOURCES CONSULTANTS

Avg Sqrt Delta P 1.15748  
 Avg Delta H 1.82583  
 Avg Sqrt Del H 1.33733  
 Total Volume 86.342  
 Avg Ts 303.91  
 Avg Tm 96.95  
 Min/Max 227/250  
 Min/Max 238/251  
 Max Temp 6.7  
 Max Vac 4.5

Comments:





# Source Gas Analysis Data Sheet - Method 3

Client DOE/WP Analyst KW  
 Location/Plant MANQUETE Date 7/14/99  
 Source # 6 STACK Analytical Method (circle one) EPA 3 using 3 A analyzer  
 W.O. Number \_\_\_\_\_

Run Number 1 <sup>cal</sup> Leak Check Good? (circle one) Yes No

Analysis Number	Analysis Time	Percent CO <sub>2</sub> (A)	Percent Total (B)	Percent O <sub>2</sub> (B - A)	Percent N <sub>2</sub> (100 - B)
1	12.6	6.1 <sup>(UK)</sup>		6.1	
2		12.6		6.1	
3		12.6		6.1	
Average		12.6		6.1	

Run Number 2 <sup>cal</sup> Leak Check Good? (circle one) Yes No

Analysis Number	Analysis Time	Percent CO <sub>2</sub> (A)	Percent Total (B)	Percent O <sub>2</sub> (B - A)	Percent N <sub>2</sub> (100 - B)
1		12.9		5.8	
2		12.9		5.8	
3		12.9		5.8	
Average		12.9		5.8	

Run Number 3 <sup>cal</sup> Leak Check Good? (circle one) Yes No

Analysis Number	Analysis Time	Percent CO <sub>2</sub> (A)	Percent Total (B)	Percent O <sub>2</sub> (B - A)	Percent N <sub>2</sub> (100 - B)
1		12.8		5.9	
2		12.8		5.9	
3		12.8		5.9	
Average		12.8		5.9	

Acceptable differences for repeat analysis:  
 if CO<sub>2</sub> > 4% than +/- 0.3%  
 if CO<sub>2</sub> < or = 4% than +/- 0.2%  
 if O<sub>2</sub> > or = 15% than +/- 0.2%  
 if O<sub>2</sub> < 15% than +/- 0.3%

Ambient Check  
 Oxygen ✓ (20.9)  
 Carbon Dioxide ✓ (0.0)

Report all values to the nearest 0.1 percent

Comments cal w/ O<sub>2</sub>, 12.63% O<sub>2</sub>, 9.91% CO<sub>2</sub>

Sample Pt. Unit 6 Inlet

Date 7/14/99  
 Run In-# 1 Boiler 6  
 Fund # \_\_\_\_\_  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	728.0	837.3	109.3 ✓
BUBBLER	KCl	733.3	748.9	15.6 ✓
IMPINGER	KCl	720.7	727.8	7.1 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	759.7	763.7	4.0 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	736.0	736.0	0.0 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	<del>743.2</del> 664.1	663.9	- 0.2 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	743.1	743.9	0.8 ✓
BUBBLER	SILICA GEL	956.6	969.9	13.3 ✓
			Total H <sub>2</sub> O (g)	150.3
FILTER				149.9 ✓
			Sig	13.3
			Total Dust (g)	

$V_{wstd} = 0.0474 * (H_2O \text{ g})$

$V_m \text{ Corrected} = V_m * C_m$

$V_{mstd} = \frac{17.71 V_m C (P_b + \Delta H / 13.6)}{T_m}$

$V_{istd} = V_{wstd} + V_{mstd}$

$\%H_2O = (V_{wstd} / V_{istd}) * 100$

$Q_{nstd} = 17.71 Q_n P_s / T_s$

$\% \text{ Isokinetic} = V_{istd} / (Q_{nstd} * \text{Time})$

**DUST LOADING CALCULATIONS (Concentration Basis)**

$DCL = 15.432 (\text{dust g}) / V_{istd}$

$\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$

$ACFM = V_s * \text{Pipe Area (ft}^2\text{)}$

$SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$

$\text{lbs/hour} = \text{grains / scf} * 0.000143 * SCFM * 60$

\_\_\_\_\_ SCF

\_\_\_\_\_ ACF

\_\_\_\_\_ SCF

\_\_\_\_\_ SCF

\_\_\_\_\_ %H<sub>2</sub>O

\_\_\_\_\_ SCFM

\_\_\_\_\_ %

\_\_\_\_\_ grains/scf

\_\_\_\_\_ %

\_\_\_\_\_ ACFM

\_\_\_\_\_ SCFM

\_\_\_\_\_ lbs/hour

Sample Pt. Unit 6 outlet

Date 7/14/99  
 Run Outlet Boiler  
 Fund # \_\_\_\_\_  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	696.1	810.4	114.3 ✓
BUBBLER	KCl	698.0	717.5	19.5 ✓
IMPINGER	KCl	745.6	751.9	6.3 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	609.2	613.7	4.5 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	744.9	746.2	1.3 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	739.0	739.3	0.3 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	730.2	730.7	0.5 ✓
BUBBLER	SILICA GEL	936.8	951.5	14.7 ✓
			Total H <sub>2</sub> O (g)	146.4 ✓
FILTER			Si gel	14.7 ✓
			Total Dust (g)	

$V_{wstd} = 0.0474 * (H_2O \text{ g})$  \_\_\_\_\_ SCF  
 $V_{m \text{ Corrected}} = V_m * C_m$  \_\_\_\_\_ ACF  
 $V_{mstd} = \frac{17.71 V_m C (P_s + \Delta H / 13.6)}{T_m}$  \_\_\_\_\_ SCF  
 $V_{tstd} = V_{wstd} + V_{mstd}$  \_\_\_\_\_ SCF  
 $\%H_2O = (V_{wstd} / V_{tstd}) * 100$  \_\_\_\_\_ %H<sub>2</sub>O  
 $Q_{nstd} = 17.71 Q_n P_s / T_s$  \_\_\_\_\_ SCFM  
 $\% \text{ Isokinetic} = V_{tstd} / (Q_{nstd} * \text{Time})$  \_\_\_\_\_ %  
**DUST LOADING CALCULATIONS (Concentration Basis)**  
 $DCL = 15.432 (\text{dust g}) / V_{tstd}$  \_\_\_\_\_ grains/scf  
 $\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$  \_\_\_\_\_ %  
 $ACFM = V_t * \text{Pipe Area (ft}^2)$  \_\_\_\_\_ ACFM  
 $SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$  \_\_\_\_\_ SCFM  
 $\text{lbs/hour} = \text{grains / scf} * 0.000143 * SCFM * 60$  \_\_\_\_\_ lbs/hour

Sample Pt. \_\_\_\_\_

Date 7/15/95  
 Run Inlet-2  
 Fund # \_\_\_\_\_  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	588.2	690.4	102.2 ✓
BUBBLER	KCl	747.9	773.3	25.4 ✓
IMPINGER	KCl	728.4	733.4	5.0 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	721.4	724.8	3.4 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub> <i>* broke during leak check</i>	<del>637.7</del> 735.7	726.8	1.1 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	655.9	656.3	0.4 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	741.8	742.1	0.3 ✓
BUBBLER	SILICA GEL	819.9	833.3	13.4 ✓
			Total H <sub>2</sub> O (g)	<del>151.2</del> 137.8
FILTER			Si gel	13.4 ✓
			Total Dust (g)	151.2 ✓

*\* broke during leak check*

$V_{wstd} = 0.0474 * (H_2O \text{ g})$  \_\_\_\_\_ SCF  
 $V_m \text{ Corrected} = V_m * C_m$  \_\_\_\_\_ ACF  
 $V_{mstd} = \frac{17.71 V_m C (P_b + \Delta H / 13.6)}{T_m}$  \_\_\_\_\_ SCF  
 $V_{std} = V_{wstd} + V_{mstd}$  \_\_\_\_\_ SCF  
 $\%H_2O = (V_{wstd} / V_{std}) * 100$  \_\_\_\_\_ %H<sub>2</sub>O  
 $Q_{nstd} = 17.71 Q_n P_s / T_s$  \_\_\_\_\_ SCFM  
 $\% \text{ Isokinetic} = V_{std} / (Q_{nstd} * \text{Time})$  \_\_\_\_\_ %  
**DUST LOADING CALCULATIONS (Concentration Basis)**  
 $DCL = 15.432 (\text{dust g}) / V_{std}$  \_\_\_\_\_ grains/scf  
 $\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$  \_\_\_\_\_ %  
 $ACFM = V_s * \text{Pipe Area (ft}^2\text{)}$  \_\_\_\_\_ ACFM  
 $SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$  \_\_\_\_\_ SCFM  
 $\text{lbs/hour} = \text{grains / scf} * 0.000143 * SCFM * 60$  \_\_\_\_\_ lbs/hour

Sample Pt. \_\_\_\_\_

Date 7/15/99  
 Run Outlet-2  
 Fund # \_\_\_\_\_  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	699.9	813.4	113.5 ✓
BUBBLER	KCl	701.2	735.1	33.9 ✓
IMPINGER	KCl	724.8	734.9	10.1 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	710.8	715.2	4.4 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	634.7	636.6	1.9 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	648.4	649.1	0.7 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	749.0	750.4	1.4 ✓
BUBBLER	SILICA GEL	829.0	846.0	17 ✓
			Total H <sub>2</sub> O (g)	165.9 -
FILTER			Si gel	17 ✓
			Total Dust (g)	

$V_{w, std} = 0.0474 * (H_2O \text{ g})$

$V_{m, Corrected} = V_m * C_m$

$V_{m, std} = \frac{17.71 V_m C (P_b + \Delta H / 13.6)}{T_m}$

$V_s, std = V_{w, std} + V_{m, std}$

$\%H_2O = (V_{w, std} / V_s, std) * 100$

$Q_n, std = 17.71 Q_n P_s / T_s$

$\% \text{ Isokinetic} = V_s, std / (Q_n, std * \text{Time})$

**DUST LOADING CALCULATIONS (Concentration Basis)**

$DCL = 15.432 (\text{dust g}) / V_s, std$

$\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$

$ACFM = V_s * \text{Pipe Area (ft}^2)$

$SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$

$\text{lbs/hour} = \text{grains / scf} * 0.000143 * SCFM * 60$

\_\_\_\_\_ SCF  
 \_\_\_\_\_ ACF  
 \_\_\_\_\_ SCF  
 \_\_\_\_\_ SCF  
 \_\_\_\_\_ %H<sub>2</sub>O  
 \_\_\_\_\_ SCFM  
 \_\_\_\_\_ %  
 \_\_\_\_\_ grains/scf  
 \_\_\_\_\_ %  
 \_\_\_\_\_ ACFM  
 \_\_\_\_\_ SCFM  
 \_\_\_\_\_ lbs/hour

Sample Pt. \_\_\_\_\_

Date 7/15/99  
 Run B06-W-3 (pm intake)  
 Fund # \_\_\_\_\_  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	695.4	809.3	113.9 ✓
BUBBLER	KCl	724.2	741.7	17.5 ✓
IMPINGER	KCl	621.8	627.4	5.6 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	758.1	762.4	4.3 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	730.2	730.9	0.7 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	718.9	718.7	-0.2 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	704.4	705.1	0.7 ✓
BUBBLER	SILICA GEL	935.7	950.0	14.3 ✓
			Total H <sub>2</sub> O (g)	143.5 ✓
FILTER				157 ✓
			Total Dust (g)	157.8P ✓

$V_{wstd} = 0.0474 * (H_2O \text{ g})$

$V_{mCorrected} = V_m * C_m$

$V_{mstd} = \frac{17.71 V_m C (P_b + \Delta H / 13.6)}{T_m}$

$V_{istd} = V_{wstd} + V_{mstd}$

$\%H_2O = (V_{wstd} / V_{istd}) * 100$

$Q_{nstd} = 17.71 Q_n P_s / T_s$

$\% \text{ Isokinetic} = V_{istd} / (Q_{nstd} * \text{Time})$

**DUST LOADING CALCULATIONS (Concentration Basis)**

$DCL = 15.432 (\text{dust g}) / V_{istd}$

$\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$

$ACFM = V_s * \text{Pipe Area (ft}^2\text{)}$

$SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$

$\text{lbs/hour} = \text{grains / scf} * 0.000143 * SCFM * 60$

\_\_\_\_\_ SCF  
 \_\_\_\_\_ ACF  
 \_\_\_\_\_ SCF  
 \_\_\_\_\_ SCF  
 \_\_\_\_\_ %H<sub>2</sub>O  
 \_\_\_\_\_ SCFM  
 \_\_\_\_\_ %  
 \_\_\_\_\_ grains/scf  
 \_\_\_\_\_ %  
 \_\_\_\_\_ ACFM  
 \_\_\_\_\_ SCFM  
 \_\_\_\_\_ lbs/hour

Sample Pt. \_\_\_\_\_

Date 7/15/99  
 Run 806-0ut3 (pm)outlet  
 Fund # \_\_\_\_\_  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	698.6	820.4	121.8 ✓
BUBBLER	KCl	619.9	643.2	23.3 ✓
IMPINGER	KCl	726.5	731.8	5.3 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	743.6	748.3	4.7 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	750.8	751.3	0.5 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	756.6	756.2	0.4 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	<del>574.6</del> 754.6	755.4	0.8 ✓
BUBBLER	SILICA GEL	808.2 ✓	826.7	18.5 ✓
			Total H <sub>2</sub> O (g)	156 ✓
FILTER			5 gpd	18.5
			Total Dust (g)	

$V_{w, std} = 0.0474 * (H_2O \text{ g})$  \_\_\_\_\_ SCF  
 $V_{m, Corrected} = V_m * C_m$  \_\_\_\_\_ ACF  
 $V_{m, std} = \frac{17.71 V_m C (P_s + \Delta H / 13.6)}{T_m}$  \_\_\_\_\_ SCF  
 $V_{i, std} = V_{w, std} + V_{m, std}$  \_\_\_\_\_ SCF  
 $\%H_2O = (V_{w, std} / V_{i, std}) * 100$  \_\_\_\_\_ %H<sub>2</sub>O  
 $Q_{n, std} = 17.71 Q_n P_s / T_s$  \_\_\_\_\_ SCFM  
 $\% \text{ Isokinetic} = V_{i, std} / (Q_{n, std} * \text{Time})$  \_\_\_\_\_ %  
**DUST LOADING CALCULATIONS (Concentration Basis)**  
 $DCL = 15.432 (\text{dust g}) / V_{i, std}$  \_\_\_\_\_ grams/scf  
 $\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$  \_\_\_\_\_ %  
 $ACFM = V_i * \text{Pipe Area (ft}^2)$  \_\_\_\_\_ ACFM  
 $SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$  \_\_\_\_\_ SCFM  
 $\text{lbs/hour} = \text{grams / scf} * 0.000143 * SCFM * 60$  \_\_\_\_\_ lbs/hour

- b. Select the "Input Data" option by moving the cursor over it and then pressing Enter. The following screens will appear:

**Field Data Input Screen:**

**Input Field Data:**

RUN NUMBER:  
RUN TYPE (C,L,P,V):  
DATE:  
TIME:  
UNITS (E or M):  
PLANT NAME:  
LOCATION:  
STACK ID:  
1ST OPERATOR:  
2ND OPERATOR:  
HOT BOX ID:  
CONTROL UNIT SN:  
PROCESSOR ID:  
PROBE SN:  
FILTER ID:  
NOZZLE SN:  
ORIFICE SN:

**Input Field Data:**

DELTA-AT:	inH2O
PITOT CP:	
AMBIENT TEMPERATURE:	degF
BAROMETRIC PRESSURE:	inHg
DGM MOISTURE CONTENT:	%
NOZZLE DIAMETER:	in
PROBE TEMPERATURE SETTING:	degF
PROBE LENGTH:	ft
HOTBOX TEMPERATURE SETTING:	degF
STACK GAS PRESSURE:	inH2O
STACK MOISTURE CONTENT:	%
DRY GAS MOLECULAR WEIGHT:	lb/M

Stack Geometry Data Input Screen:

Input Stack Geometry Data:

STACK GEOMETRY (C or R):  
STACK DIAMETER: in  
STACK WIDTH: in  
STACK LENGTH: in  
FRONT-WALL THICKNESS: in  
SIDE-WALL THICKNESS: in  
PORT LENGTH: in  
UPSTREAM DISTANCE: ft  
DOWNSTREAM DISTANCE: ft

Traverse Points Input Screen:

Input Traverse Points Rectangular: (\* If stack geometry is Rectangular)

TOTAL NUMBER OF POINTS:  
NO. X-DIRECTION POINTS:  
NO. Y-DIRECTION POINTS:  
FRONT-WALL DISTANCE: in  
X-DIRECTION INCREMENT: in  
SIDE-WALL DISTANCE: in  
Y-DIRECTION INCREMENT: in

Input Traverse Points Circular: (\* If stack geometry is Circular)

TOTAL NUMBER OF POINTS:  
P1 DISTANCE: in  
P2 DISTANCE: in  
P3 DISTANCE: in  
P4 DISTANCE: in  
P5 DISTANCE: in  
P6 DISTANCE: in  
P7 DISTANCE: in  
P8 DISTANCE: in  
P9 DISTANCE: in  
P10 DISTANCE: in  
P11 DISTANCE: in  
P12 DISTANCE: in  
P13 DISTANCE: in  
P14 DISTANCE: in  
P15 DISTANCE: in  
P16 DISTANCE: in

Calibration Data Input Screen: (\* If run type is Calibration)

Input Calibration Data:

PITOT OFFSET:	inH2O
PITOT SLOPE:	inH2O/V
PITOT ZERO VALUE:	inH2O
PITOT ZERO DATE:	
PITOT FULL SCALE VALUE:	inH2O
PITOT FULL SCALE DATE:	
ORIFICE OFFSET:	inH2O
ORIFICE SLOPE:	inH2O/V
ORIFICE ZERO VALUE:	inH2O
ORIFICE ZERO DATE:	
ORIFICE FULL SCALE VALUE:	inH2O
ORIFICE FULL SCALE DATE:	

End Of Run Data Input Screen: (\* If run type is Particulate or Velocity Traverse)

Input End Of Run Data:

DELTA-P AVG.:	inH2O
STACK TEMPERATURE AVG.:	degF
DELTA-H AVG:	inH2O
DGM TEMPERATURE AVG.:	degF
STACK VELOCITY AVG.:	ft/s
STACK FLOWRATE AVG.:	cfm
RUN TIME:	sec
GAS VOLUME:	cf
ISOKINETIC VARIATION AVG.:	%

- c. On the Control Unit go to the "1.6 Host Communication" menu and select the "3. Download Data" option.

When the "1.6.3. Download Data" menu appears, answer YES to the question "Do you really want to download data?". This causes the Control Unit to enter the host communication mode and be ready to "receive" the Run Data from the Host Computer.

- d. On the Host Computer, select the "Send Data" option by moving the cursor over it and then pressing Enter. This will start the Data Sending process.

You can monitor the progress of the operation on the "Sending Data Screen". This screen will show a series of rapidly changing messages during the downloading process. When the operation is completed, the message "@END" will appear on the screen.

You can exit the NAPPLINK program by pressing Escape and then selecting the "Goodbye" option.

- e. On the Control Unit, after the "Download Data" operation is completed, you can return to the "1.6 Host Communication" menu by pressing the 'A' key on the keypad. You can, then, optionally proceed to list the Data Bank contents to verify the presence of the Run Data downloaded from the Host Computer by selecting the "1. List Data Bank" option.

NAPP DATA DOWNLOAD

①

FIELD DATA

RUN\_NUMBER: 1  
 RUN\_TYPE: PARTICULATE  
 DATE: 7-16-99  
 TIME: 08:20  
 UNITS: ENGLISH  
 PLANT\_NAME: PRESQUE ISLE  
 LOCATION: MARQUETTE  
 STACK\_ID: 134  
 1ST\_OPERATR RS RS  
 2ND\_OPERA GD GD  
 HOT\_BOX\_ID:  
 CONTROL\_UNIT\_ID:  
 PROBE\_ID:  
 FILTER\_ID:  
 NOZZLE\_ID:  
 ORIFICE\_ID:  
 DELTA-AT: 1.70 ✓  
 PITOT\_CP: 0.84  
 TEMP\_AMB: 75  
 PRES\_ATM: 29.26 ✓  
 B\_WM: 0.005  
 NOZZLE\_DIA .185 / 0.150  
 PROBE\_TEMP\_SET 300  
 PROBE\_LENGTH: 12  
 HB\_TEMP\_SET: 250  
 LEAK\_RATE: 0.014  
 PRESS\_STAT: 29.11  
 B\_WS: 0.083  
 M\_DRY\_GAS: 30.39

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STACK GEOMETRY DATA

STACK\_GEOMETRY: CIRCULAR  
 STACK\_DIAMETER: 134 = 97.93  
 FRONT\_WALL\_THICK: 0.25  
 SIDE\_WALL\_THICK: 0.25  
 PORT\_LENGTH: 7.00  
 UPSTREAM\_DIST: +22  
 DOWNSTREAM\_DIST: +89

TRAVERS POINT DATA (CIRC)

NUM\_POINTS: 12

POINT\_NO DIST

1	12.90	S
2	26.56	
3	46.66	
4	101.34	
5	121.44	
6	135.10	
7	12.90	E
8	26.56	
9	46.66	
10	101.34	
11	121.44	
12	135.10	

PARTICULATE TRAVERS DATA

P_#	S_TIME	DH_V	TS	DP_S	DH_M	V_G	TM_I	TM_O	T_HB	T_PR	T_CB
1	600.13	3.52	283.76	2.84	2.28	8.814	75.31	74.98	245.72	298.14	70.55
2	600.00	2.32	283.17	2.90	1.04	5.792	84.22	81.93	261.41	299.27	68.94
3	600.00	2.31	284.29	2.95	1.08	5.813	92.13	88.74	260.19	301.02	67.53
4	600.00	2.43	284.43	2.98	1.09	5.831	100.81	95.03	249.54	300.54	65.72
5	600.00	2.56	285.02	2.90	1.08	5.781	107.32	102.65	254.10	299.96	65.87
6	600.71	2.57	284.89	2.81	1.06	5.693	112.42	106.18	248.12	299.15	65.02
7	600.23	2.60	285.13	2.63	0.93	5.058	85.69	83.42	262.93	300.67	72.19
8	600.00	2.73	286.27	2.79	0.98	5.224	93.57	91.08	248.33	298.32	69.11
9	600.00	2.82	286.89	2.85	1.03	5.269	99.48	96.24	252.57	301.45	67.34
10	600.00	2.89	287.04	2.78	1.03	5.213	106.36	102.97	258.52	305.11	66.39
11	600.00	2.85	287.42	2.72	1.00	5.139	110.13	105.35	249.67	298.37	66.41
12	600.57	2.91	286.12	2.53	0.99	5.132	113.42	107.81	253.28	298.01	66.35

*ΔP 1.6749*

END OF RUN DATA

DELTA-P\_AVE: 2.81  
 STACK\_TEMP\_AVE: 285.37 ✓  
 STACK\_VEL\_AVE: 112.33  
 STACK\_FLOW\_AVE 2.50E+07  
 DELTA-H\_AVE: 1.13 ✓  
 DGM\_TEMP\_AVE: 96.5517 ✓  
 RUN\_TIME: 7201.64 ✓  
 GAS\_VOLUME: 68.759 ✓  
 ISOKINETIC\_VAR: 104.76

*sec 120 min*

TRAVERS POINT DATA (CIRC)

NUM\_POINTS: 12

POINT\_NO DIST

1	12.90	E
2	26.56	
3	46.66	
4	101.34	
5	121.44	
6	135.10	
7	12.90	S
8	26.56	
9	46.66	
10	101.34	
11	121.44	
12	135.10	

PARTICULATE TRAVERS DATA

P_#	S_TIME	DH_V	TS	DP_S	DH_M	V_G	TM_I	TM_O	T_HB	T_PR	T_CB
1	600.19	3.03	296.83	2.41	0.86	4.466	78.49	76.48	240.29	302.59	71.34
2	600.00	3.09	297.30	2.47	0.90	4.508	87.38	83.72	256.83	298.07	70.18
3	600.00	3.06	298.19	2.51	0.93	4.534	95.10	90.09	264.81	299.32	68.93
4	600.00	3.19	298.64	2.53	0.94	4.552	102.94	97.55	254.17	300.78	68.03
5	600.00	3.18	298.52	2.51	0.95	4.536	109.31	104.53	249.54	306.82	67.12
6	600.93	3.21	297.85	2.42	0.92	4.467	114.65	108.87	246.88	302.45	66.89
7	600.17	3.17	298.38	2.56	0.93	4.648	87.45	85.23	252.02	300.57	70.96
8	600.00	3.24	299.03	2.61	0.96	4.694	95.03	91.61	257.77	301.37	69.99
9	600.00	3.45	299.86	2.66	0.99	4.739	102.33	98.25	250.94	302.44	69.27
10	600.00	3.62	300.19	2.60	0.98	4.682	109.11	104.40	254.04	298.73	68.72
11	600.00	3.71	299.59	2.55	0.97	4.603	112.97	107.12	249.97	303.71	68.38
12	600.85	3.68	298.40	2.48	0.94	4.553	115.62	109.94	253.76	301.60	67.62

1.58912

END OF RUN DATA

DELTA-P\_AVE: 2.53  
 STACK\_TEMP\_AVE: 298.57  
 STACK\_VEL\_AVE: 107.52  
 STACK\_FLOW\_AVE 2.35E+07  
 DELTA-H\_AVE: 0.94  
 DGM\_TEMP\_AVE: 98.67  
 RUN\_TIME: 7202.14  
 GAS\_VOLUME: 54.982  
 ISOKINETIC\_VAR: 90.98

## FIELD DATA

RUN\_NUMBER: 2  
RUN\_TYPE: PARTICULATE  
DATE: 7-16-99  
TIME: 11:15  
UNITS: ENGLISH  
PLANT\_NAME: PRESQUE ISLE  
LOCATION: MARQUETTE  
STACK\_ID: 134  
1ST\_OPERAT RS RS  
2ND\_OPERA GD GD  
HOT\_BOX\_ID:  
CONTROL\_UNIT\_ID:  
PROBE\_ID:  
FILTER\_ID:  
NOZZLE\_ID:  
ORIFICE\_ID:  
DELTA-AT: 1.70  
PITOT\_CP: 0.84  
TEMP\_AMB: 78  
PRES\_ATM: 29.26  
B\_WM: 0.005  
NOZZLE\_DIAM: 0.152  
PROBE\_TEMP\_SET 300  
PROBE\_LENGTH: 12  
HB\_TEMP\_SET: 250  
LEAK\_RATE: 0.011  
PRESS\_STAT: 29.11  
B\_WS: 0.085  
M\_DRY\_GAS: 30.22

## STACK GEOMETRY DATA

STACK\_GEOMETRY: CIRCULAR  
STACK\_DIAMETER: 134  
FRONT\_WALL\_THICK: 0.25  
SIDE\_WALL\_THICK: 0.25  
PORT\_LENGTH: 7.00  
UPSTREAM\_DIST: +22  
DOWNSTREAM\_DIST: +89

TRAVERS POINT DATA (CIRC)

NUM\_POINTS: 12

POINT\_NO DIST

1	12.90	S
2	26.56	
3	46.66	
4	101.34	
5	121.44	
6	135.10	
7	12.90	E
8	26.56	
9	46.66	
10	101.34	
11	121.44	
12	135.10	

PARTICULATE TRAVERS DATA

P_#	S_TIME	DH_V	TS	DP_S	DH_M	V_G	TM_I	TM_O	T_HB	T_PR	T_CB
1	600.11	2.87	308.51	2.80	0.93	5.081	79.52	78.37	254.71	310.67	73.85
2	600.00	2.92	310.92	2.89	0.97	5.122	88.49	84.41	259.51	309.28	71.06
3	600.00	2.91	311.24	2.95	1.00	5.197	96.08	91.13	250.84	301.27	69.16
4	600.00	2.98	310.98	2.96	1.02	5.204	103.56	98.21	246.37	305.96	68.21
5	600.00	3.01	310.41	2.89	1.01	5.147	110.23	105.38	256.61	299.92	67.31
6	601.42	3.21	309.52	2.79	0.98	5.098	115.44	109.61	251.55	303.33	67.17
7	600.21	3.19	309.76	2.76	0.93	4.812	88.75	86.34	247.39	305.84	72.32
8	600.00	3.24	310.47	2.82	0.96	4.839	98.12	94.57	252.58	304.01	71.94
9	600.00	3.30	311.03	2.93	1.01	4.926	103.59	99.04	249.99	297.34	71.03
10	600.00	3.35	310.95	2.94	1.02	4.951	110.21	105.46	255.47	306.75	68.25
11	600.00	3.32	310.05	2.79	0.98	4.952	113.87	108.28	250.09	302.52	67.43
12	600.61	3.39	309.32	2.77	0.97	4.832	115.35	110.80	252.16	308.28	67.92

1.69028

END OF RUN DATA

DELTA-P\_AVE: 2.86  
 STACK\_TEMP\_AVE: 310.26  
 STACK\_VEL\_AVE: 115.18  
 STACK\_FLOW\_AVE 2.46E+07  
 DELTA-H\_AVE: 0.98  
 DGM\_TEMP\_AVE: 99.78  
 RUN\_TIME: 7202.35  
 GAS\_VOLUME: 60.161  
 ISOKINETIC\_VAR: 97.43

## FIELD DATA

RUN\_NUMBER: 3  
RUN\_TYPE: PARTICULATE  
DATE: 7-16-99  
TIME: 14:10  
UNITS: ENGLISH  
PLANT\_NAME: PRESQUE ISLE  
LOCATION: MARQUETTE  
STACK\_ID: 134  
1ST\_OPERATORS: RS  
2ND\_OPERATOR: GD  
HOT\_BOX\_ID:  
CONTROL\_UNIT\_ID:  
PROBE\_ID:  
FILTER\_ID:  
NOZZLE\_ID:  
ORIFICE\_ID:  
DELTA-AT: 1.70  
PITOT\_CP: 0.84  
TEMP\_AMB: 81  
PRES\_ATM: 29.29  
B\_WM: 0.005  
NOZZLE\_DIAM: 0.150  
PROBE\_TEMP\_SET: 300  
PROBE\_LENGTH: 12  
HB\_TEMP\_SET: 250  
LEAK\_RATE: 0.007  
PRESS\_STAT: 29.14  
B\_WS: 0.091  
M\_DRY\_GAS: 30.38

## STACK GEOMETRY DATA

STACK\_GEOMETRY: CIRCULAR  
STACK\_DIAMETER: 134  
FRONT\_WALL\_THICK: 0.25  
SIDE\_WALL\_THICK: 0.25  
PORT\_LENGTH: 7.00  
UPSTREAM\_DIST: +22  
DOWNSTREAM\_DIST: +89

DATE 7-16-99  
 RUN # Unit 1-4 Stack run 1  
 FUND # 5344  
 COST CENTER NUMBER \_\_\_\_\_

5 on computer

DUST LOADING DATA SHEET

Time at Start 8:20  
 Sample Pt. \_\_\_\_\_  
 $P_B$  (Barometric Pressure) = 29.26

Operators R8 / JLD  
 Traverse Pt. \_\_\_\_\_

$P_s$  (Stack Pressure) =  $P_B \pm$  ( \_\_\_\_\_ ) in  $H_2O/13.6$  = \_\_\_\_\_ in Hg  
 $T_s$  (Stack Temp) = 283 °F + 460 = \_\_\_\_\_ °R

5/6

$\Delta P$  (Pitot) = \_\_\_\_\_ in  $H_2O$  Type S  $C_p = .84$  Standard  
 $D_n$  (Nozzle Diam) = 185 / 150 in changed at 1st port R8  
 Approx %  $H_2O$  = \_\_\_\_\_  
 $\Delta H @$  = \_\_\_\_\_ in  $H_2O$   $C_m$  = \_\_\_\_\_

$V_s$  (Stack Velocity) =  $951.6 C_p \sqrt{\frac{\Delta P}{P_s}}$  = \_\_\_\_\_ ft/min

$Q_n$  (Nozzle flow Rate) =  $V_s \pi D_n^2 / 576$  = \_\_\_\_\_ ACFM

$Q_m$  (meter flow rate) =  $Q_n T_m Q_n (1 - \%H_2O) =$  \_\_\_\_\_ ACFM  
 $C_m T_s (P_B + \Delta H / 13.6)$  100

$\Delta H$  (orifice) =  $\frac{Q_m^2 \Delta H @ (P_B + \Delta H / 13.6)}{0.03175 T_m} =$  \_\_\_\_\_ in  $H_2O$

Second/Rev = \_\_\_\_\_ %  $CO_2$  \_\_\_\_\_ %  $O_2$

Note: Standard Temperature and Pressure are 70 °F and 29.92 in Hg

S/R	Trav # Point	Time	Gas Meter	$\Delta P$	$\Delta H$	Pump Vac.	Stack Temp.	Probe Temp.	Meter In	Meter Out				
	1	8:20	881.342											
			923.030		End									
					leak ✓ - OK									
	2		923.193											
			957.961		End									
					leak ✓ - OK									

Filter .15085  
 Comments: change nozzle at the 1st loc. = 28 to 109  
74 89 109 150 to

127 121 135

Sample Pt. \_\_\_\_\_

Date \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Run Unit 1-4 Stack, sample # 1

Fund # \_\_\_\_\_

Cost Center # \_\_\_\_\_

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	698.2	774.6	76.4 ✓
BUBBLER	KCl	713.3	740.4	27.1 ✓
IMPINGER	KCl	596.4	605.1	8.7 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	728.6	732.4	3.8 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	701.4	700.9	-0.5 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	708.9	709.3	.4 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	691.9	693.9	2.0 ✓
BUBBLER	SILICA GEL	931.1	952.1	21 ✓
		Total H <sub>2</sub> O (g)		138.9
FILTER		.15085	.15359	.00274
		H <sub>2</sub> O = 117.9 ✓		
		SG = 21		
		Total Dust (g)		

$V_{wstd} = 0.0474 * (H_2O \text{ g})$

$V_{mCorrected} = V_m * C_m$

$V_{mstd} = \frac{17.71 V_m C (P_s + AH/13.6)}{J_m}$

$V_{istd} = V_{wstd} + V_{mstd}$

$\%H_2O = (V_{wstd} / V_{istd}) * 100$

$Q_{nstd} = 17.71 Q_n P_s / T_s$

$\% \text{ Isokinetic} = V_{istd} / (Q_{nstd} * \text{Time})$

**DUST LOADING CALCULATIONS (Concentration Basis)**

$DCL = 15.432 (\text{dust g}) / V_{istd}$

$\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$

$ACFM = V_i * \text{Pipe Area (ft}^2)$

$SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$

$\text{lbs/hour} = \text{grains / scf} * 0.000143 * SCFM * 60$

\_\_\_\_\_ SCF

\_\_\_\_\_ ACF

\_\_\_\_\_ SCF

\_\_\_\_\_ SCF

\_\_\_\_\_ %H<sub>2</sub>O

\_\_\_\_\_ SCFM

\_\_\_\_\_ %

\_\_\_\_\_ grains/scf

\_\_\_\_\_ %

\_\_\_\_\_ ACFM

\_\_\_\_\_ SCFM

\_\_\_\_\_ lbs/hour

DATE 7-16-99

RUN # Unit 1-4 stack-run 2 (6 on computer)

FUND # 5344

COST CENTER NUMBER \_\_\_\_\_

**DUST LOADING DATA SHEET**

Time at Start 11:15

Operators RL / GD

Sample Pt. 1-4 Stack

Traverse Pt. E45

$P_B$  (Barometric Pressure) = 29.26 in. Hg

$P_s$  (Stack Pressure) =  $P_B \pm$  ( \_\_\_\_\_ ) in  $H_2O/13.6$  =  in Hg

$T_s$  (Stack Temp) = \_\_\_\_\_ °F + 46 =  °R

$\Delta P$  (Pitot) = \_\_\_\_\_ in  $H_2O$  \_\_\_\_\_ Type S  $C_p = .84$  \_\_\_\_\_ Standard

$D_n$  (Nozzle Diam) = .152 in Approx %  $H_2O$  = 10

$\Delta H @$  = \_\_\_\_\_ in  $H_2O$   $C_m$  = \_\_\_\_\_

$V_s$  (Stack Velocity) =  $951.6 C_p \sqrt{\frac{\Delta P}{P_s T_s}}$  = \_\_\_\_\_ ft/min

$Q_n$  (Nozzle flow Rate) =  $V_s \pi D_n^2 / 576$  = \_\_\_\_\_ ACFM

$Q_m$  (meter flow rate) =  $\frac{Q_n T_m Q_n}{C_m T_s (P_B + \Delta H / 13.6)} (1 - \%H_2O)$  = \_\_\_\_\_ ACFM

$\Delta H$  (orifice) =  $\frac{Q_m^2 \Delta H @ (P_B + \Delta H / 13.6)}{0.03175 T_m}$  = \_\_\_\_\_ in  $H_2O$

Second/Rev = \_\_\_\_\_ %  $CO_2$  \_\_\_\_\_ %  $O_2$

Note: Standard Temperature and Pressure are 70 °F and 29.92 in Hg

S/R	Trav. Point	Time	Gas Meter	$\Delta P$	$\Delta H$	Pump Vac.	Stack Temp.	Probe Temp.	Meter In	Meter Out				
	1	11:15	958.073											
			988.186											
			Leak	✓										
	2	12:30	988.286											
			1019.686											

Comments: -15076 Pne Leak ✓ OK

Sample Pt. \_\_\_\_\_

Date 7/16/99  
 Run Unit 1-4 Stack-run 2  
 Fund # 5344  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	753.8	<del>667.9</del> 830.2 <i>kw</i>	76.4 ✓
BUBBLER	KCl	723.4	735.8	12.4 ✓
IMPINGER	KCl	734.9	737.1	2.2 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	742.2	744.3	2.1 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	733.8	733.4	-.4 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	625.8	626.2	.4 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	706.8	707.5	.7 ✓
BUBBLER	SILICA GEL	968.0	980.3	12.3 ✓
		Total H <sub>2</sub> O (g)		106.1
FILTER		15096	15126	.00080
		H <sub>2</sub> O = 93.8 ✓		
		SG = 12.3		
		Total Dust (g)		

$V_{wstd} = 0.0474 * (H_2O \text{ g})$

$V_{m \text{ Corrected}} = V_m * C_m$

$V_{mstd} = \frac{17.71 V_m C (P_b + \Delta H / 13.6)}{T_m}$

$V_{istd} = V_{wstd} + V_{mstd}$

$\%H_2O = (V_{wstd} / V_{istd}) * 100$

$Q_{nstd} = 17.71 Q_n P_s / T_s$

$\% \text{ Isokinetic} = V_{istd} / (Q_{nstd} * \text{Time})$

**DUST LOADING CALCULATIONS (Concentration Basis)**

$DCL = 15.432 (\text{dust g}) / V_{istd}$

$\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL})}{\text{Inlet DCL}} * 100$

$ACFM = V_s * \text{Pipe Area (ft}^2\text{)}$

$SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$

$\text{lbs/hour} = \text{grains / scf} * 0.000143 * SCFM * 60$

\_\_\_\_\_ SCF

\_\_\_\_\_ ACF

\_\_\_\_\_ SCF

\_\_\_\_\_ SCF

\_\_\_\_\_ %H<sub>2</sub>O

\_\_\_\_\_ SCFM

\_\_\_\_\_ %

\_\_\_\_\_ grains/scf

\_\_\_\_\_ %

\_\_\_\_\_ ACFM

\_\_\_\_\_ SCFM

\_\_\_\_\_ lbs/hour

DATE 7/16/99  
 RUN # Unit 1-4 Stack, Ln #3  
 FUND # \_\_\_\_\_  
 COST CENTER NUMBER \_\_\_\_\_

**DUST LOADING DATA SHEET**

Time at Start 14:10

Operators RS / JO

Sample Pt. Stack

Traverse Pt. \_\_\_\_\_

$P_B$  (Barometric Pressure) = 29.29 in. Hg

$P_s$  (Stack Pressure) =  $P_B \pm$  (-2) in  $H_2O/13.6$  = 29.17 in Hg

$T_s$  (Stack Temp) = 310 °F + 46 = 770 °R

$\Delta P$  (Pitot) = 2.85 in  $H_2O$  Y Type S  $C_p = .84$  Standard

$D_n$  (Nozzle Diam) = .150 in Approx %  $H_2O$  = 10

$\Delta H @$  = 1.96 in  $H_2O$   $C_m$  = .96

STACK ID  
134

$V_s$  (Stack Velocity) =  $951.6 C_p \sqrt{\frac{\Delta P}{P_s T_s}}$  = 6938 ft/min

$Q_n$  (Nozzle flow Rate) =  $V_s \pi D_n^2 / 576$  = .8512 ACFM

$Q_m$  (meter flow rate) =  $Q_n T_m Q_n (1 - \%H_2O) / (C_m T_s (P_B + \Delta H/13.6))$  = .5813 ACFM

$\Delta H$  (orifice) =  $\frac{Q_m^2 \Delta H @ (P_B + \Delta H/13.6)}{0.03175 T_m}$  = .99 in  $H_2O$

Second/Rev = 10.7 %  $CO_2$  %  $O_2$  \_\_\_\_\_

Note: Standard Temperature and Pressure are 70 °F and 29.92 in Hg

85

S/R	Trav. Point	Time	Gas Meter	$\Delta P$	$\Delta H$	Pump Vac.	Stack Temp.	Probe Temp.	Meter In	Meter Out			
1		14:10	20.177										
			Leak	Y	~	1 CF							
2		15:18	~			computer							
				78.8137		DGM							
			87.736			DGM			84.8667		computer		
			60.559										

Comments: \_\_\_\_\_

Sample Pt. \_\_\_\_\_

Date 7/16/99  
 Run Unit 1-4 Stack, Run 3  
 Fund # \_\_\_\_\_  
 Cost Center # \_\_\_\_\_

Train Type : **ONTARIO-HYDRO METHOD**

Stopper Type	Type Of Solution	Initial Wt. (g)	Final Wt. (g)	Net Wt. (g)
BUBBLER	KCl	713.9	796.1	82.2 ✓
BUBBLER	KCl	707.9	726.9	19.0 ✓
IMPINGER	KCl	712.3	716.5	4.2 ✓
BUBBLER	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	615.9	620.1	4.2 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	700.5	700.4	-0.1 ✓
BUBBLER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	743.0	743.9	.9 ✓
IMPINGER	KMnO <sub>4</sub> /H <sub>2</sub> SO <sub>4</sub>	718.6	718.5	-0.1 ✓
BUBBLER	SILICA GEL	930.6	946.0	15.4 ✓
		Total H <sub>2</sub> O (g)		125.7 ✓
FILTER		-15549	.15619	.00070
		H <sub>2</sub> O	110.3	
		DG=	15.4	
		Total Dust (g)		

$V_{wstd} = 0.0474 * (H_2O \text{ g})$   
 $V_m \text{ Corrected} = V_m * C_m$   
 $V_{mstd} = \frac{17.71 V_m C (P_s + \Delta H / 13.6)}{T_m}$   
 $V_sstd = V_{wstd} + V_{mstd}$   
 $\% H_2O = (V_{wstd} / V_sstd) * 100$   
 $Q_{nstd} = 17.71 Q_n P_s / T_s$   
 $\% \text{ Isokinetic} = V_sstd / (Q_{nstd} * \text{Time})$   
**DUST LOADING CALCULATIONS (Concentration Basis)**  
 $DCL = 15.432 (\text{dust g}) / V_sstd$   
 $\% \text{ Efficiency} = \frac{(\text{Inlet DCL} - \text{Outlet DCL}) * 100}{\text{Inlet DCL}}$   
 $ACFM = V_s * \text{Pipe Area (ft}^2)$   
 $SCFM = ACFM * P_s / 29.92 * 530 / T_s = ACFM * P_s / T_s * 17.71$   
 $\text{lbs/hour} = \text{grams / scf} * 0.000143 * SCFM * 60$

5.927	SCF
63.897	ACF
61.000	SCF
67.027	SCF
8.8	%H <sub>2</sub> O
.570	SCFM
97.9	%
0.0002	grams/scf
	%
	ACFM
	SCFM
	lbs/hour

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**APPENDIX D**  
**LABORATORY ANALYTICAL REPORTS**

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**PROCESS SOLID SAMPLES ANALYTICAL REPORT**

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CONSOL INC.  
RESEARCH & DEVELOPMENT  
ANALYTICAL LABORATORY  
4000 BROWNSVILLE ROAD, LIBRARY, PA 15129

DESCRIPTION PRESQUE ISLE COAL SAMPLE

SAMPLE NUMBER UNIT 1 - 4 COMPOSITE

DATE LOGGED 07/26/99  
DATE COMPLETED 08/26/99  
PROJECT NUMBER 1621-29 -7  
ANALYTICAL NUMBER 994581

ANALYSIS REPORT

<u>PROXIMATE</u>	<u>(Dry)%</u>	<u>ULTIMATE</u>	<u>(Dry)%</u>	<u>MAJOR ASH ELEM</u>	<u>%</u>
Ash	9.79	Carbon	73.90	Ignited at 750 C	
Volatile Matter	35.95	Hydrogen	4.76	SiO2	56.30
Fixed Carbon	54.26	Nitrogen	1.56	Al2O3	25.05
		Chlorine	0.021	TiO2	0.81
Sulfur, Total	0.98	Sulfur, Total	0.98	Fe2O3	4.75
BTU/lb	12872	Ash	9.79	CaO	3.19
MAF BTU/lb	14269	Oxygen (DIFF)	8.99	MgO	1.67
				Na2O	2.19
				K2O	0.95
				P2O5	0.47
				SO3	2.92
				UND	1.70
<u>MISC. (As Det.)</u>					
Hg	22 ppb				

AS DETERMINED MOISTURE: 5.38 %

DISTRIBUTION:  
M. DEVITO

Approved for transmittal



CONSOL INC.  
 RESEARCH & DEVELOPMENT  
 ANALYTICAL LABORATORY  
 4000 BROWNSVILLE ROAD, LIBRARY, PA 15129

DESCRIPTION      PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER BAGHOUSE 1

DATE LOGGED      07/23/99  
 DATE COMPLETED 08/25/99  
 PROJECT NUMBER 1621-29 -7  
 ANALYTICAL NUMBER 994540

ANALYSIS REPORT

<u>PROXIMATE</u> (Dry)%	<u>ULTIMATE</u> (Dry)%	<u>MAJOR ASH ELEM</u> (Dry)%
Ash                                      69.66	Carbon                                      28.91	SiO2    43.21
Sulfur, Total                              0.92	Hydrogen                                      0.03	Al2O3    15.55
	Nitrogen                                      0.29	TiO2    0.44
<u>MISC. (As Det.)</u>	Sulfur, Total                              0.92	Fe2O3    4.35
	Ash    69.66	CaO    2.41
Hg    131 ppb	Oxygen (DIFF)                              0.15	MgO    1.17
		Na2O    1.38
		K2O    0.74
		P2O5    0.25
		SO3    0.40
		UND    30.10

AS DETERMINED MOISTURE: 0.35 %

DISTRIBUTION:  
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DESCRIPTION      PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER BAGHOUSE 2

DATE LOGGED      07/23/99  
 DATE COMPLETED 08/25/99  
 PROJECT NUMBER 1621-29 -7  
 ANALYTICAL NUMBER 994541

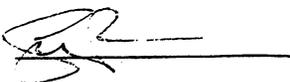
ANALYSIS REPORT

<u>PROXIMATE</u>	<u>(Dry)%</u>	<u>ULTIMATE</u>	<u>(Dry)%</u>	<u>MAJOR ASH ELEM</u>	<u>(Dry)%</u>
Ash	74.58	Carbon	24.19	SiO2	46.85
Sulfur, Total	0.92	Hydrogen	0.00	Al2O3	16.64
		Nitrogen	0.22	TiO2	0.49
<u>MISC. (As Det.)</u>		Sulfur, Total	0.92	Fe2O3	5.15
		Ash	74.58	CaO	2.56
Hg	145 ppb	Oxygen (DIFF)	0.06	MgO	1.33
				Na2O	1.51
				K2O	0.79
				P2O5	0.28
				SO3	0.42
				UND	23.98

AS DETERMINED MOISTURE: 0.25 %

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DESCRIPTION PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER BAGHOUSE 3

DATE LOGGED 07/23/99  
DATE COMPLETED 08/25/99  
PROJECT NUMBER 1621-29 -7  
ANALYTICAL NUMBER 994542

ANALYSIS REPORT

<u>PROXIMATE</u> (Dry)%		<u>ULTIMATE</u> (Dry)%		<u>MAJOR ASH ELEM</u> (Dry)%	
Ash	71.88	Carbon	26.84	SiO <sub>2</sub>	46.07
Sulfur, Total	0.92	Hydrogen	-0.01	Al <sub>2</sub> O <sub>3</sub>	15.25
		Nitrogen	0.28	TiO <sub>2</sub>	0.41
<u>MISC. (As Det.)</u>		Sulfur, Total	0.92	Fe <sub>2</sub> O <sub>3</sub>	5.15
Hg	129 ppb	Ash	71.88	CaO	2.44
		Oxygen (DIFF)	0.06	MgO	1.25
				Na <sub>2</sub> O	1.39
				K <sub>2</sub> O	0.76
				P <sub>2</sub> O <sub>5</sub>	0.24
				SO <sub>3</sub>	0.34
				UND	26.70

AS DETERMINED MOISTURE: 0.36 %

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DESCRIPTION      PRESQUE ISLE COAL SAMPLE

SAMPLE NUMBER UNIT 6 - TEST 1

DATE LOGGED      07/26/99  
 DATE COMPLETED 08/12/99  
 PROJECT NUMBER 1621-29 -7  
 ANALYTICAL NUMBER 994572

ANALYSIS REPORT

<u>PROXIMATE</u> (Dry)%	<u>ULTIMATE</u> (Dry)%	<u>MAJOR ASH ELEM</u> %			
Ash	10.28	Carbon	72.90	Ignited at 750 C	
Volatile Matter	37.83	Hydrogen	4.64	SiO <sub>2</sub>	55.57
Fixed Carbon	51.89	Nitrogen	1.57	Al <sub>2</sub> O <sub>3</sub>	24.78
		Chlorine	0.020	TiO <sub>2</sub>	0.80
Sulfur, Total	1.02	Sulfur, Total	1.02	Fe <sub>2</sub> O <sub>3</sub>	5.42
BTU/lb	12694	Ash	10.28	CaO	3.51
MAF BTU/lb	14148	Oxygen (DIFF)	9.57	MgO	1.78
				Na <sub>2</sub> O	2.12
<u>MISC. (As Det.)</u>				K <sub>2</sub> O	1.05
Hg	24.5 PPB			P <sub>2</sub> O <sub>5</sub>	0.46
				SO <sub>3</sub>	3.69
				UND	0.82

AS DETERMINED MOISTURE: 5.17 %

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DESCRIPTION      PRESQUE ISLE COAL SAMPLE

SAMPLE NUMBER UNIT 6 - TEST 2

DATE LOGGED      07/26/99  
 DATE COMPLETED 08/12/99  
 PROJECT NUMBER 1621-29 -7  
 ANALYTICAL NUMBER 994573

ANALYSIS REPORT

<u>PROXIMATE</u> (Dry)%	<u>ULTIMATE</u> (Dry)%	<u>MAJOR ASH ELEM</u> %			
		Ignited at 750 C			
Ash	10.05	Carbon	72.84	SiO2	55.59
Volatile Matter	38.10	Hydrogen	4.64	Al2O3	25.29
Fixed Carbon	51.85	Nitrogen	1.61	TiO2	0.82
		Chlorine	0.021	Fe2O3	5.10
Sulfur, Total	1.04	Sulfur, Total	1.04	CaO	3.27
BTU/lb	12784	Ash	10.05	MgO	1.69
MAF BTU/lb	14212	Oxygen (DIFF)	9.80	Na2O	2.08
				K2O	1.02
<u>MISC. (As Det.)</u>				P2O5	0.46
Hg	46 PPB			SO3	3.20
				UND	1.48

AS DETERMINED MOISTURE: 5.10 %

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DESCRIPTION      PRESQUE ISLE COAL SAMPLE

SAMPLE NUMBER UNIT 6 - TEST 3

DATE LOGGED      07/26/99  
DATE COMPLETED 08/13/99  
PROJECT NUMBER 1621-29 -7  
ANALYTICAL NUMBER 994574

ANALYSIS REPORT

<u>PROXIMATE</u> (Dry)%	<u>ULTIMATE</u> (Dry)%	<u>MAJOR ASH ELEM</u> %			
Ash	9.99	Carbon	74.46	Ignited at 750 C	
Volatile Matter	38.04	Hydrogen	4.76	SiO2	57.17
Fixed Carbon	51.97	Nitrogen	1.61	Al2O3	25.89
		Chlorine	0.018	TiO2	0.83
Sulfur, Total	1.04	Sulfur, Total	1.04	Fe2O3	5.00
BTU/lb	12772	Ash	9.99	CaO	3.31
MAF BTU/lb	14190	Oxygen (DIFF)	8.12	MgO	1.75
				Na2O	2.15
				K2O	1.05
				P2O5	0.46
				SO3	3.07
				UND	-0.68
<u>MISC. (As Det.)</u>					
Hg	41 PPB				

AS DETERMINED MOISTURE: 5.10 %

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DESCRIPTION PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER UNIT 6 #1 - FRONT

DATE LOGGED 07/23/99  
DATE COMPLETED 08/25/99  
PROJECT NUMBER 1621-29 -7  
ANALYTICAL NUMBER 994547

ANALYSIS REPORT

<u>PROXIMATE</u>	<u>(Dry)%</u>	<u>ULTIMATE</u>	<u>(Dry)%</u>	<u>MAJOR ASH ELEM</u>	<u>(Dry)%</u>
Ash	83.41	Carbon	15.57	SiO <sub>2</sub>	49.67
Sulfur, Total	0.62	Hydrogen	-0.02	Al <sub>2</sub> O <sub>3</sub>	21.12
		Nitrogen	0.18	TiO <sub>2</sub>	0.66
<u>MISC. (As Det.)</u>		Sulfur, Total	0.62	Fe <sub>2</sub> O <sub>3</sub>	4.09
		Ash	83.41	CaO	2.56
Hg	67 ppb	Oxygen (DIFF)	0.21	MgO	1.37
				Na <sub>2</sub> O	1.67
				K <sub>2</sub> O	0.80
				P <sub>2</sub> O <sub>5</sub>	0.35
				SO <sub>3</sub>	0.38
				UND	17.33

AS DETERMINED MOISTURE: 0.34 %

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DESCRIPTION      PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER UNIT 6 #2 - FRONT

DATE LOGGED      07/23/99  
 DATE COMPLETED 08/25/99  
 PROJECT NUMBER 1621-29 -7  
 ANALYTICAL NUMBER 994548

ANALYSIS REPORT

<u>PROXIMATE</u> (Dry)%	<u>ULTIMATE</u> (Dry)%	<u>MAJOR ASH ELEM</u> (Dry)%
Ash                                      81.80	Carbon                                      17.39	SiO2    50.01
Sulfur, Total                              0.65	Hydrogen                                      -0.01	Al2O3    20.67
	Nitrogen                                      0.21	TiO2    0.66
<u>MISC. (As Det.)</u>	Sulfur, Total                                      0.65	Fe2O3    4.13
	Ash    81.80	CaO    2.75
Hg    69 ppb	Oxygen (DIFF)                                      -0.07	MgO    1.38
		Na2O    1.75
		K2O    0.81
		P2O5    0.35
		SO3    0.37
		UND    17.12

AS DETERMINED MOISTURE: 0.32 %

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DESCRIPTION      PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER UNIT 6 #3 - FRONT

DATE LOGGED      07/23/99  
 DATE COMPLETED 08/25/99  
 PROJECT NUMBER 1621-29 -7  
 ANALYTICAL NUMBER 994549

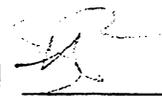
ANALYSIS REPORT

<u>PROXIMATE</u> (Dry)%	<u>ULTIMATE</u> (Dry)%	<u>MAJOR ASH ELEM</u> (Dry)%
Ash                                      81.17	Carbon                                      17.65	SiO2    48.72
Sulfur, Total                              0.66	Hydrogen                                      0.00	Al2O3    20.38
	Nitrogen                                      0.21	TiO2    0.66
<u>MISC. (As Det.)</u>	Sulfur, Total                              0.66	Fe2O3    4.09
	Ash    81.17	CaO    2.78
Hg    80 ppb	Oxygen (DIFF)                              0.29	MgO    1.37
		Na2O    1.72
		K2O    0.81
		P2O5    0.36
		SO3    0.37
		UND    18.74

AS DETERMINED MOISTURE: 0.27 %

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DESCRIPTION PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER UNIT 6 #1 - BACK

DATE LOGGED 07/23/99  
DATE COMPLETED 08/10/99  
PROJECT NUMBER 1621-29 -7  
ANALYTICAL NUMBER 994550

ANALYSIS REPORT

<u>PROXIMATE</u>	<u>(Dry)%</u>	<u>ULTIMATE</u>	<u>(Dry)%</u>
Ash	79.72	Carbon	18.64
Sulfur, Total	0.86	Hydrogen	-0.03
		Nitrogen	0.22
<u>MISC. (As Det.)</u>		Sulfur, Total	0.86
Hg	228	Ash	79.72
		Oxygen (DIFF)	0.55

AS DETERMINED MOISTURE: 0.41 %

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DESCRIPTION PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER UNIT 6 #2 - BACK

DATE LOGGED 07/23/99  
DATE COMPLETED 08/10/99  
PROJECT NUMBER 1621-29 -7  
ANALYTICAL NUMBER 994551

ANALYSIS REPORT

<u>PROXIMATE</u>	<u>(Dry)%</u>	<u>ULTIMATE</u>	<u>(Dry)%</u>
Ash	80.12	Carbon	18.27
Sulfur, Total	0.82	Hydrogen	0.01
		Nitrogen	0.20
<u>MISC. (As Det.)</u>		Sulfur, Total	0.82
Hg	280	Ash	80.12
		Oxygen (DIFF)	0.54

AS DETERMINED MOISTURE: 0.36 %

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DESCRIPTION      PRESQUE ISLE ASH SAMPLES

SAMPLE NUMBER UNIT 6 #3 - BACK

DATE LOGGED      07/23/99  
DATE COMPLETED 08/10/99  
PROJECT NUMBER 1621-29 -7  
ANALYTICAL NUMBER 994552

ANALYSIS REPORT

<u>PROXIMATE</u>	<u>(Dry)%</u>	<u>ULTIMATE</u>	<u>(Dry)%</u>
Ash	80.23	Carbon	18.36
Sulfur, Total	0.81	Hydrogen	0.00
		Nitrogen	0.20
<u>MISC. (As Det.)</u>		Sulfur, Total	0.81
		Ash	80.23
Hg	264	Oxygen (DIFF)	0.38

AS DETERMINED MOISTURE: 0.22 %

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Unit 6  
Test 1  
Coal

PROCESS STREAM SAMPLING SHEET

Plant WEPCO Presque Isle Sample Stream: Unit #6 Coal

Date 7/14/99

Increment	1	2	3	4	5	6	7	8
Time	1415	1435	1455	1515	1535	1555	1615	1635
Weight / Volume	500g							
Comp / Grab								
Process Status	75 mw	75	75	75	75	75	75	75
Sampler Condition	Clean							
Container Condition	Clean							
Container Label	yes							
Sampler	MSD	MSD	MSD	MSD	MSD	MSD	MSD	MSD
Sample Stored	yes							
pH (if required)								
Temperature								
Preservative								
	A-1	A-2	B-1	B-2	C-1	C-2	D-1	D-2

Test ID Unit #6 - Test 1  
 Sample Stream Unit #6 Coal  
 Sample ID Unit 6 - Test 1 - Coal  
 Target Size 3-5 kg  
 Sample Device mill sampler  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Bag / Bag / Bucket  
 Frequency 20 min  
 Safety Issues Dust  
 Protective Gear mask

Composite Logged? Yes

Sample Stored? Yes

Storage Method: Bag / Bag / Bucket

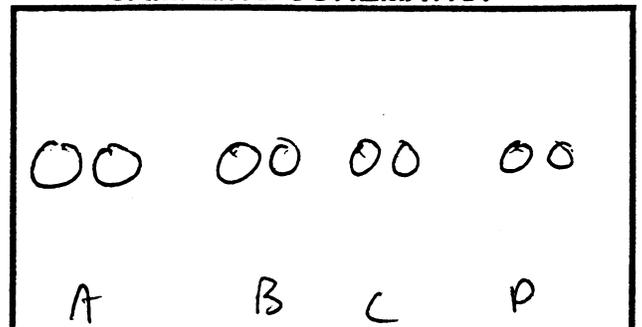
Checked By: MS DeVito

Shipped By: MSD

Received By: MSD 7-23-99

SAMPLING NOTES: 1415 to ~~1611~~ 1641

SAMPLING SCHEMATIC:



Mill Gas Temperatures  
140°F to 160°F

← Unit 5

→ Unit 7

Unit 6  
 Test 1  
 ESP Ash - Front

PROCESS STREAM SAMPLING SHEET

Sample Stream: Unit 6 ESP Ash  
Front

Plant WEPco Presque Isel

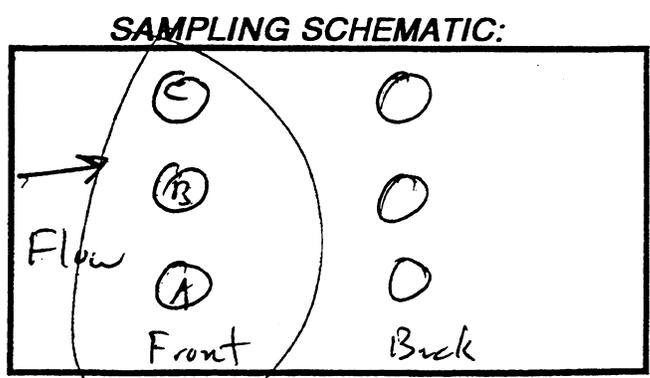
Date 7/14/97

Increment	1	2	3	4	5	6	7	8
Time	1545							
Weight / Volume								
Comp / <u>Grab</u>	3-hopper							
Process Status								
Sampler Condition								
Container Condition								
Container Label								
Sampler								
Sample Stored								
pH (if required)								
Temperature								
Preservative								

Test ID Unit 6 - Test 1  
 Sample Stream Front Field ESP Ash  
 Sample ID \_\_\_\_\_  
 Target Size \_\_\_\_\_  
 Sample Device Thief  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Glass Bottles  
 Frequency Grab  
 Safety Issues Dust  
 Protective Gear mask

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Glass Bottle  
 Checked By: MS DeWitt  
 Shipped By: MSD  
 Received By: MSD 7-23-97

SAMPLING NOTES: 1545 hrs  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_



Unit 6  
 Test 1  
 ESP Ash - Back

PROCESS STREAM SAMPLING SHEET

Plant Presque Isle

Sample Stream: Unit 6 ESP Ash Back

Date 7/14/99

Increment	1	2	3	4	5	6	7	8
Time	1540							
Weigth / Volume								
Comp // <u>Grab</u>	3-hoppers							
Process Status								
Sampler Condition								
Container Condition								
Container Label								
Sampler								
Sample Stored								
pH (if required)								
Temperature								
Preservative								

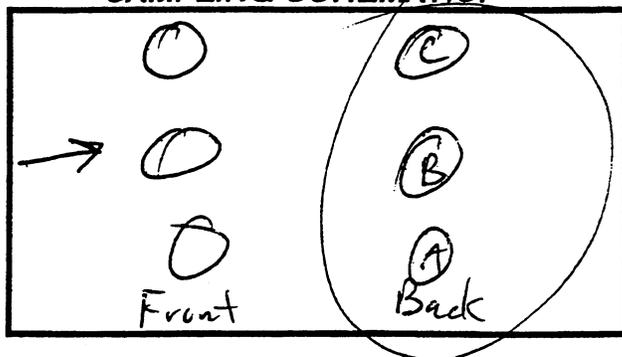
Test ID Unit 6 - Test 1  
 Sample Stream Back Field ESP Ash  
 Sample ID \_\_\_\_\_  
 Target Size \_\_\_\_\_  
 Sample Device Thief  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Glass Bottles  
 Frequency Grab  
 Safety Issues Dust  
 Protective Gear mask

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Glass Bottle  
 Checked By: M.S. DeVito  
 Shipped By: msd  
 Received By: msd 7-23-99

SAMPLING NOTES:

\_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

SAMPLING SCHEMATIC:



Unit 6  
Test 2  
Coal

PROCESS STREAM SAMPLING SHEET

Plant: Presque Isle

Sample Stream: Unit 6 Coal

Date: 7-15-99

Increment	1	2	3	4	5	6	7	8
Time	0825	0845	0905	0925	0945	1005	1025	1045
Weight / Volume	550g							
Comp / Grab								
Process Status	76	75	75	76	76	76	76	76
Sampler Condition	Clean							
Container Condition	Clean							
Container Label	Y							
Sampler	MSD							
Sample Stored	-1							
pH (if required)								
Temperature								
Preservative								
% O <sub>2</sub>	3.2				3.1			
	D-2	D-1	C-2	C-1	B-1	B-1	A-2	A-1

Test ID: Unit 6 - Test 2 - Coal  
 Sample Stream: Unit #6 COAL  
 Sample ID: Unit 6 - Test 2 - Coal  
 Target Size: 3-5K6  
 Sample Device: Mill Sampler  
 Analysis: \_\_\_\_\_  
 Preservative: \_\_\_\_\_  
 Container: Bag / Bucket  
 Frequency: 20min  
 Safety Issues: \_\_\_\_\_  
 Protective Gear: \_\_\_\_\_

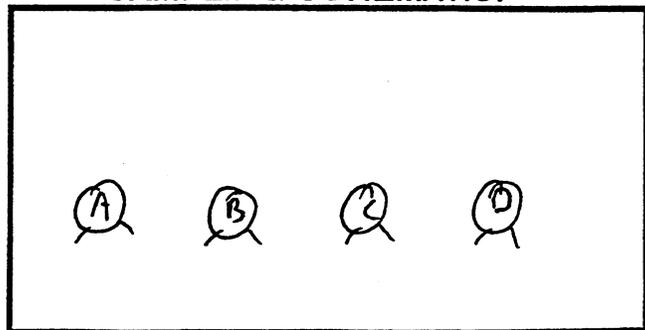
Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Bag / Bag / Bucket  
 Checked By: M. S. DeWitt  
 Shipped By: MSD  
 Received By: MSD 7-23-99

SAMPLING NOTES: 0825 to

Mill Temp - 145° to 160°

(Sandborn Creek Coal)

SAMPLING SCHEMATIC:



Unit 6  
 Test 2  
 ESP - Front

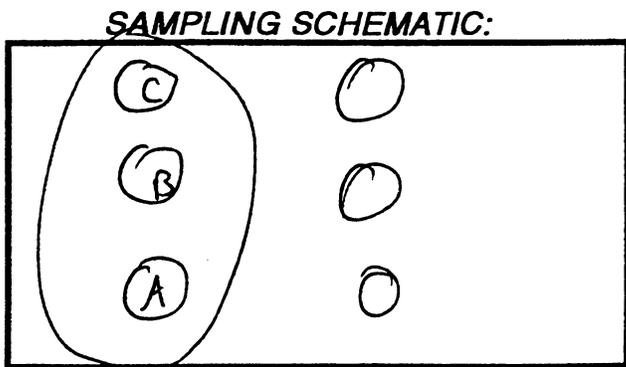
PROCESS STREAM SAMPLING SHEET

Plant Pressure Duse Sample Stream: Unit 6 - ESP Ash Date 7-15-99  
Front

Increment	1	2	3	4	5	6	7	8
Time	1010							
Weight / Volume	1 kg							
Comp / Grab								
Process Status	76 mm							
Sampler Condition	clean							
Container Condition	clean							
Container Label	Y							
Sampler	msd							
Sample Stored	Y							
pH (if required)								
Temperature								
Preservative								
	3% O <sub>2</sub>							

Test ID Unit 6 - Test 2 Composite Logged? Yes  
 Sample Stream Unit 6  
 Sample ID Unit 6 - Test 2 - ESP - Front Sample Stored? Yes  
 Target Size \_\_\_\_\_ Storage Method: Glass Bottle  
 Sample Device Thief Checked By: M.S. DeVito  
 Analysis \_\_\_\_\_ Shipped By: MSD  
 Preservative \_\_\_\_\_ Received By: msd 7-23-99  
 Container Glass Bottle  
 Frequency \_\_\_\_\_  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

SAMPLING NOTES: Ash P-11 complete  
@ 0930  
 \_\_\_\_\_  
Sampled @ 1010 hrs  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_



Unit 6  
 Test 2  
 ESP-Back

PROCESS STREAM SAMPLING SHEET

Plant Presque Isle

Sample Stream: Unit 6 ESP Ash Back

Date 7-15-99

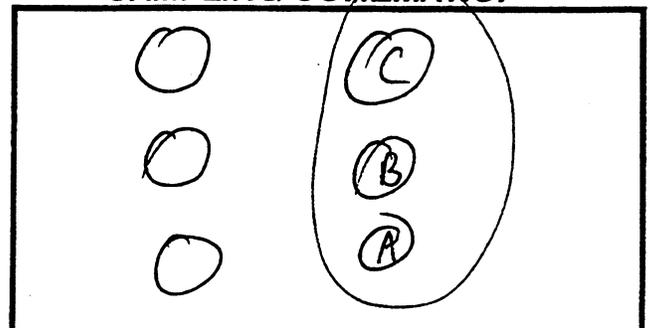
Increment	1	2	3	4	5	6	7	8
Time	1050							
Weight / Volume	1 Kg							
Comp / Grab								
Process Status	76mw							
Sampler Condition	Clean							
Container Condition	Clean							
Container Label	Y							
Sampler	MSD							
Sample Stored	Y							
pH (if required)								
Temperature								
Preservative								

Test ID Unit 6 - Test 2  
 Sample Stream Unit 6 - ESP Ash - Back  
 Sample ID Unit 6 - Test 2 - ESP - Back  
 Target Size \_\_\_\_\_  
 Sample Device Thief  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Glass Bottle  
 Frequency \_\_\_\_\_  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Glass Bottle  
 Checked By: M. S. White  
 Shipped By: MSD  
 Received By: MSD 7-23-99

SAMPLING NOTES: Ash Pull Completed @ 0930  
Sampled @ 1050 hrs

SAMPLING SCHEMATIC:



Unit 6  
Test 3  
Coal

PROCESS STREAM SAMPLING SHEET

Plant Presque Isle

Sample Stream: Unit 6 Coal

Date 7/15/99

Increment	1	2	3	4	5	6	7	8
Time	1250	1310	1330	1350	1410	1430	1450	1510
Weight / Volume	500g							
Comp / Grab								
Process Status	75	75	75	75	75	75	76	76
Sampler Condition	Clean							
Container Condition	clean							
Container Label	Y							
Sampler	MSD	MSD	MSD	MSD	MSD	MSD	MSD	MSD
Sample Stored	Y							
pH (if required)								
Temperature								
Preservative								
Bucket & Mill	A1	A2	B1	B2	C1	C2	D1	D2
% O <sub>2</sub>	3.1							

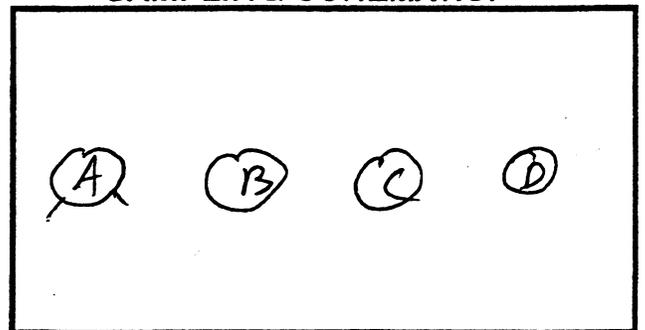
Test ID Unit 6 - Test 3  
 Sample Stream Unit 6 - Coal  
 Sample ID Unit 6 - Test 3 - Coal  
 Target Size 3-5 kg  
 Sample Device Mill Sampler  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Bag / Pallet  
 Frequency 20 min  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Bag / Bag / Pallet  
 Checked By: MSD  
 Shipped By: MSD  
 Received By: MSD - 7/23/99

SAMPLING NOTES:

Mill Temp 145-165°F  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

SAMPLING SCHEMATIC:



Unit 6  
 Test 3  
 ESP - Back

PROCESS STREAM SAMPLING SHEET

Plant Presque Isle Sample Stream: Unit 6 ESP Ash Back Date 7/15/99

Increment	1	2	3	4	5	6	7	8
Time								
Weight / Volume	1 kg							
Comp / Grab								
Process Status	<del>Grab</del>							
Sampler Condition	clean							
Container Condition	clean							
Container Label	Y							
Sampler	msd							
Sample Stored	Y							
pH (if required)								
Temperature								
Preservative								

Test ID	<u>Unit 6 Test 3</u>	Composite Logged?	<u>Yes</u>
Sample Stream	<u>Unit 6 - ESP Ash - Front</u>	Sample Stored?	<u>Yes</u>
Sample ID	<u>Unit 6 - Test 3 - ESP - Back</u>	Storage Method:	<u>Glass Bottle</u>
Target Size	_____	Checked By:	<u>msd</u>
Sample Device	<u>Thref</u>	Shipped By:	<u>msd</u>
Analysis	_____	Received By:	<u>msd 723-99</u>
Preservative	_____		
Container	<u>Glass Bottle</u>		
Frequency	<u>Grab</u>		
Safety Issues	_____		
Protective Gear	_____		

**SAMPLING NOTES:**

\_\_\_\_\_

\_\_\_\_\_

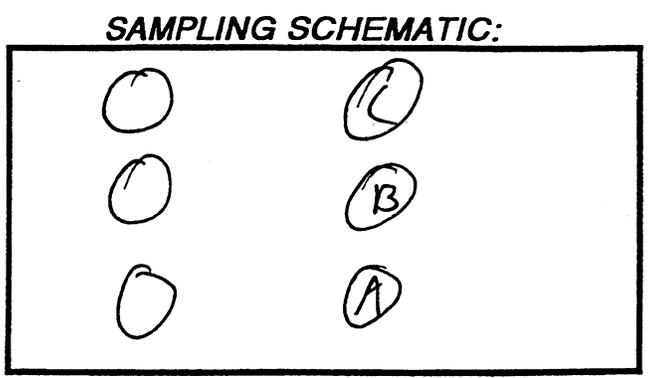
\_\_\_\_\_

\_\_\_\_\_

\_\_\_\_\_

\_\_\_\_\_

\_\_\_\_\_



Unit 6  
 Test 3  
 ESP Front

PROCESS STREAM SAMPLING SHEET

Plant Presque Isle

Sample Stream: Unit 6 - ESP Ash Front

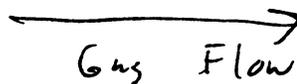
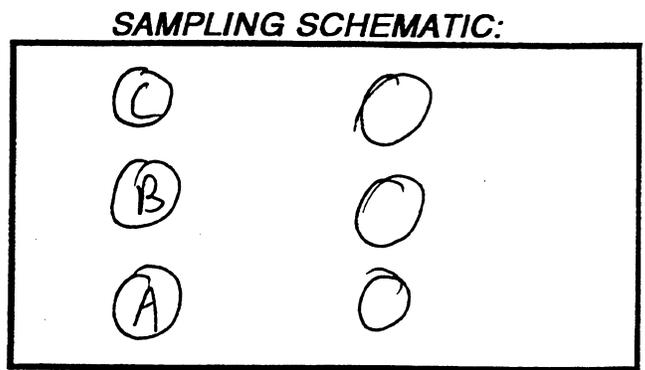
Date 7-15-99

Increment	1	2	3	4	5	6	7	8
Time	1400							
Weight / Volume	1 Kg							
Comp / Grab								
Process Status	75mc							
Sampler Condition	Clean							
Container Condition	Clean							
Container Label	Y							
Sampler	MSD							
Sample Stored	Y							
pH (if required)								
Temperature								
Preservative								

Test ID Unit 6 Test 3  
 Sample Stream Unit 6 - ESP Ash - Front  
 Sample ID Unit 6 - Test 3 - ESP - Front  
 Target Size \_\_\_\_\_  
 Sample Device Thief  
 Analysis \_\_\_\_\_  
 Preservative Glass Bottle  
 Container \_\_\_\_\_  
 Frequency Grab  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Glass Bottle  
 Checked By: MSD  
 Shipped By: MSD  
 Received By: MSD - 7/23/99

**SAMPLING NOTES:**  
Ash pulled @ 1230 hrs  
Sample @ 1400 hrs  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_



PROCESS STREAM SAMPLING SHEET

Plant Panque Isle

Sample Stream: Units 1, 2, 3, 4 Coal

Date 7/16/99

Increment	1	2	3	4	5	6	7	8
Time	0815	0840	0915	0950	1115	1200	1240	1300
Weight / Volume	500g							
Comp / Grab								
Process Status	2-3-4 Fall Lampil							
Sampler Condition	OK							
Container Condition	OK							
Container Label	✓							
Sampler	MSD	MSD	MSD	MSD	MSD	MSD	MSD	MSD
Sample Stored	✓							
pH (if required)								
Temperature								
Preservative								
Unit / mill	4-B	4-B	4-B	4A	4A	4A		

Test ID Units 1-4 Coal  
 Sample Stream Units 1-4 Coal  
 Sample ID \_\_\_\_\_  
 Target Size MSD  
 Sample Device Mill Sampler  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Bag  
 Frequency \_\_\_\_\_  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? Yes

Sample Stored? Yes

Storage Method: Bag/Bag/Bagged

Checked By: MSD

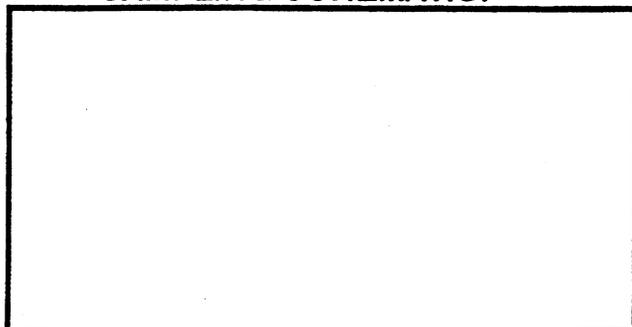
Shipped By: MSD

Received By: MSD 7/23/99

SAMPLING NOTES:

Unit 1 on Oil  
1st test started @ 0815 hrs  
Second test started @ 1115 hrs  
3rd test  
1410 to 1630  
12 splits

SAMPLING SCHEMATIC:



Coal  
Coal

### PROCESS STREAM SAMPLING SHEET

Plant Preece Isle

Sample Stream: Unit 1, 2, 3, 4  
Coal Page 2

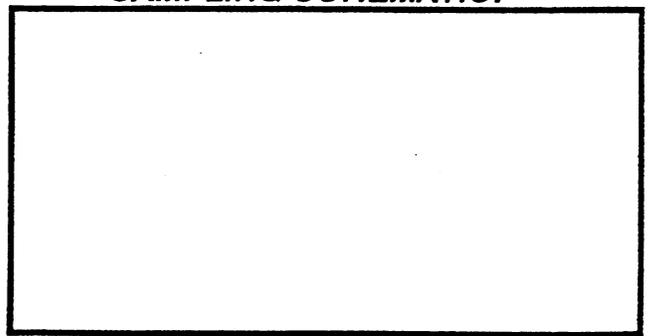
Date 7/16/99

Increment	1	2	3	4	5	6	7	8
Time	1410	1450	1330	1610				
Weight / Volume								
Comp / Grab								
Process Status								
Sampler Condition								
Container Condition								
Container Label								
Sampler	MSD	MSD	MSD	MSD				
Sample Stored								
pH (if required)								
Temperature								
Preservative								

Test ID \_\_\_\_\_  
 Sample Stream \_\_\_\_\_  
 Sample ID \_\_\_\_\_  
 Target Size \_\_\_\_\_  
 Sample Device \_\_\_\_\_  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container \_\_\_\_\_  
 Frequency \_\_\_\_\_  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? \_\_\_\_\_  
 Sample Stored? \_\_\_\_\_  
 Storage Method: \_\_\_\_\_  
 Checked By: \_\_\_\_\_  
 Shipped By: \_\_\_\_\_  
 Received By: \_\_\_\_\_

**SAMPLING NOTES:** 12 splits  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**SAMPLING SCHEMATIC:**  


Unit 1-4  
 Test 1  
 Baghouse Ash

PROCESS STREAM SAMPLING SHEET

Plant Presque Isle

Sample Stream: Baghouse Ash

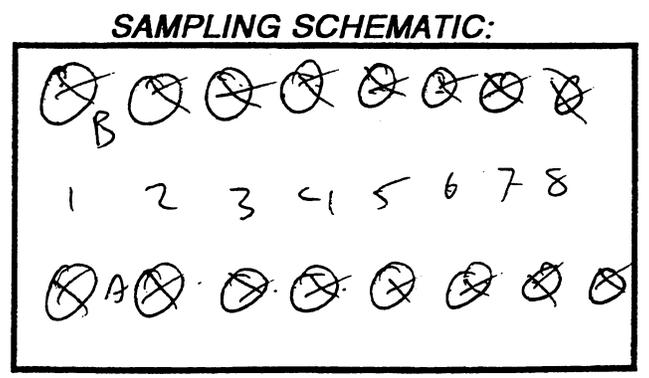
Date 7-18-99

Increment	1	2	3	4	5	6	7	8
Time	0925-0945							
Weight / Volume	1 Kg							
Comp / Grab								
Process Status								
Sampler Condition	Clean							
Container Condition	OK							
Container Label	Y							
Sampler	MSD							
Sample Stored	Y							
pH (if required)								
Temperature								
Preservative								

Test ID Units 1-4 - Test 1  
 Sample Stream Baghouse Ash - Both Units  
 Sample ID \_\_\_\_\_  
 Target Size \_\_\_\_\_  
 Sample Device Thief  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Glass bottle  
 Frequency 1/test  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Bottle/Glass  
 Checked By: MSD  
 Shipped By: MSD  
 Received By: MSD 7-23-99

SAMPLING NOTES: 0925-0945  
Thief from all hoppers!  
hopper cleaned @ 0900



Unit 1-4  
 Test 2  
 Baghouse Ash

PROCESS STREAM SAMPLING SHEET

Plant Presque Isle Sample Stream: Baghouse Ash

Date 7-16-99

Increment	1	2	3	4	5	6	7	8
Time	1240 - 1300							
Weight / Volume	1 Kg							
Comp/ Grab								
Process Status								
Sampler Condition	Clean							
Container Condition	Clean							
Container Label	✓							
Sampler	MSD							
Sample Stored	✓							
pH (if required)								
Temperature								
Preservative								

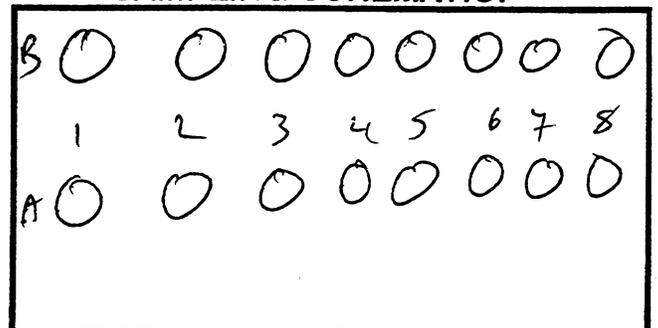
Test ID Units 1-4 Test 2  
 Sample Stream Baghouse Ash - Both units  
 Sample ID \_\_\_\_\_  
 Target Size \_\_\_\_\_  
 Sample Device Thief  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Glass Bottle  
 Frequency 1 per Test  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Yes 5L, Both  
 Checked By: MSD  
 Shipped By: MSD  
 Received By: MSD 7-23-99

SAMPLING NOTES:

Sample from every hopper 1240-1300  
Hoppers cleaned @ 1100

SAMPLING SCHEMATIC:



Unit 1-4  
 Test 3  
 Bayhouse

PROCESS STREAM SAMPLING SHEET

Plant Process Islp

Sample Stream: Bayhouse Ash

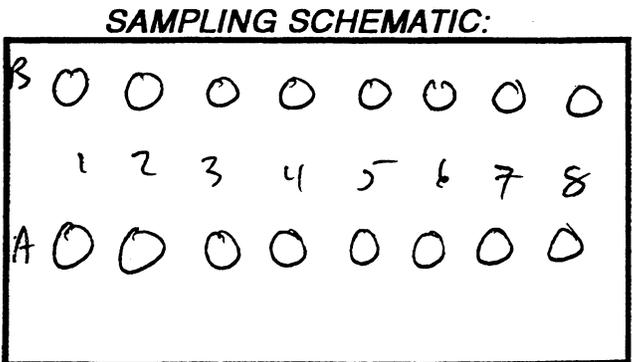
Date 7-16-99

Increment	1	2	3	4	5	6	7	8
Time	1500	1540						
Weight / Volume								
Comp / Grab								
Process Status								
Sampler Condition								
Container Condition								
Container Label								
Sampler								
Sample Stored								
pH (if required)								
Temperature								
Preservative								

Test ID Units 1-4 - Test 3  
 Sample Stream Bayhouse Ash - Both Units  
 Sample ID \_\_\_\_\_  
 Target Size \_\_\_\_\_  
 Sample Device Thick  
 Analysis \_\_\_\_\_  
 Preservative \_\_\_\_\_  
 Container Glass Bottle  
 Frequency 1/Test  
 Safety Issues \_\_\_\_\_  
 Protective Gear \_\_\_\_\_

Composite Logged? Yes  
 Sample Stored? Yes  
 Storage Method: Glass Bottle  
 Checked By: M.S. DeWitt  
 Shipped By: MSD  
 Received By: MSD - 7-23-99

SAMPLING NOTES:  
 \_\_\_\_\_  
Sample from every hopper  
1500 - 1540 hrs.  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_



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## PROCESS SOLID SAMPLES QA/QC SUMMARY

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## **QA/QC Text for Coal and Ash Samples Analyzed by CONSOL Inc.**

All process stream samples were analyzed by CONSOL following carefully written sampling and analytical procedures. These procedures are reviewed periodically to maintain consistency with industry standards and practices. Professional staff members take an active part in the development and testing of the ASTM methods used in this program. The individual determinations were completed by experienced staff personnel who were specifically trained in the individual analytical procedures. Analyst performance and data quality are monitored using quality control samples, certified standards, blind samples and duplicate samples. For this program, duplicate analysis was performed on every sample. The CONSOL R&D Laboratory participates in a variety of external auditing programs specific to coal analyses. Two of these programs specific to these samples are the EPRI-sponsored mercury-in-coal-analysis round robin study and the Standard Laboratories Inc., "Interlab" round robin program. A summary of the performance indicators used to assess data quality for this program are discussed as follows.

### **Quality Control Check Samples**

The CONSOL R&D lab utilized a number of quality control check samples (QCCS) for this program. Accuracy is determined from the percent difference in the measured value from the QCCS reference value. The specific samples and the results obtained from the analysis of these samples used to assess the quality of the coal analysis are shown Table 1. Similar data for the ash samples are presented in Table 3.

### **Analytical Precision**

All process stream samples were analyzed in duplicate. Analytical precision was determined by the percent difference in the duplicate sample analysis. The percent relative difference (PRD) obtained in for the sample analyses completed in this program are summarized in Table 2 (coal samples) and Table 4 (ash samples).

### **Summary of Analytical Performance**

A summary of the QC checks and relative percent differences are as follows:

Parameter	Coal Samples		ESP Ash Samples	
	Accuracy	PRD	Accuracy	PRD
Ult./Prox.	98% - 102%	0% - 2%	—	—
Carbon	—	—	98% - 102%	1%
Ash	—	—	98% - 102%	<1%
Sulfur	98% - 102%	2%	98% - 102%	2%
Btu	100%	0.1%	—	—
Ash Elements	94% - 107%	1% - 4%	96% - 105%	2% - 6%

Mercury	105% - 109%	10%	88% - 92%	6%
Chlorine	92% - 96%	6%	—	—

The analytical accuracy for both the coal and ash samples were  $100 \pm 10\%$ . This is well within the data quality objectives. The relative percent differences, as an indication of analytical precision were  $\leq 10\%$ . Again, this is within the data quality objective. The coal mercury analysis showed the greatest PRD at 10%. This is a result of the extremely low mercury concentration in the coal samples which for this test ranged from 0.04 to 0.06 ppm. A precision of 10% is excellent for this low level.

**Table 1. QCCS Summary for Coal Analysis**  
(units are % unless noted)

Parameter	QC Sample	QCCS Value	# of Checks	Avg Result	% Recovery
Moisture	Coal	1.08	1	1.06	98.0
Carbon	EDTA	41.10	4	40.81	99.3
Hydrogen	EDTA	5.52	4	5.54	100.3
Nitrogen	EDTA	9.59	4	9.78	102.0
Ash	Coal	6.01	1	5.92	98.5
Volatile Matter	Coal	38.05	1	37.82	99.4
Sulfur	NIST 2692A	1.16	2	1.16	100.0
Cl, ppm	NIST 1630a	1143	1	1078	94.3
Hg, ppm	BCR 181	0.138	2	0.148	107.2
Btu	Benzoic Acid	1136	1	11356	99.9
SiO <sub>2</sub>	NIST 1633a	48.78	2	49.20	100.9
Al <sub>2</sub> O <sub>3</sub>	NIST 1633a	27.02	2	26.70	98.8
TiO <sub>2</sub>	NIST 1633a	1.33	2	1.33	100.0
Fe <sub>2</sub> O <sub>3</sub>	NIST 1633a	13.44	2	13.50	100.4
CaO	NIST 1633a	1.55	2	1.58	101.9
MgO	NIST 1633a	0.75	2	0.74	98.7

Na <sub>2</sub> O	NIST 1633a	0.22	2	0.23	104.5
K <sub>2</sub> O	NIST 1633a	2.26	2	2.25	99.6
P <sub>2</sub> O <sub>5</sub>	NIST 1633a	0.44	2	0.44	100.0
SO <sub>3</sub>	NIST 1633a	0.37	2	0.31	83.8

**Table 2. Precision Summary for Coal Analysis**

Parameter	No. of Pairs	Average PRD
Moisture	4	1.2
Carbon	4	0.5
Hydrogen	4	0.5
Nitrogen	4	0.5
Ash	4	0.5
Volatile Matter	4	0.7
Sulfur	4	0.5
Cl, ppm	4	8.9
Hg, ppm	4	11.3
Btu	4	0.2
SiO <sub>2</sub>	4	0.8
Al <sub>2</sub> O <sub>3</sub>	4	1.0
TiO <sub>2</sub>	4	2.5
Fe <sub>2</sub> O <sub>3</sub>	4	2.0
CaO	4	1.2
MgO	4	0.7
Na <sub>2</sub> O	4	1.3
K <sub>2</sub> O	4	0.8
P <sub>2</sub> O <sub>5</sub>	4	1.1
SO <sub>3</sub>	4	0.7

**Table 3. QCCS Summary for Ash Analysis**  
(units are % unless noted)

Parameter	QC Sample	QCCS Value	# of Checks	Avg Result	% Recovery
Moisture	Coal	1.08	2	1.04	96.3
Carbon	EDTA	41.10	2	41.13	100.1
Ash	Coal	6.01	2	6.12	102.0
Sulfur	Ash	1.96	4	1.94	99.0
Hg, ppm	BCR 181	0.138	1	0.124	89.9
SiO <sub>2</sub>	NIST 1633a	48.78	2	49.40	101.3
Al <sub>2</sub> O <sub>3</sub>	NIST 1633a	27.02	2	26.84	99.3
TiO <sub>2</sub>	NIST 1633a	1.33	2	1.32	99.2
Fe <sub>2</sub> O <sub>3</sub>	NIST 1633a	13.44	2	13.41	99.8
CaO	NIST 1633a	1.55	2	1.55	100.0
MgO	NIST 1633a	0.75	2	0.75	100.0
Na <sub>2</sub> O	NIST 1633a	0.22	2	0.23	104.5
K <sub>2</sub> O	NIST 1633a	2.26	2	2.28	100.9
P <sub>2</sub> O <sub>5</sub>	NIST 1633a	0.44	2	0.42	95.5
SO <sub>3</sub>	NIST 1633a	0.37	2	0.33	89.2

**Table 4. Precision Summary for Ash Analysis**

<b>Parameter</b>	<b>No. of Pairs</b>	<b>Average PRD</b>
Carbon	9	0.6
Ash	9	0.2
Sulfur	9	1.4
Hg, ppm	9	6.9
SiO <sub>2</sub>	6	1.0
Al <sub>2</sub> O <sub>3</sub>	6	1.1
TiO <sub>2</sub>	6	2.3
Fe <sub>2</sub> O <sub>3</sub>	6	1.6
CaO	6	0.8
MgO	6	1.3
Na <sub>2</sub> O	6	1.1
K <sub>2</sub> O	6	1.9
P <sub>2</sub> O <sub>5</sub>	6	2.1
SO <sub>3</sub>	6	3.5

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## ONTARIO HYDRO SAMPLES ANALYTICAL REPORT

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### Mercury in Ash Collecting in the Sampling Train Thimbles at Presque Isle

Sample Code Code	Sample ID ID	Measured Hg	Total Hg µg	Total Ash g
49863-07	DOE-BO6 IN-1	0.256	4.341	16.95539
49863-08	DOE-BO6 OUT-1 (total ug)	0.100	0.100	
49863-09	DOE-BO6 IN-2	0.258	4.983	19.31361
49863-10	DOE-BO6 OUT-2 (total ug)	0.051	0.051	
49863-11	DOE-BO6 IN-3	0.279	5.013	17.96909
49863-12	DOE-BO6 OUT-3 (total ug)	<0.002	< 0.002	

MERCURY ANALYSIS					
DATE:	7/14/99				
LOCATION:	PRESQUE ISLE POWER PLANT				
LAB #	SAMPLE ID	SAMPLE TYPE	VOLUME, ml	CONCENTRATION, ug/L	
71399-22	10% HNO3 BLANK	10% HNO3	100	<0.03	
71399-23	KCL BLANK	KCL	100	<0.03	
71399-24	H2O2 BLANK	H2O2	100	<0.03	
71399-25	KMNO4 BLANK	KMNO4	100	<0.03	

MERCURY ANALYSIS						
DATE:	7/15/99					
LOCATION:	PRESQUE ISLE POWER PLANT					
LAB #	SAMPLE ID	SAMPLE TYPE	VOLUME, ml	CONCENTRATION, ug/L		
71499-16	BO6-IN-1-FHHNO3	0.1 N HNO3	250	<0.03		
71499-17	BO6-IN-1-PFHNO3	0.1 N HNO3	250	<0.03		
71499-18	BO6-IN-1-BHKCL	KCL	500	2		
71499-19	BO6-IN-1-BHHNO3	H2O2	250	<0.03		
71499-20	BO6-IN-1-BHKMNO4	KMnO4	500	0.54		
71499-21	BO6-OUT-1-FHHNO3	0.1 N HNO3	250	<0.03		
71499-22	BO6-OUT-1-PFHNO3	0.1 N HNO3	200	<0.03		
71499-23	BO6-OUT-1-BHKCL	KCL	500	2.86		
71499-24	BO6-OUT-1-BHHNO3	H2O2	250	<0.03		
71499-25	BO6-OUT-1-BHKMNO4	KMnO4	500	2.36		
71499-26	BO6-FBSPK-KCL	KCL	500	2.24		
71499-27	BO6-FBSPK-HNO3	H2O2	250	1.89		
71499-28	BO6-FBSPK-KMNO4	KMnO4	500	1.83		

		MERCURY ANALYSIS				
DATE:		7/16/99				
LOCATION:		PRESQUE ISLE POWER PLANT				
LAB #	SAMPLE ID	SAMPLE TYPE	VOLUME, ml	CONCENTRATION, ug/L		
71599-1	BO6-IN-2-FHHNO3	0.1 N HNO3	250	<0.03		
71599-2	BO6-IN-2-PFHNO3	0.1 N HNO3	250	<0.03		
71599-3	BO6-IN-2-BHKCL	KCL	500	2.42		
71599-4	BO6-IN-2-BHHNO3	H2O2	250	<0.03		
71599-5	BO6-IN-2-BHKMNO4	KMnO4	500	0.83		
71599-6	BO6-OUT-2-FHHNO3	0.1 N HNO3	250	<0.03		
71599-7	BO6-OUT-2-PFHNO3	0.1 N HNO3	100	<0.03		
71599-8	BO6-OUT-2-BHKCL	KCL	500	3.95		
71599-9	BO6-OUT-2-BHHNO3	H2O2	250	<0.03		
71599-10	BO6-OUT-2-BHKMNO4	KMnO4	500	3.63		
71599-11	BO6-IN-BT-FHHNO3	0.1 N HNO3	100	<0.03		
71599-12	BO6-IN-BT-PFHNO3	0.1 N HNO3	200	<0.03		
71599-13	BO6-IN-BT-BHKCL	KCL	500	<0.03		
71599-14	BO6-IN-BT-BHHNO3	H2O2	250	<0.03		
71599-15	BO6-IN-BT-BHKMNO4	KMnO4	500	<0.03		
71599-16	BO6-OUT-BT-FHHNO3	0.1 N HNO3	100	<0.03		
71599-17	BO6-OUT-BT-PFHNO3	0.1 N HNO3	200	<0.03		
71599-18	BO6-OUT-BT-BHKCL	KCL	500	<0.03		
71599-19	BO6-OUT-BT-BHHNO3	H2O2	250	<0.03		
71599-20	BO6-OUT-BT-BHKMNO4	KMnO4	500	<0.03		
71599-21	BO6-IN-3-FHHNO3	0.1 N HNO3	250	<0.03		
71599-22	BO6-IN-3-PFHNO3	0.1 N HNO3	200	<0.03		
71599-23	BO6-IN-3-BHKCL	KCL	500	2.07		
71599-24	BO6-IN-3-BHHNO3	H2O2	250	<0.03		
71599-25	BO6-IN-3-BHKMNO4	KMnO4	500	0.59		
71599-26	BO6-OUT-3-FHHNO3	0.1 N HNO3	250	<0.03		
71599-27	BO6-OUT-3-PFHNO3	0.1 N HNO3	100	<0.03		
71599-28	BO6-OUT-3-BHKCL	KCL	500	2.76		
71599-29	BO6-OUT-3-BHHNO3	H2O2	250	<0.03		
71599-30	BO6-OUT-3-BHKMNO4	KMnO4	500	3.06		
71599-31	BO6-FBSPK-15JUL1999-KCL	KCL	500	2.21		
71599-32	BO6-FBSPK-15JUL1999-HNO3	H2O2	250	1.64		
71599-33	BO6-FBSPK-15JUL1999-KMNO4	KMnO4	500	1.99		

MERCURY ANALYSIS					
DATE:	7/17/99				
LOCATION:	PRESQUE ISLE POWER PLANT				
	UNIT 1-4 STACK SAMPLES				
LAB #	SAMPLE ID	SAMPLE TYPE	VOLUME. ml	CONCENTRATION. ug/L	
71699-1	RUN #1	0.1 N HNO3	200	<0.03	
71699-2	RUN #1	0.1 N HNO3	200	<0.03	
71699-3	RUN #1	KCL	500	0.97	
71699-4	RUN #1	H2O2	250	<0.03	
71699-5	RUN #1	KMnO4	500	0.17	
71699-6	RUN #2	0.1 N HNO3	200	<0.03	
71699-7	RUN #2	0.1 N HNO3	200	<0.03	
71699-8	RUN #2	KCL	500	0.52	
71699-9	RUN #2	H2O2	250	<0.03	
71699-10	RUN #2	KMnO4	500	0.31	
71699-11	RUN #3	0.1 N HNO3	200	<0.03	
71699-12	RUN #3	0.1 N HNO3	200	<0.03	
71699-13	RUN #3	KCL	500	0.65	
71699-14	RUN #3	H2O2	250	<0.03	
71699-15	RUN #3	KMnO4	500	0.04	

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## ONTARIO HYDRO SAMPLES QA/QC SUMMARY

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LOCATION: PRESQUE ISLE POWER PLANT				
UNIT 1-4 STACK SAMPLES TRIPLICATE ANALYSIS AND LAB SPIKE DATA				
<b>TRIPLICATE ANALYSIS</b>				
	<b>TRIAL #</b>			
<u>SAMPLE ID</u>	<u>1</u>	<u>2</u>	<u>3</u>	<u>S.D.</u>
KCL	0.99	0.95	0.96	0.0208
KMNO4	0.316	0.312	0.309	0.0035
<b>LAB SPIKE RESULTS</b>				
Calibration Standards:			0, 1, 5, 10, 20 ppb	R=0.9999
<u>SAMPLE ID</u>	<u>SPIKE</u>	<u>SAMPLE</u>	<u>SPIKE</u>	<u>SPIKE</u>
	<u>AMOUNT (ppb)</u>	<u>READING(ug/L)</u>	<u>READING(ug/L)</u>	<u>RECOVERY%</u>
KCL	5	0.97	5.92	99.00
KCL	10	0.97	11.18	102.10
KMNO4	5	0.31	5.06	95.00
KMNO4	10	0.31	10.09	97.80
<b>FIELD BLANKS</b>				
	<u>SAMPLE</u>	<u>SAMPLE</u>		
<u>SAMPLE ID</u>	<u>VOLUME (ml)</u>	<u>READING(ug/L)</u>		
10% HNO3	100	<0.03		
KCL	100	<0.03		
H2O2	100	<0.03		
KMNO4	100	<0.03		



DATE:	7/15/99	SAMPLE ID		SAMPLE TYPE	SPIKE AMOUNT (ppb)	SAMPLE READING(ug/L)	SPIKE READING(ug/L)	SPIKE LOCATION	SPIKE RECOVERY%
Calibration Standards:		0, 1, 5, 10, 20 ppb					R=0.9999	QC=4.08(4)	
71499-26	BO6-FBSPK-KCL	KCI	2	0	2.24			FIELD	112.00
71499-26	BO6-FBSPK-KCL	KCI	5	2.24	7.9			LAB	113.20
71499-3	BO5-IN-3-BHKCL	KCI	5	1.57	7.08			LAB	110.20
71499-3	BO5-IN-3-BHKCL	KCI	10	1.57	12.29			LAB	107.20
71499-27	B06-FBSPK-HNO3	H2O2	2	0	1.89			FIELD	94.50
71499-27	B06-FBSPK-HNO3	H2O2	5	1.89	7.34			LAB	109.00
71499-27	B06-FBSPK-HNO3	H2O2	10	1.89	12.76			LAB	108.70
DATE:	7/16/99								



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**APPENDIX E**  
**SAMPLE CALCULATIONS**

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## SAMPLE CALCULATIONS FOR FLOW, MOISTURE AND ISO

Client: DOE  
Test Number: Run 1  
Test Location: Unit 6 Inlet

Plant: Presque Isle  
Test Date: 7/14/99  
Test Period: 1415-1640

### 1. Volume of dry gas sampled at standard conditions (68 deg F, 29.92 in. Hg), dscf.

$$Vm(std) = \frac{17.64 \times Y \times Vm \times \left( Pb + \frac{\text{delta H}}{13.6} \right)}{(Tm + 460)}$$

$$Vm(std) = \frac{17.64 \times 1.0090 \times 68.275 \times \left( 29.47 + \frac{1.015}{13.6} \right)}{112.50 + 460} = 62.713$$

Where:

$Vm(std)$  = Volume of gas sample measured by the dry gas meter, corrected to standard conditions, dscf.  
 $Vm$  = Volume of gas sample measured by the dry gas meter at meter conditions, dcf.  
 $Pb$  = Barometric Pressure, in Hg.  
 $\text{delt H}$  = Average pressure drop across the orifice meter, in H<sub>2</sub>O  
 $Tm$  = Average dry gas meter temperature, deg F.  
 $Y$  = Dry gas meter calibration factor.  
 $17.64$  = Factor that includes ratio of standard temperature (528 deg R) to standard pressure (29.92 in. Hg), deg R/in. Hg.  
 $13.6$  = Specific gravity of mercury.

**2. Volume of water vapor in the gas sample corrected to standard conditions, scf.**

$$Vw(std) = (0.04707 \times Vwc) + (0.04715 \times Wwsg)$$

$$Vw(std) = (0.04707 \times 136.6) + (0.04715 \times 13.3) = 7.1$$

Where:

$Vw(std)$  = Volume of water vapor in the gas sample corrected to standard conditions, scf.

$Vwc$  = Volume of liquid condensed in impingers, ml.

$Wwsg$  = Weight of water vapor collected in silica gel, g.

$0.04707$  = Factor which includes the density of water (0.002201 lb/ml), the molecular weight of water (18.0 lb/lb-mole), the ideal gas constant 21.85 (in. Hg) (ft<sup>3</sup>/lb-mole)(deg R); absolute temperature at standard conditions (528 deg R), absolute pressure at standard conditions (29.92 in. Hg), ft<sup>3</sup>/ml.

$0.04715$  = Factor which includes the molecular weight of water (18.0 lb/lb-mole), the ideal gas constant 21.85 (in. Hg) (ft<sup>3</sup>/lb-mole)(deg R); absolute temperature at standard conditions (528 deg R), absolute pressure at standard conditions (29.92 in. Hg), and 453.6 g/lb, ft<sup>3</sup>/g.

**3. Moisture content**

$$bws = \frac{Vw(std)}{Vw(std) + Vm(std)}$$

$$bws = \frac{7.057}{7.057 + 62.713} = 0.101$$

Where:

$bws$  = Proportion of water vapor, by volume, in the gas stream, dimensionless.

**4. Mole fraction of dry gas.**

$$Md = 1 - bws$$

$$Md = 1 - 0.101 = 0.899$$

Where:

$$Md = \text{Mole fraction of dry gas, dimensionless.}$$

**5. Dry molecular weight of gas stream, lb/lb-mole.**

$$MWd = (0.440 \times \% CO_2) + (0.320 \times \% O_2) + (0.280 \times (\% N_2 + \% CO))$$

$$MWd = (0.440 \times 13.7) + (0.320 \times 4.9) + (0.280 \times (81.4 + 0.00))$$

$$= 30.39$$

Where:

$$MWd = \text{Dry molecular weight, lb/lb-mole.}$$

$$\% CO_2 = \text{Percent carbon dioxide by volume, dry basis.}$$

$$\% O_2 = \text{Percent oxygen by volume, dry basis.}$$

$$\% N_2 = \text{Percent nitrogen by volume, dry basis.}$$

$$\% CO = \text{Percent carbon monoxide by volume, dry basis.}$$

$$0.440 = \text{Molecular weight of carbon dioxide, divided by 100.}$$

$$0.320 = \text{Molecular weight of oxygen, divided by 100.}$$

$$0.280 = \text{Molecular weight of nitrogen or carbon monoxide, divided by 100.}$$

**6. Actual molecular weight of gas stream (wet basis), lb/lb-mole.**

$$MWs = (MWd \times Md) + (18 \times (1 - Md))$$

$$MWs = (30.39 \times 0.899) + (18 \times (1 - 0.899)) = 29.14$$

Where:

$$MWs = \text{Molecular weight of wet gas, lb/lb-mole.}$$

$$18 = \text{Molecular weight of water, lb/lb-mole.}$$

**7. Average velocity of gas stream at actual conditions, ft/sec.**

$$V_s = 85.49 \times C_p \times ((\Delta p)^{1/2})_{avg} \times \left( \frac{T_s (avg)}{P_s \times MW_s} \right)^{1/2}$$

$$V_s = 85.49 \times 0.84 \times 0.587660 \times \left( \frac{769}{28.85 \times 29.14} \right)^{1/2} = 40.4$$

Where:

$V_s$  = Average gas stream velocity, ft/sec.

85.49 = Pitot tube constant, ft/sec  $\times \frac{(lb/lb-mole)(in. Hg)^{1/2}}{(deg R)(in H_2O)}$

$C_p$  = Pitot tube coefficient, dimensionless.

$T_s$  = Absolute gas stream temperature, deg R =  $T_s, deg F + 460.$

$P_s$  = Absolute gas stack pressure, in. Hg. =  $P_b + \frac{P(static)}{13.6}$

$\Delta p$  = Velocity head of stack, in.  $H_2O$

**8. Average gas stream volumetric flowrate at actual conditions, wacf/min.**

$$Q_s(act) = 60 \times V_s \times A_s$$

$$Q_s(act) = 60 \times 40.37 \times 151.96 = 368086$$

Where:

$Q_s(act)$  = Volumetric flowrate of wet stack gas at actual conditions, wacf/min.

$A_s$  = Cross-sectional area of stack,  $ft^2$ .

60 = Conversion factor from seconds to minutes.

**9. Average gas stream dry volumetric flowrate at standard conditions, dscf/min.**

$$Qs(std) = 17.64 \times Md \times \frac{Ps}{Ts} \times Qs(act)$$

$$Qs(std) = 17.64 \times 0.899 \times \frac{28.85}{769} \times 368086$$

$$= 218890$$

Where:

Qs(std) = Volumetric flowrate of dry stack gas at standard conditions, dscf/min.

Note: Volumetric flowrate from the unit 5 outlet (corrected to the Unit 5 inlet O<sub>2</sub> concentration) was used in the emission rate calculations. That value is 182,746 dscfm.

**10. Isokinetic variation calculated from intermediate values, percent.**

$$I = \frac{17.327 \times Ts \times Vm(std)}{Vs \times O \times Ps \times Md \times (Dn)^2}$$

$$I = \frac{17.327 \times 769 \times 62.713}{40.37 \times 120 \times 28.85 \times 0.899 \times (0.253)^2} = 103.9$$

Where:

I = Percent of isokinetic sampling.  
 O = Total sampling time, minutes.  
 Dn = Diameter of nozzle, inches.  
 17.327 = Factor which includes standard temperature (528 deg R), standard pressure (29.92 in. Hg), the formula for calculating area of circle  $D^{2/4}$ , conversion of square feet to square inches (144), conversion of seconds to minutes (60), and conversion to percent (100),  
 $\frac{(in. Hg)(in^2)(min)}{(deg R)(ft^2)(sec)}$

## SAMPLE CALCULATIONS FOR MERCURY

Client: DOE  
Test Number: Run 1  
Test Location: Unit 6 Inlet

Plant: Presque Isle  
Test Date: 7/14/99  
Test Period: 1415-1640

### 1. Total Mercury concentration, lb/dscf.

$$C_1 = \frac{W \times 2.2046 \times 10E-9}{Vm_{(std)}}$$

$$C_1 = \frac{5.61 \times 2.2046 \times 10E-9}{62.713}$$

$$= 1.97E-10$$

Where:

W = Weight of Total Mercury collected in sample in ug.  
C<sub>1</sub> = Total Mercury concentration, lb/dscf.  
2.2046x10<sup>-9</sup> = Conversion factor from ug to pounds.

### 2. Total Mercury concentration, ug/dscm

$$C_2 = \frac{W}{Vm_{(std)} \times 0.02832}$$

$$C_2 = \frac{5.611}{62.713 \times 0.02832}$$

$$= 3.16$$

Where:

C<sub>2</sub> = Total Mercury concentration, μg/dscm.  
W = Total Mercury catch, μg.  
0.02832 = Conversion factor from cubic feet to cubic meters.

### 3. Total Mercury concentration, ug/Nm<sup>3</sup>

$$C_3 = \frac{W}{V_{m(\text{std})} \times 0.02832 \times (16.44/17.64)}$$
$$C_3 = \frac{5.611}{1.66}$$
$$C_3 = 3.39$$

Where:

$C_3$  = Total Mercury concentration, ug/Nm<sup>3</sup>  
 $W$  = Total Mercury catch,  $\mu\text{g}$ .  
0.02832 = Conversion factor from cubic feet to cubic meters.  
16.44/17.64 = Ratio of conversion factors for standard temperature and pressure and normal temperature.

### 4. Total Mercury mass emission rate, lbs/hr.

$$\text{MR1} = C_1 \times Q_s(\text{std}) \times 60$$
$$\text{MR1} = 1.97\text{E-}10 \times 163300 \times 60$$
$$\text{MR1} = 1.93\text{E-}03$$

Where:

$\text{MR1}$  = Total Mercury mass emission rate, lbs/hr.  
60 = Conversion factor from minutes to hours.

### 5. Total Mercury mass emission rate, lbs/10E+12 Btu.

$$\text{MR2} = \text{MR1}/\text{F-Factor} \times 10\text{E}+6$$
$$\text{MR2} = 1.93\text{E-}03 / 761 \times 10\text{E}+6$$
$$\text{MR2} = 2.54$$

Where:

$\text{MR2}$  = Total Mercury mass emission rate, lbs/10E+12 Btu.  
Heat Input = 761.3 x 10E+6 Btu/hr

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**APPENDIX F**  
**EQUIPMENT CALIBRATION RECORDS**

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LONG/PRE DRY GAS METER CALIBRATION DATA FORM

Calibrator P. Mack  
 Date 3/22/99  
 Barometric pressure,  $P_b = 29.33$

Meter Box Number 66 Plant \_\_\_\_\_  
 in. Hg Dry Gas Meter Number 9429 Comments \_\_\_\_\_

Setting	Gas volume			Temperatures			Time (t), min	$Y_1$	$\Delta H @ 1 \text{ in. H}_2\text{O}$
	Wet test meter	Dry gas meter	( $V_1$ ) ft <sup>3</sup>	Wet test meter	Inlet (td) °F	Outlet (td) °F			
0.5	5		658.876 678.870	64	74.77	74.75	12.6	.9927	1.7613
1.0	5		680.127 684.936	64	78.81	76.77	9.1	.9961	1.5271
1.5	10		700.434 690.127	64	81.88	77.80	15.5	.9940	1.97850
2.0	10		710.441 702.984	64	83.92	80.83	13.5	.9915	1.9811
3.0	10		721.401 702.941	64	93.97	83.86	11.1	.9960	1.99994
							AVG	.9991	1.9078

If there is only one thermometer on the dry gas meter, record the temperature under td.

( $\Delta H$ ) in. H <sub>2</sub> O	$\frac{\Delta H}{13.6}$	$Y_1 = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H @ 1 = \frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[ \frac{(t_w + 460) \Theta}{V_w} \right]^2$
0.5	0.0368	(65) (29.33) (75 + 460) (5.136) (29.33 + 0.368) (64 + 460)	(.0317) (.5) (64 + 460) (12.6) <sup>2</sup> (29.33) (75 + 460) 5
1.0	0.0735	(5) (29.33) (78 + 460) (5.14) (29.33 + 0.735) (64 + 460)	(.0317) (1.0) (64 + 460) (9.1) <sup>2</sup> (29.33) (78 + 460) 5
1.5	0.110	(10) (29.33) (81.88 + 460) (10.357) (29.33 + 1.10) (64 + 460)	(.0317) (1.5) (64 + 460) (15.5) <sup>2</sup> (29.33) (81.5 + 460) 10
2.0	0.147	(10) (29.33) (83.92 + 460) (10.457) (29.33 + 1.47) (64 + 460)	(.0317) (2.0) (64 + 460) (13.5) <sup>2</sup> (29.33) (86 + 460) 10
3.0	0.221	(10) (29.33) (93.97 + 460) (10.96) (29.33 + 2.21) (64 + 460)	(.0317) (3.0) (64 + 460) (11.1) <sup>2</sup> (29.33) (90 + 460) 10



### STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

DATE <u>3/09/99</u>	POTENTIOMETER NUMBER <u>2010 26</u>
AMBIENT TEMPERATURE <u>76</u>	BAROMETRIC PRESSURE <u>29.33</u>
CALIBRATION <u>W.C. Pitts</u>	REFERENCE: THERMOCOUPLE SIMULATOR (ACCURACY: 1°F)

REFERENCE TEMPERATURE		TEMPERATURE READING FROM THERMOCOUPLE CHANNEL INPUT NUMBER					AVERAGE TEMPERATURE READING °C	TEMPERATURE DIFFERENCE °C (%)
		1	2	3	4	5		
°C	°F							
0	32	32	32	32	32	32	32	0% - 0%
100	212	213	213	213	213	213	213	1% - 15%
500	932	933	933	933	933	933	933	1% - 107%
1000	1832	1831	1831	1831	1831	1831	1831	1% - .04

**COMMENTS**

⊙ AVERAGE TEMPERATURE READING = MEAN OF THE TEMPERATURE READINGS FOR THE THERMOCOUPLE CHANNELS

⊙ THE CHANNEL READINGS MUST AGREE WITHIN ± 5°F OR 3°C

ACCEPTABLE TEMPERATURE DIFFERENCE ± 1.5 =  $\left( \frac{(\text{REF TEMP}^{\circ}\text{F} + 460) \cdot (\text{TEST TEMP}^{\circ}\text{F} + 460)}{(\text{REF TEMP}^{\circ}\text{F} + 460)} \right) \times 100$



STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

DATE 7/24/89  
AMBIENT TEMPERATURE 77  
CALIBRATION OK

POTENTIOMETER NUMBER 2010 #6  
BAROMETRIC PRESSURE 29.27  
REFERENCE: THERMOCOUPLE SIMULATOR  
(ACCURACY: ±1°F)

REFERENCE TEMPERATURE °C      °F		TEMPERATURE READING FROM THERMOCOUPLE CHANNEL INPUT NUMBER					AVERAGE TEMPERATURE READING °	TEMPERATURE DIFFERENCE (%)
		1	2	3	4	5		
0	32	33	33	33	33	33	33	1° - .20%
100	212	214	214	214	214	214	214	2° - .30%
500	932	933	933	933	933	933	933	1° - .07%
1000	1832	1830	1830	1830	1830	1830	1830	2° - .09%

COMMENTS

- ⊙ AVERAGE TEMPERATURE READING = MEAN OF THE TEMPERATURE READINGS FOR THE THERMOCOUPLE CHANNELS
  - ⊙ THE CHANNEL READINGS MUST AGREE WITHIN ±5°F OR 3°C
- ACCEPTABLE TEMPERATURE DIFFERENCE ±1.5 =  $\left( \frac{(\text{REF TEMP}^{\circ}\text{F} + 450) \cdot (\text{TEST TEMP}^{\circ}\text{F} + 450)}{(\text{REF TEMP}^{\circ}\text{F} + 450)} \right) \times 100$



**DRY GAS METER CALIBRATION USING CRITICAL ORIFICES**

CLIENT: DOE-Wisconsin Electric Co.

FACILITY: Marquette, MI.

DATE: 7/21/79  
 METER BOX #: 6  
 DRY GAS METER SERIAL #: 9429  
 CRITICAL ORIFICE SET SERIAL #: 13229  
 AVG (P<sub>bar</sub>) 29.72  
 IF Y VARIATION ORIFICE SHOULD

FINAL 29.27

INITIAL 29.27

BAROMETRIC PRESSURE (in Hg):

TESTED VACUUM (in Hg)

ORIFICE #	RUN #	K' FACTOR (AVG)	TESTED VACUUM (in Hg)	DGM READINGS (FT <sup>3</sup> )		TEMPERATURES °F		DGM INLET	DGM OUTLET	DGM AVG	ELAPSED TIME (MIN)	DGM ΔH (in H <sub>2</sub> O)	V <sub>m</sub> (STD)	V <sub>c</sub> (STD)	(3)
				INITIAL	FINAL	INITIAL	FINAL								
11	1	0.3237	24	630.698	638.293	72	73	74	71	71	10.00	0.82	4.2977	4.1722	0.9708
	2	0.3237	24	638.263	639.690	72	74	76	72	72	10.10	0.82	4.3666	4.2139	0.9668
	3	0.3237	24	639.690	644.078	72	77	76	73	74	10.10	0.82	4.3137	4.2139	0.9789
													AVG =		0.9716
24	1	0.6703	21	644.078	653.294	72	79	84	74	77	10.20	2.5	9.0330	8.8123	0.9766
	2	0.6703	21	653.294	662.389	72	84	88	77	79	10.00	2.5	8.8276	8.6396	0.9787
	3	0.6703	21	662.389	671.490	72	89	91	80	81	10.00	2.5	8.6368	8.6396	0.9774
													AVG =		0.9772
16	1	0.4801	22	671.490	677.706	72	87	89	82	83	10.00	1.2	6.9979	6.8013	0.9672
	2	0.4801	22	677.706	689.928	72	88	89	83	84	10.00	1.2	6.9880	6.8013	0.9672
	3	0.4801	22	689.928	690.166	72	89	89	84	85	10.00	1.2	6.9849	6.8013	0.9677
													AVG =		0.9674

USING THE CRITICAL ORIFICES AS CALIBRATION STANDARDS:

- Select three critical orifices to calibrate the dry gas meter which bracket the expected operating range.
- Record barometric pressure before and after calibration procedure.
- Run at maximum attainable vacuum (open coarse valve, close fine valve), for period of 5 minutes minimum for large orifice up to 10 minutes for smallest orifice.
- Record readings in outlined boxes, other columns are automatically calculated.

$$(1) V_m (std) = K_1 V_m \frac{P_{bar} + (\Delta H/13.6)}{T_m}$$

= Net volume of gas sample passed through DGM, corrected to standard conditions  
 $K_1 = 17.64 \text{ }^{\circ}\text{R/in. Hg (English), } 0.3858 \text{ }^{\circ}\text{K/mm Hg (Metric)}$   
 $T_m = \text{Absolute DGM avg. temperature (}^{\circ}\text{R - English, }^{\circ}\text{K - Metric)}$

$$(2) V_c (std) = K' \sqrt{\frac{P_{bar} \theta}{T_{amb}}}$$

= Volume of gas sample passed through the critical orifice, corrected to standard conditions  
 $T_{amb} = \text{Absolute ambient temperature (}^{\circ}\text{R - English, }^{\circ}\text{K - Metric)}$   
 $K' = \text{Average K' factor from Critical Orifice Calibration}$

AVERAGE DRY GAS METER CALIBRATION FACTOR, Y = **0.9720**



LONG/PRE DRY GAS METER CALIBRATION DATA FORM

Calibrator P. Mack  
 Date 2/25/99

Meter Box Number 12 Plant \_\_\_\_\_  
 Barometric pressure, P<sub>b</sub> = 29.72 in. Hg Dry Gas Meter Number 6898070 Comments \_\_\_\_\_

Setting	Gas volume		Temperatures			Time (θ), min	Y <sub>i</sub>	ΔH @, in. H <sub>2</sub> O
	Wet test meter (V <sub>w</sub> ) ft <sup>3</sup>	Dry gas meter (V <sub>d</sub> ) ft <sup>3</sup>	Wet test meter (t <sub>w</sub> ) °F	Inlet (t <sub>d</sub> ) °F	Outlet (t <sub>d</sub> ) °F			
0.5	5	328.659 323.650	66	69.75	69.72	71	1.006	1.7646
1.0	5	733.685 728.659	66	75.77	72.73	74	1.007	1.8710
1.5	10	743.761 733.685	66	79.84	73.76	78	1.011	1.9513
2.0	10	753.860 743.761	67	83.86	76.77	80.5	1.010	1.9977
3.0	10	763.877 753.860	67	87.70	78.79	83.5	1.012	1.9927
							AVG	Y 1.009 ΔH @ 1.9055

If there is only one thermometer on the dry gas meter, record the temperature under t<sub>d</sub>.

(ΔH) in. H <sub>2</sub> O	$\frac{\Delta H}{13.6}$	$Y_i = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H @ i = \frac{0.0317 \Delta H}{P_b (t_d + 460)}$	$\left[ \frac{(t_w + 460) \Theta}{V_w} \right]$
0.5	0.0368	(5) (29.72) (71 + 460) (5.009) (29.72 + 0.368) (66 + 460)	(0.0317) (6.5) (29.72) (71 + 460)	(66 + 460) (12.6) 5
1.0	0.0735	(5) (29.72) (74 + 460) (5.026) (29.72 + 0.735) (66 + 460)	(0.0317) (1.0) (29.72) (74 + 460)	(66 + 460) (9.2) 5
1.5	0.110	(10) (29.72) (78 + 460) (10.076) (29.72 + 1.10) (66 + 460)	(0.0317) (1.5) (29.72) (78 + 460)	(66 + 460) (15.4) 10
2.0	0.147	(10) (29.99) (80.5 + 460) (10.099) (29.72 + 1.47) (67 + 460)	(0.0317) (2.0) (29.72) (80.5 + 460)	(67 + 460) (13.5) 10
3.0	0.221	(10) (29.72) (83.5 + 460) (10.112) (29.72 + 2.21) (67 + 460)	(0.0317) (3.0) (29.72) (83.5 + 460)	(67 + 460) (10.9) 10



STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

DATE 23 FEB 99  
 AMBIENT TEMPERATURE 68.2  
 CALIBRATION 6P

POTENTIOMETER NUMBER 11-1224 L 12  
 BAROMETRIC PRESSURE 29.99  
 REFERENCE: THERMOCOUPLE SIMULATOR  
 (ACCURACY: 1°F)

REFERENCE TEMPERATURE		TEMPERATURE READING FROM THERMOCOUPLE CHANNEL INPUT NUMBER					AVERAGE TEMPERATURE READING <sup>⊙</sup>	TEMPERATURE DIFFERENCE <sup>⊙</sup> (%)
°C	°F	1	2	3	4	5		
0	32	32	32	32	32	32	32	0% - 0%
100	212	213	213	213	213	213	213	1% - .15%
500	932	933	933	933	933	933	933	1% - .07%
1000	1832	1830	1830	1831	1831	1832	1830.8	1.2% - .05%

COMMENTS

⊙ AVERAGE TEMPERATURE READING = MEAN OF THE TEMPERATURE READINGS FOR THE THERMOCOUPLE CHANNELS

⊙ THE CHANNEL READINGS MUST AGREE WITHIN ± 5°F OR 3°C

ACCEPTABLE TEMPERATURE DIFFERENCE ± 1.5 = 
$$\left( \frac{(\text{REF TEMP}^{\circ}\text{F} + 460) \cdot (\text{TEST TEMP}^{\circ}\text{F} + 460)}{(\text{REF TEMP}^{\circ}\text{F} + 460)} \right) \times 100$$



DRY GAS METER CALIBRATION USING CRITICAL ORIFICES

CLIENT: DOE-Wisconsin Electric Co.

FACILITY: Marquette, MI

DATE: 8/29/89 METER BOX #: 12 DRY GAS METER SERIAL #: 8086070 CRITICAL ORIFICE SET SERIAL #: 13225

IF Y VARIATION ORIFICE SHOULD

INITIAL 29.25 FINAL 29.25 AVG (P<sub>bar</sub>) 29.25

BAROMETRIC PRESSURE (in Hg): 29.25

ORIFICE #	RUN #	K FACTOR (AVG)	TESTED VACUUM (in Hg)	DGM READINGS (FT <sup>2</sup> )		TEMPERATURES °F		DGM INLET INITIAL	DGM INLET FINAL	DGM OUTLET INITIAL	DGM OUTLET FINAL	DGM AVG	ELAPSED TIME (MIN)	DGM AH (in H <sub>2</sub> O)	(1) V <sub>m</sub> (STD)	(2) V <sub>m</sub> (STD)	(3) Y
				INITIAL	FINAL	INITIAL	FINAL										
11	1	0.3237	27	931.266	935.964	72	74	74	76	71	72	73.25	10.00	0.68	4.2642	4.1062	0.9630
	2	0.3237	27	935.564	940.081	72	80	80	73	72	72	76.25	10.00	0.68	4.2393	4.1062	0.9666
	3	0.3237	27	940.061	944.472	72	80	82	73	74	74	77.25	10.00	0.68	4.2449	4.1062	0.9673
18	1	0.6114	22	944.472	951.382	72	77	81	74	74	74	76.5	10.00	1.6	6.6568	6.4872	0.9746
	2	0.6114	22	951.362	965.283	72	80	82	74	76	77.75	10.00	1.6	6.6520	6.4872	0.9762	
	3	0.6114	22	958.283	966.182	72	84	85	77	77	80.75	10.00	1.6	6.6131	6.4872	0.9810	
24	1	0.6703	20	965.162	973.844	72	81	86	78	78	80	82.75	10.00	2.66	8.4620	8.5029	1.0060
	2	0.6703	20	973.944	982.994	72	80	86	76	78	80	82.75	10.00	2.66	8.7099	8.5029	0.9762
	3	0.6703	20	982.994	992.024	72	86	88	78	79	82.75	10.00	2.66	8.6468	8.5029	0.9834	
													AVG =	0.9663			
													AVG =	0.9769			
													AVG =	0.9853			
													AVG =	0.9772			

USING THE CRITICAL ORIFICES AS CALIBRATION STANDARDS:

- Select three critical orifices to calibrate the dry gas meter which bracket the expected operating range.
- Record barometric pressure before and after calibration procedure.
- Run at maximum attainable vacuum (open coarse valve, close fine valve), for period of 5 minutes minimum for large orifice up to 10 minutes for smallest orifice
- Record readings in outlined boxes, other columns are automatically calculated

(1)  $V_m (std) = K_1 V_n \frac{P_{bar} + (\Delta H/13.6)}{T_m}$  = Net volume of gas sample passed through DGM, corrected to standard conditions  
 $K_1 = 17.64 \frac{in. Hg (English)}{in. Hg (Metric)}$   
 $T_m$  = Absolute DGM avg. temperature (°R - English, °K - Metric)

(2)  $V_m (std) = K \sqrt{\frac{P_{bar} \theta}{T_{amb}}}$  = Volume of gas sample passed through the critical orifice, corrected to standard conditions  
 $T_{amb}$  = Absolute ambient temperature (°R - English, °K - Metric)

(3)  $Y = \frac{V_m (std)}{V_m (std)}$  = DGM calibration factor  
 $K$  = Average K factor from Critical Orifice Calibration



STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

DATE 8/09/99  
AMBIENT TEMPERATURE 72  
CALIBRATION Sp / Pichella

POTENTIOMETER NUMBER 2010 #12  
BAROMETRIC PRESSURE 29.25  
REFERENCE: THERMOCOUPLE SIMULATOR  
(ACCURACY ± 1°F)

REFERENCE TEMPERATURE °C      °F	TEMPERATURE READING FROM THERMOCOUPLE CHANNEL INPUT NUMBER					AVERAGE TEMPERATURE READING °	TEMPERATURE DIFFERENCE (%)
	1	2	3	4	5		
0      32	31	31	31	31	31	31	1° - 1.2%
100      212	212	212	212	212	212	212	0° - 0%
500      932	932	932	932	932	932	932	0° - 0%
1000      1832	1828	1828	1828	1828	1828	1828	4° - 1.7%

COMMENTS

⊙ AVERAGE TEMPERATURE READING = MEAN OF THE TEMPERATURE READINGS FOR THE THERMOCOUPLE CHANNELS

⊙ THE CHANNEL READINGS MUST AGREE WITHIN ± 5°F OR 3°C

ACCEPTABLE TEMPERATURE DIFFERENCE ± 1.5 = 
$$\left( \frac{(\text{REF TEMP}^{\circ}\text{F} + 460) \cdot (\text{TEST TEMP}^{\circ}\text{F} + 460)}{(\text{REF TEMP}^{\circ}\text{F} + 460)} \right) \times 100$$



LONG/PRE DRY GAS METER CALIBRATION DATA FORM

Calibrator P. Mack  
 Date 3/30/99

Meter Box Number 19 Plant 684869  
 Barometric pressure, P<sub>b</sub> = 29.83 in. Hg Dry Gas Meter Number 684869 Comments

Setting	Gas volume			Temperatures			Time (e), min	Y <sub>1</sub>	ΔH @, in. H <sub>2</sub> O
	Wet test meter (V <sub>w</sub> ) ft <sup>3</sup>	Dry gas meter (V <sub>d</sub> ) ft <sup>3</sup>	Wet test meter (t <sub>w</sub> ) °F	Inlet (td) °F	Dry gas meter Outlet (td) °F	Avg (t <sub>d</sub> ) °F			
0.5	5	838.464 835.448	69	77.79	74.75	76	13.0	1.0088	1.8753
1.0	5	843.784 838.444	69	80.82	76.76	78.5	9.2	1.0130	1.8697
1.5	10	853.507 845.481	69.5	82.87	76.78	81	15.7	1.0097	2.0362
2.0	10	863.443 853.780	69.5	85.89	79.80	83	13.4	1.0102	1.9705
3.0	10	873.675 863.780	69.5	85.90	80.81	84	10.9	1.0082	1.9521
							Avg	Y	ΔH @
								1.0088	1.9408

If there is only one thermometer on the dry gas meter, record the temperature under td.

(ΔH) in. H <sub>2</sub> O	$\frac{\Delta H}{13.6}$	$Y_1 = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H @ i = \frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[ \frac{(t_w + 460) \Theta}{V_w} \right]^2$
0.5	0.0368	(5) (29.83) (76 + 460) (5.015) (29.83 + 0.368) (69 + 460)	(1.0317) (-.5) (29.83) (76 + 460) 5 (13.0)
1.0	0.0735	(5) (29.83) (78.5 + 460) (5.017) (29.83 + 0.735) (69 + 460)	(1.0317) (1.0) (29.83) (78.5 + 460) 5 (13.2)
1.5	0.110	(10) (29.83) (81 + 460) (10.082) (29.83 + 1.10) (69.5 + 460)	(1.0317) (1.5) (29.83) (81 + 460) 10 (15.7)
2.0	0.147	(10) (29.83) (83 + 460) (10.102) (29.83 + 1.47) (69.5 + 460)	(1.0317) (2.0) (29.83) (83 + 460) 10 (15.4)
3.0	0.221	(10) (29.83) (84 + 460) (10.115) (29.83 + 2.21) (69.5 + 460)	(1.0317) (3.0) (29.83) (84 + 460) 10 (16.9)



### STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

DATE 23 FEB 99  
 AMBIENT TEMPERATURE 67.6 ± .2  
 CALIBRATION GP

POTENTIOMETER NUMBER NUTRIT #14  
 BAROMETRIC PRESSURE 29.94  
 REFERENCE: THERMOCOUPLE SIMULATOR  
 (ACCURACY: ±1°F)

REFERENCE TEMPERATURE		TEMPERATURE READING FROM THERMOCOUPLE CHANNEL INPUT NUMBER					AVERAGE TEMPERATURE READING °	TEMPERATURE DIFFERENCE (%)
°C	°F	1	2	3	4	5		
0	32	34	34	34	34	34	34	2° - .4%
100	212	214	214	214	214	214	214	2° - .30%
500	932	934	934	934	934	934	934	2° - .14%
1000	1832	1831	1831	1831	1831	1831	1831	1° - .04%

COMMENTS

⊙ AVERAGE TEMPERATURE READING = MEAN OF THE TEMPERATURE READINGS FOR THE THERMOCOUPLE CHANNELS

⊙ THE CHANNEL READINGS MUST AGREE WITHIN ±5°F OR 3°C

ACCEPTABLE TEMPERATURE DIFFERENCE ±1.5 =

$$\left( \frac{(\text{REF TEMP}^{\circ}\text{F} + 460) \cdot (\text{TEST TEMP}^{\circ}\text{F} + 460)}{(\text{REF TEMP}^{\circ}\text{F} + 460)} \right) \times 100$$



**DRY GAS METER CALIBRATION USING CRITICAL ORIFICES**

CLIENT: DOE-Wisconsin Electric Co. \_\_\_\_\_

FACILITY: Marquette, MI. \_\_\_\_\_

DATE: 7/24/99 METER BOX #: 14 DRY GAS METER SERIAL #: 6648169 CRITICAL ORIFICE SET SERIAL #: 13225 INITIAL BAROMETRIC PRESSURE (in Hg): 29.27 FINAL BAROMETRIC PRESSURE (in Hg): 29.27 AVG (P<sub>bar</sub>) 29.27 IP Y VARIATH ORIFICE SHOULD

ORIFICE #	RUN #	K' FACTOR (AVG)	TESTED VACUUM (in Hg)	DGM READINGS (FT <sup>3</sup> )		TEMPERATURES °F				DGM AVG	ELAPSED TIME (MIN)	DGM ΔH (in H <sub>2</sub> O)	(1) V <sub>m</sub> (STD)	(2) V <sub>w</sub> (STD)	(3) Y
				INITIAL	FINAL	NET (V <sub>g</sub> )	AMBIENT	DOM INLET	DOM INLET						
24	1	0.6703	19	158.210	167.871	8.661	72	83	84	82	82	10.00	8.2878	8.6087	1.0284
	2	0.6703	19	167.871	176.521	8.660	72	83	86	81	81	10.00	8.2911	8.6087	1.0282
	3	0.6703	19	176.521	185.174	8.663	72	84	86	81	82	10.00	8.2826	8.6087	1.0273
16	1	0.4801	22	188.174	190.997	6.823	72	86	86	82	82	10.00	6.6491	6.7186	1.0296
	2	0.4801	22	190.997	196.813	6.816	72	86	86	82	82	10.00	6.6460	6.7186	1.0304
	3	0.4801	22	196.813	202.633	6.820	72	86	87	83	84	10.00	6.6396	6.7186	1.0326
11	1	0.3237	24	202.633	206.799	4.166	72	86	86	84	84	10.00	3.9648	4.1060	1.0390
	2	0.3237	24	206.799	210.965	4.166	72	86	86	84	83	10.00	3.9632	4.1060	1.0381
	3	0.3237	24	210.965	215.125	4.160	72	86	87	84	86	10.00	3.9453	4.1060	1.0416
												AVG =	8.6087	1.0283	
												AVG =	6.7186	1.0296	
												AVG =	4.1060	1.0390	

**USING THE CRITICAL ORIFICES AS CALIBRATION STANDARDS:**

- Select three critical orifices to calibrate the dry gas meter which bracket the expected operating range.
- Record barometric pressure before and after calibration procedure.
- Run at maximum attainable vacuum (open coarse valve, close fine valve), for period of 5 minutes minimum for large orifice up to 10 minutes for smallest orifice.
- Record readings in outlined boxes, other columns are automatically calculated.

(1)  $V_m (std) = K_i V_m \frac{P_{bar} + (\Delta H/13.6)}{T_m}$  = Net volume of gas sample passed through DGM, corrected to standard conditions  
 $K_i = 17.64 \frac{P_{bar}}{T_m} \frac{1}{P_{bar} + (\Delta H/13.6)}$   
 $T_m$  = Absolute DGM avg. temperature (°R - English, °K - Metric)

(2)  $V_w (std) = K' \sqrt{\frac{P_{bar} \theta}{T_{amb}}}$  = Volume of gas sample passed through the critical orifice, corrected to standard conditions  
 $T_{amb}$  = Absolute ambient temperature (°R - English, °K - Metric)

(3)  $Y = \frac{V_w (std)}{V_m (std)}$  = DGM calibration factor  
 $K' = \text{Average } K' \text{ factor from Critical Orifice Calibration}$

AVERAGE DRY GAS METER CALIBRATION FACTOR, Y = 1.0322



### STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

DATE 7/24/97  
 AMBIENT TEMPERATURE 72  
 CALIBRATION OK by [Signature]

POTENTIOMETER NUMBER 2010 #14  
 BAROMETRIC PRESSURE 29.27  
 REFERENCE: THERMOCOUPLE SIMULATOR  
 (ACCURACY: ±1°F)

REFERENCE TEMPERATURE		TEMPERATURE READING FROM THERMOCOUPLE CHANNEL INPUT NUMBER					AVERAGE TEMPERATURE READING	TEMPERATURE DIFFERENCE
°C	°F	1	2	3	4	5	°	(%)
0	32	33	33	33	33	33	33	1° - .29%
100	212	214	214	214	214	214	214	2° - .30%
500	932	934	934	934	934	934	934	2° - .14%
1000	1832	1831	1831	1831	1831	1831	1831	1° - .04%

COMMENTS

⊙ AVERAGE TEMPERATURE READING = MEAN OF THE TEMPERATURE READINGS FOR THE THERMOCOUPLE CHANNELS

⊙ THE CHANNEL READINGS MUST AGREE WITHIN: ±5°F OR ±3°C

ACCEPTABLE TEMPERATURE DIFFERENCE ±1.5 = 
$$\left( \frac{(\text{REF TEMP}^{\circ}\text{F} + 460) \cdot (\text{TEST TEMP}^{\circ}\text{F} + 460)}{(\text{REF TEMP}^{\circ}\text{F} + 460)} \right) \times 100$$

APRIL 97



PITOT TUBE IDENTIFICATION NUMBER: P142

### TYPE S PITOT TUBE INSPECTION DATA FORM

PITOT TUBE ASSEMBLY LEVEL?  (YES)  (NO)  
PITOT TUBE OPENINGS DAMAGED?  (YES-EXPLAIN BELOW)  (NO)

$\alpha_1 = 0^\circ (<10)$                        $\alpha_2 = 0^\circ (<10)$

$\beta_1 = 0^\circ (<5)$                        $\beta_2 = 0^\circ (<5)$

$\gamma = 1^\circ$                        $\theta = 0^\circ$                        $A = 94$  in.

$z = A \sin \gamma = 1.01$  in.; (<1/8 in.),

$w = A \sin \theta = 0$  in.; (<1/32 in.),

$P_a = 47$  in.                       $P_b = 47$  in.

$D_1 = 38$  in.                       $P_a = P_b?$   (YES)  (NO)

COMMENTS \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

CALIBRATION REQUIRED?  (YES)  (NO)

INSPECTOR: Tom Buegel                      DATE 12-22-98



PITOT TUBE IDENTIFICATION NUMBER: P200

### TYPE S PITOT TUBE INSPECTION DATA FORM

PITOT TUBE ASSEMBLY LEVEL?  (YES)  (NO)

PITOT TUBE OPENINGS DAMAGED?  (YES-EXPLAIN BELOW)  (NO)

$\alpha_1 = 0^\circ (<10)$

$\alpha_2 = 1^\circ (<10)$

$\beta_1 = 1^\circ (<5)$

$\beta_2 = 0^\circ (<5)$

$\gamma = 0^\circ$

$\theta = 0^\circ$

$A = .62$  in.

$z = A \sin \gamma = 0$  in.; ( $<1/8$  in.),

$w = A \sin \theta = 0$  in.; ( $<1/32$  in.),

$P_a = .31$  in.

$P_b = .31$  in.

$D_t = .25$  in.

$P_a = P_b$ ?  (YES)  (NO)

COMMENTS \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

CALIBRATION REQUIRED?  (YES)  (NO)

INSPECTOR [Signature] DATE 4/14/99



PITOT TUBE IDENTIFICATION NUMBER: P-300

### TYPE S PITOT TUBE INSPECTION DATA FORM

PITOT TUBE ASSEMBLY LEVEL?  (YES)  (NO)

PITOT TUBE OPENINGS DAMAGED?  (YES-EXPLAIN BELOW)  (NO)

$\alpha_1 = 3^\circ (< 10^\circ)$        $\alpha_2 = 2^\circ (< 10^\circ)$

$\beta_1 = 1^\circ (< 5^\circ)$        $\beta_2 = 1^\circ (< 5^\circ)$

$\gamma = 0^\circ$        $\theta = 0^\circ$        $A = .94$  in.

$z = A \sin \gamma = 0$  in. ( $< 1/32$  in.)

$w = A \sin \theta = 0$  in. ( $< 1/32$  in.)

$P_1 = .47$  in.       $P_2 = .47$  in.

$D_1 = .58$  in.       $P_1 = P_2?$   (YES)  (NO)

COMMENTS 17 inch head  
\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

CALIBRATION REQUIRED?  (YES)  (NO)

INSPECTOR Judy Ann DATE 2-10-99



PITOT TUBE IDENTIFICATION NUMBER: P-301

### TYPE S PITOT TUBE INSPECTION DATA FORM

PITOT TUBE ASSEMBLY LEVEL?  (YES)  (NO)

PITOT TUBE OPENINGS DAMAGED?  (YES-EXPLAIN BELOW)  (NO)

$\alpha_1 = \underline{0^\circ}$  (<10)

$\alpha_2 = \underline{0^\circ}$  (<10)

$\beta = \underline{0^\circ}$  (<5)

$\beta_2 = \underline{6^\circ}$  (<5)

$\gamma = \underline{1^\circ}$

$\theta = \underline{0^\circ}$

A = .83 in.

$\delta = \underline{.01}$  in. (<.8)

w = A sin  $\theta = \underline{0}$  in. (<1/32 in.)

$P_1 = \underline{.465}$  in.

$P_2 = \underline{.465}$  in.

$P_3 = \underline{.38}$  in.

$P_3 = P_2$ ?  (YES)  (NO)

COMMENTS 17 inch head  
\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

CALIBRATION REQUIRED?  (YES)  (NO)

[Signature] DATE 2-10-99



IDENTIFICATION NUMBER: 302

### TYPE S PITOT TUBE INSPECTION DATA FORM

PITOT TUBE ASSEMBLY LEVEL?  (YES)  (NO)

PITOT TUBE OPENINGS DAMAGED?  (YES-EXPLAIN BELOW)  (NO)

$\alpha_1 = 0^\circ (< 10)$

$\alpha_2 = 0^\circ (< 10)$

$\beta_1 = 0^\circ (< 5)$

$\beta_2 = 0^\circ (< 5)$

$\gamma = 1^\circ$

$\theta = 0$

A = 23 in.

$\delta = 0^\circ (< 8)$

W = A sin  $\theta = 0$  in. ( $< 1/32$  in.)

$P_1 = 465$

$P_2 = 465$

$P_3 = 38$

$P_1 = P_2?$   (YES)  (NO)

COMMENTS 18 in head

CALIBRATION REQUIRED?  (YES)  (NO)

John [Signature] DATE 2/10/77